

1 **New anti-clogging perspective by discharging sediment from**  
2 **drip irrigation emitters with high-sediment loaded water**

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10 **Abstract:** The promotion of drip irrigation technology has been severely constrained by the emitter  
11 clogging caused by sediment deposition when using high-sediment loaded water. To fill this gap, a  
12 novel solution to the emitter clogging issue has been developed by allowing fine sediment particles  
13 to drain as much through the emitter as possible. The sediment deposition and discharge ratio, the  
14 sediment discharge rate, and the control threshold for particle size were used to determine the  
15 sediment discharge capacity (SDC) of the emitter. The result shows that almost all (>99%) the fine-  
16 grained sediment (<100  $\mu\text{m}$ ) can be discharged from the flow path of eight emitters, which varied  
17 greatly in different emitters. Specifically, pressure compensating emitters (PCE) had higher SDC  
18 than non-pressure compensating emitters (NPCE), with relative average flow rate increased by  
19 16.9%-33.0%. Meanwhile, the emitter flow path structure significantly affects SDC. The side wall  
20 of the flow path could be changed from a toothed structure to a swirl wash wall optimized structure,  
21 which would significantly improve the SDC. Furthermore, the SDC of NPCE was primarily affected  
22 by the flow path length (L), and the ratio of the cross-sectional area to the length ( $\sqrt{A}/L$ ). Lastly,  
23 stronger emitter SDC closely related to both smaller particle size and concentration of water source.  
24 This study presents a fresh idea of sediment treatment for drip irrigation systems with high sediment  
25 content water and may contribute to the design of emitters with high sediment discharge capacity,  
26 and the effective management and filtration treatment of high-sediment loaded water.

27 **Keywords:** drip irrigation; clogging; self-discharge capacity; flow path structure

## 28 **1. Introduction**

29       The scarcity of irrigation water has become a key obstacle to sustainable agricultural  
30 production. High-sediment water (HSW), which can adequately compensate the lack of traditional  
31 water resources, is widely distributed throughout the world, in areas such as southwest Europe and  
32 northwest China (Puertes et al, 2021; Duker et al, 2020; Niu et al, 2013). Meanwhile, due to the  
33 precise and regulated volume of applied irrigation water, drip irrigation is regarded as one of the  
34 most effective water-saving methods (Zhou et al, 2019). As a result, the invention of drip irrigation  
35 utilizing high-sediment loaded water is regarded as an effective method for solving the problem of  
36 water scarcity in agriculture (Qin et al, 2019; Zeng et al, 2018). However, A significant amount of  
37 sediment in high-sediment water can easily cause serious clogging of emitters, which impairs  
38 distribution uniformity, reduces efficiency and crop productivity, thus, the application and  
39 promotion of drip irrigation with high-sediment water is severely constrained by the emitter  
40 clogging (EI-Bouhali et al, 2020; Han et al, 2019; Zhang et al, 2017).

41       Sedimentation and filtration are the most frequently used methods to prevent particles enter  
42 into emitter, and thereby they help controlling the emitter clogging in HSW drip irrigation systems  
43 (Shen et al, 2022; Bové et al, 2017; Capra et al, 2004). These methods are effective in reducing the  
44 coarse-grained sediment, but they are always unsatisfactory for filtering the HSW with primarily  
45 fine sediment particles (e.g., the Yellow River water) (Zhang et al, 2021; Puig-Bargués and Lamm,  
46 2013). This is mainly because the slow settling rate of fine sediment particles makes it difficult to  
47 treat high concentrations of sediment using the conventional sedimentation and filtration methods  
48 (Tao et al., 2017). Moreover, due to the large amount of filter mesh required for fine particle  
49 sediment filtering, regular automatic back-washing and high energy consumption are necessary

50 (Zhang et al., 2021). Therefore, efficient treatment of fine particles of sediment has become the key  
51 to alleviate the clogging of HSW drip irrigation emitters.

52 In fact, fine sediment particles in the water are smaller than the emitter flow path size, usually  
53 being less than 1/7 of the flow path size (Liu et al., 2012). This suggested that fine sediment particles  
54 could be directly discharged from the emitter flow path. In this case, it could be possible to promote  
55 the discharge of fine sediment particles by enhancing the self-discharge capacity of the emitter, and  
56 thereby mitigate emitter clogging. Moreover, another advantage of the suggested method was to  
57 reduce the requirements of the filtration system. Therefore, the range of sediment particle sizes and  
58 concentrations that the emitter can discharge must be further investigated. According to previous  
59 studies, emitter clogging was more likely to occur in the case of a sediment particle size of  $>17\ \mu\text{m}$ ,  
60 and the risk of emitter clogging increases significantly when the particle size was  $>30\ \mu\text{m}$ , or when  
61 more fine sediment particles are contained (Wu et al., 2014). Besides, it is believed that the sensitive  
62 particle size of the labyrinth flow path of the emitter was 0.031-0.038 mm, and that the more  
63 sensitive sediment content range was 1.25-1.50 g/L (Niu et al., 2013; Liu et al., 2012). In general,  
64 the current research is only targeted at dynamic changes in the silt content and particle size  
65 distribution inside the emitter, and there has been no research reported that specifically targets at the  
66 evaluation index of the emitter's sediment removal capacity. Also, it is still unclear what influences  
67 the emitter self-discharge ability and what the optimization and enhancement method is.

68 Based on this, an in-situ test on the Yellow River water drip irrigation system emitter clogging  
69 was conducted in the river-loop irrigation area, and the difference of sediment particle size and  
70 concentration inside the emitter of different structures under different water source particle size and  
71 concentration conditions were tested systematically. The objectives of the study were to: (1) present

72 an evaluation index for the sediment self-discharge capacity of the emitter; (2) confirm the factors  
73 (e.g., emitter flow path, sediment particle size, sediment concentration) that influence the self-  
74 discharge sediment capacity of emitters.

## 75 **2. Materials and Methods**

### 76 **2.1 Experimental system**

77 This experiment was conducted at Dengkou County Irrigation Experiment Station in the Hetao  
78 Irrigation District of Bayannur City, Inner Mongolia Autonomous Region (China). The Yellow River  
79 sediment was mixed with water to simulate sandy water sources. The treatments carried out on the  
80 irrigation water are shown in Supplementary Material (Table S1). The particle size ranges of the  
81 water sources were 0-41  $\mu\text{m}$ , 0-75  $\mu\text{m}$  and 0-100  $\mu\text{m}$ , and the concentration of sediment in water  
82 distribution was 1 g/L and 3g/L. Considering the sediment loss during operation, sediment  
83 concentration test was conducted once every three days to ensure that the concentration deviation  
84 was controlled within 5%. In addition, the water source was replaced once every 6 days.

85 The drip irrigation pipeline was laid out in the mode of "4 layers + 4 columns". The length of  
86 the drip irrigation unit was 15 m, the flow rate inside the drip tape is 0.07-0.11m/s, the emitter is  
87 facing upwards. The pressure (0.1 MPa) was maintained at a particular level by gradually regulating  
88 and diverting the flow. Filtration system can filter sediment with a particle size of 150 $\mu\text{m}$  or above,  
89 which has no effect on the experimental configuration of the sediment particle size. The flushing  
90 flow rate control device was placed at the end of the platform. The system was flushed with a  
91 flushing velocity of 0.45m/s during 6 min every 80 h of operation. Combining the ISO standard  
92 (ISO 9261) of clogging test methods for emitters and the clogging determination criteria studied by  
93 Pei et al (2014), the experimental system test was operated for 10 h per day and the system was

94 operated for a total of 640 h.

95 Consistent with Muhammad et al. (2021), the test platform is mainly composed of three parts  
96 (including the water source, the filtration system, and the drip irrigation unit), as shown in Fig. 1.  
97 The system operation mode is shown in Supplementary Material. The experimental system run 10  
98 h per day up to a total operation time of 640 h. Eight flat emitters with different structure were  
99 hereby selected. Non-pressure compensating emitters (NPC) with toothed flow path (NPCL) of 1.0  
100 L/h, 1.4 L/h and 1.6 L/h flow rate, respectively. And non-pressure compensating emitters with vortex  
101 wash wall optimized flow path (NPCW) of the same flow rate were chosen. Similarly, pressure  
102 compensating emitters (PC) with two different discharges (1.0 L/h and 1.6 L/h) were selected. Both  
103 Table 1 and Fig. 2 display their flow path parameters and structures.

104 # Fig. 1 approximately here #

105 # Table 1 approximately here #

106 # Fig. 2 approximately here #

## 107 **2.2 Sampling and testing methods**

### 108 **2.2.1 Performance evaluation of drip irrigation emitter clogging**

109 In this experiment, the discharges of 45 emitters were measured using the weighing method  
110 described by Feng et al. (2018). Given that outdoor tests are susceptible to environmental influences  
111 that may cause testing and measurement bias, the emitter discharges were corrected according to  
112 the water temperature at the time of testing, following Pei et al. (2014) procedure. Emitter clogging  
113 was assessed by computing the average discharge variation rate (Dra) according to Muhammad et  
114 al. (2021) and Ghaemi (1998).

115 
$$Dra = \frac{\sum_i^n \frac{q_i^t}{q_i^0}}{n} \times 100\% \quad (1)$$

116 In Eq.1 is the flow at the initial moment of No.i emitter, in L/h; is the flow at  $t$  hour of No.i  
117 emitter, in L/h; and  $n$  is the total number of emitter installed along the lateral.

## 118 **2.2.2 Sampling and dry weight test of sediment**

119 Following Liu et al. (2019), sampling and dry weight (DW) determination of the sediment  
120 granules were carried out using ultrasonic techniques to flake off the clogging substance present.  
121 DW was measured from 15 emitters, including 5 emitters at the beginning, in the middle and at the  
122 end of the drip irrigation unit, respectively. The detailed test methods are shown in the  
123 Supplementary Materials.

## 124 **2.2.3 Concentration sample and test method**

125 The sediment concentration was measured using the weighing method with 300 mL sampling  
126 bottles at the water source and emitter outlet, respectively, following the procedure described by  
127 Hou et al. (2022). Concentration was measured from 9 emitters, including 3 emitters were taken at  
128 the beginning, in the middle and at the end of the drip irrigation unit, respectively.

## 129 **2.2.4 Particle size sample and test method**

130 Following Hou et al. (2022), The sediment particle size was measured using the weighing  
131 method with 300 mL sampling bottles at the water source and emitter outlet. The detailed test  
132 methods are shown in the Supplementary Materials.

## 133 **2.3 Evaluation index of the self-discharge capacity of sediment**

### 134 **2.3.1 Sediment discharge rate**

135 The calculation formula for the sediment discharge rate  $\phi_e$  for each type of emitter is shown in

136 Equation (1):

$$137 \quad \varphi_e = \frac{\rho_i}{\rho_0} \times 100\% \quad (1)$$

138 Where,  $\rho_0$  denotes the average value of irrigation water sediment concentration, g/L; and  $\rho_i$   
139 represents the average value of sediment concentration of the  $i$  th emitter outflow, g/L.

### 140 2.3.2 Sediment deposition and discharge ratio

141 The calculation formula for the sediment deposition and discharge ratio  $\varphi$  is shown in Equation  
142 (2):

$$143 \quad \varphi = \frac{\sum_{i=1}^n m_i \times n_i \times 15}{\sum_{i=1}^n \rho_i \times v_i} \times 100\% \quad (2)$$

144 Where,  $m_i$  is the average dry weight of clogging substances in emitter during the  $i$ -th flow  
145 measurement (each 15 m long), g/m;  $n_i$  is the corresponding number of emitter (each 15 m long drip  
146 irrigation unit);  $\rho_i$  is the  $i$  th emitter outflow sediment concentration, g/L; and  $v_i$  is the cumulative  
147 irrigation water volume, L.

### 148 2.3.3 Control threshold for the particle size

149 In order to explore the critical value of the sediment particle size discharged by different  
150 emitters, the distribution curve  $\lambda$  and the average line of total sediment discharge  $\eta$  were proposed  
151 for the interval of mass proportion of the sediment particle size discharged by emitters:

$$152 \quad \eta = \frac{m}{M} \quad (3)$$

$$153 \quad \lambda = \frac{m \times \mu_f}{M \times \mu} \quad (4)$$

154 Where,  $m$  refers to the average emitter discharge sediment dry weight, g;  $M$  is the total dry  
155 weight of sediment into the emitter, g;  $\mu_f$  is the particle size distribution of the sediment discharged  
156 from the emitter,  $\mu\text{m}$ ; and  $\mu$  is the particle size distribution of sediment into the emitter,  $\mu\text{m}$ .

157 From the above Equations (3) and (4), the calculated data for NPCL1 emitter, as example, is



158 shown in Fig. 3(a). When the emitter d the distribution curve  $\lambda$  is higher than the total sediment  
159 discharge average line  $\eta$ , the grain size interval mass ratio is considered positive (i.e., the emitter is  
160 releasing more solids than the average ratio of solids introduced), and the opposite, negative. Fig.  
161 3(b) was obtained by integrating the difference between  $\lambda$  and  $\eta$ . The highest positive value in Fig.  
162 3(b) corresponds to the particle size  $\mu_0$ , which is defined as the maximum value when the sediment  
163 particle is easy to discharge from the emitter. That is, the critical threshold of the emitter sediment  
164 discharge particle size.

165 # Fig. 3 approximately here #

## 166 2.4 Statistical analysis

167 Regression analysis was used to quantify the correlation among the Dra, sediment discharge  
168 capacity indicators, and structural parameters of the emitter. The significance of independent  
169 variables was determined at  $p < 0.05$ . The forecasting model for the control threshold  $\mu_0$  was based  
170 in a multivariate linear relationship. The variance inflation factor (VIF) was used during the process  
171 of establishing the multivariate linear relationship between  $\mu_0$  and its influences to exclude the multi-  
172 collinearity among the influences. All the above statistical processes were performed using SPSS  
173 (version 17.0, IBM Analytics).

## 174 3. Results and analysis

### 175 3.1 Emitter clogging performance

176 The variation of the Dra for different types of emitters is shown in Fig. 4(a) under the working  
177 conditions of 0-75  $\mu\text{m}$  and 3.0 g/L, while the rest of the working conditions are shown in the  
178 Supplementary Materials (Fig. S1). Fig. 4(b) shows the correlation of Dra of the different emitters  
179 regarding that of NPCL1. With the increase of the system's running time, Dra exhibited a trend of

180 slow decline until around the 300 h of operation, followed by a rapid reduction. Besides, there were  
181 obvious differences between the different emitters. The PCE performed better than NPCE under the  
182 same flow conditions. Overall, under the same flow conditions, the Dra of PCE was improved by  
183 16.9%-33.0% compared with the different NPCL emitters, and 23.0%-32.8% regarding the NPCW  
184 emitters. Among NPCE, the NPCW performed better, showing Dra 10.7%-14.1% higher than those  
185 of NPCL. Emitters at different flow rates presented different trends. At a flow rate of 1.0 L/h, the  
186 Dra of the NPCW and the PC emitters was improved by 13.1% and 33.0%, respectively, when  
187 compared with the NPCL1 emitter. However, at a flow rate of 1.6 L/h, NPCW3 and PC3 emitters  
188 only improved Dra by 14.1% and 16.9%, respectively, regarding NPCL3.

189 **# Fig. 4 approximately here #**

### 190 **3.2 Control threshold for particle size $\mu_0$**

191 The relative variation of the control threshold for particle size  $\mu_0$  for different types of emitters  
192 is shown in Fig. 5(a) under the working conditions of 0-75  $\mu\text{m}$  and 3.0 g/L. The evolution of the  
193 control threshold for the rest of experimental conditions is shown in the Supplementary Materials  
194 (Fig. S2), while Fig. 5(b) shows the correlation between  $\mu_0$  for NPCL1 and the other emitters tested.  
195 With the increase of the system's running time,  $\mu_0$  exhibited a declining trend, appearing obvious  
196 differences between emitters. Under the same flow conditions, PCE had higher  $\mu_0$  than NPCE.  
197 Overall,  $\mu_0$  of PCE was improved by 1.4%-21.3% compared with the NPCL emitters, and it was  
198 0.2%-7.61% when compared with the NPCW emitters. Among NPCE, the  $\mu_0$  of the NPCW emitters  
199 was larger than that of the NPCL, with an average improvement rate of 0.9%-14.2%. At the same  
200 time, emitters at different flow rates present different trends. At a flow rate of 1.0 L/h, the NPCW1  
201 and the PC1 emitters improved  $\mu_0$  regarding NPCL1 by 2.1%-14.2% and 4.1%-21.3%, respectively,

202 while at a flow rate of 1.6 L/h, the NPCW3 and PC3 emitters increased  $\mu_0$  by 0.9%-3.2% and 1.4%-  
203 2.8%, respectively. With the accumulated system operation, the control threshold value of the  
204 sediment discharge particle size of different types of emitters gradually decreased. With the increase  
205 of sediment concentration and particle size of the water source, the control threshold value of the  
206 sediment discharge particle size presents a decreasing and increasing trend, respectively  
207 (Supplementary Materials, Fig. S3). Further, control threshold for particle size was more influenced  
208 by particle size than concentration.

209 # Fig. 5 approximately here #

### 210 3.3 Sediment discharge rate ( $\varphi_e$ )

211 The relative variation of the  $\varphi_e$  for the different types of emitters under the working conditions  
212 of 0-75  $\mu\text{m}$  and 3.0 g/L is shown in Fig. 6(a). Results for the other working conditions are shown in  
213 the Supplementary Materials (Fig. S4). Fig. 6(b) depicts the correlations of  $\varphi_e$  between each emitter  
214 and NPCL1. With the increase of the system's running time,  $\varphi_e$  exhibited an increasing trend first  
215 and then a decrease. The sediments discharge rate of each emitter reached the maximum value when  
216 the system operated 200-400 h. Besides, there are obvious differences between different emitters.  
217 Under the same flow conditions,  $\varphi_e$  of PCE was higher than that of NPCE. Overall,  $\varphi_e$  of PCE was  
218 improved by -0.4%-2.7% compared with the NPCL emitters and -0.9%-1.2% compared with the  
219 NPCW emitters. For NPCE, the NPCW emitter performed better than the NPCL emitter, with a  
220 relative improvement of  $\varphi_e$  in the range -0.8%-2.3%. Besides, emitters at different flow rates  
221 presented different trends. At a flow rate of 1.0 L/h, the  $\varphi_e$  of the NPCW1 and the PC1 emitters were  
222 improved by -0.2%-2.3% and -0.1%-2.7%, respectively. Compared with the NPCL1, while at a flow  
223 rate of 1.6L/h,  $\varphi_e$  of the NPCW3 and the PC3 emitter were improved by -0.8%-0.7% and -0.9%-

224 0.6%, respectively. With the increase of the sediment concentration and particle size of the water  
225 source, the control threshold value of the sediment discharge particle size presents a trend of  
226 increasing and then decreasing, respectively (Supplementary Materials, Fig. S4).

227 **# Fig. 6 approximately here #**

### 228 **3.4 Sediment deposition and discharge ratio ( $\phi$ )**

229 The relative variation of  $\phi$  for the different types of emitters is shown in Fig. 7(a) under the  
230 working conditions of 0-75  $\mu\text{m}$  and 3.0 g/L. In the Supplementary Materials, Fig. S5 represents the  
231 rest of experimental conditions. It is shown that the emitter discharges more than 99% of sediment  
232 particles that enter it. Fig.7(b) depicts the correlation for  $\phi$  between each emitter and NPCL1. With  
233 the increase of the system's running time,  $\phi$  exhibited an increasing trend first and then decreasing,  
234 but there were clear differences between different emitters. Under the same conditions, the  $\phi$  of PCE  
235 is lower than NPCE. Overall, the relative effect of PCE was improved by 0.1%-69.8%, among which,  
236 the effect was improved by 11.5%-69.8% compared with the NPCL emitters and 0.1%-42.2%  
237 compared with the NPCW emitters. For NPCE, the NPCW emitter performed better than the NPCL  
238 emitter, with a  $\phi$  relative improved by 9.4%-50.7%. Besides, emitters at different flow rates  
239 presented different trends. At a flow rate of 1.0 L/h, the  $\phi$  of the NPCW1 and the PC1 emitters were  
240 improved by 14.7%-43.7% and 35.1%-67.6%, respectively, compared with the NPCL1, while at a  
241 flow rate of 1.6 L/h, those of the NPCW3 and the PC3 emitters were improved by 9.4%-29.6% and  
242 11.5%-34.4%, respectively. With the increase of the sediment concentration of the water source, the  
243 control threshold value for particle size presented a decreasing trend. (Fig. S5).

244 **# Fig. 7 approximately here #**

245 **3.5 Influence of NPC emitter geometry parameters and indicators for the sediment**  
246 **self-discharge capacity**

247 For NPCE, the influence of structural parameters and water source parameters on the indicators  
248 of the self-discharge capacity of the emitter is shown in Fig. 8. Among the structural parameters,  
249 there was a significant correlation between the emitter channel length (L), the ratio of the cross-  
250 sectional area to the length ( $\sqrt{A}/L$ ), the section mean flow velocity (v), the rated flow rate (Q) and  
251 three self-discharge sediment indicators. Among the water source parameters, the particle size, and  
252 the concentration had significant effects on the indicators of self-discharge capacity of the emitter.  
253 Taking the control threshold for particle size  $\mu_0$  as an example, a forecasting model for the control  
254 threshold  $\mu_0$  was constructed with its structural parameters (length of flow path (L), ratio of cross-  
255 sectional area of flow path open to length ( $\sqrt{A}/L$ ), section mean flow velocity (v), and rated flow  
256 rate (Q) as variables. As it is greatly influenced by the particle size gradation of the water source,  
257  $\mu_0$  varies within 6% under different concentration conditions (Fig. S6). Consequently, under the  
258 operating conditions of this experiment, prediction models for emitter sediment discharge particles  
259 by each of the three different sediment gradations (0-41  $\mu\text{m}$ , 0-75  $\mu\text{m}$ , and 0-100  $\mu\text{m}$ ) were obtained  
260 as shown in Equations (5-7) ( $p < 0.05$ ).

261 # Fig. 8 approximately here #

262 
$$\mu_0 = 128.16 \times \sqrt{A}/L - 0.29 \times L + 0.29 \times v + 1.37 \times Q + 30.53 \quad (0-41 \mu\text{m}, P < 0.05) \quad (5)$$

263 
$$\mu_0 = 120.00 \times \sqrt{A}/L - 0.21 \times L + 0.75 \times v + 1.27 \times Q + 56.28 \quad (0-75 \mu\text{m}, P < 0.05) \quad (6)$$

264 
$$\mu_0 = 121.79 \times \sqrt{A}/L - 0.21 \times L + 0.62 \times v + 1.29 \times Q + 62.30 \quad (0-100 \mu\text{m}, P < 0.05) \quad (7)$$

265 Where,  $\sqrt{A}/L$ , the flow path cross-sectional area opening to length; L, the channel length, mm;  
266 v, the flow velocity, m/s; and Q, the emitter flow rate, L/h.

## 267 **4. Discussion**

### 268 **4.1 Emitter self-discharge sediment mechanism**

269 It is hereby discovered that the total amount of sediment deposited inside the emitter was 0.3-  
270 1.1g when it was operated up to 640h, and the total amount of sediment entering the emitter during  
271 the operation time (the product of the outflow flow rate of the emitter and the concentration of solid  
272 suspended particles in the water source) was about 384.2-1843.2g, which means that more than 99%  
273 of sediment particles ( $< 100 \mu\text{m}$ ) was discharged out through the emitter, indicating the effectiveness  
274 of the emitter in removing sediment. The sediment discharge rate  $\varphi_e$  was between 36%-52%, this  
275 indicates that 36%-52% of the water source sediment is discharged from the drip irrigation system  
276 through the emitter, while the remaining 48%-64% sediment is discharged through the drip  
277 irrigation belt flushing or siltation in the belt. But the sediment deposition and discharge ratio  $\varphi$  (i.e.,  
278 the percentage of the sediment entering the emitter which is silted up in the emitter) was between  
279 0.01%-0.12%, and the rest of the sediment was discharged through flushing or silted up in the drip  
280 irrigation pipe. This finding also demonstrates the possibility of modifying the current conception  
281 of drip irrigation systems so that small particles of sediment can be discharged directly through the  
282 emitter rather than intercepting them through a filtration system, thereby reducing the requirement  
283 for a filtration system. Both the sediment deposition discharge ratio and emitter sediment discharge  
284 rate exhibit a rising and then falling trend with the system operation time going by. Besides, both  
285 the sediment deposition and discharge ratio  $\varphi$  and sediment discharge rate  $\varphi_e$  rise at first and fall  
286 then with system operation time. Additionally, the initial operation of the system  $\varphi$  and  $\varphi_e$  shows a  
287 rising trend due to the emitter and drip irrigation pipe sediment particles and wall collision adhesion,  
288 while the sediment surface microbial adhesion growth maybe enhances the sediment particles by

289 the adsorption force (Shen et al, 2022; Song et al, 2017; Guan et al, 2018). In the middle and late  
290 system operating stage, the emitter internal fouling increased gradually, reducing the cross-sectional  
291 area of the flow path, so that the adhering sediment particles with enhanced water flow shear force  
292 effect were gradually flushed out of the emitter (Zhou et al, 2021; Li et al, 2015), and the sediment  
293 deposition and discharge ratio  $\varphi$  and sediment discharge rate  $\varphi_e$  declined slowly. With the system  
294 operating time going by, the control threshold for particle size  $\mu_0$  showed a gradually decreasing  
295 trend, maybe because additional particle retention effect caused by previously settled particles, and  
296 large sediment particles are more likely to be wall captured and adsorbed. (Xiao et al, 2020).

297       The emitter sediment discharge rate decreases with higher water source particle sizes.  
298 Conversely, the sediment deposition discharge ratio, and the control threshold of sediment discharge  
299 particle size present an increasing trend. The reason is mainly because, at the same flow rate, larger  
300 particles could be easily settled in the pipe and water is not conveyed better within the emitter  
301 channel (Hou et al, 2022), and, consequently, the degree of emitter clogging is worsened. As more  
302 sediment is deposited, the rate at which sediment is discharged from the emitter is lowered, and  
303 therefore sediment deposition discharge ratio is increased. At the same time, given that more than  
304 99% of the sediment smaller than 100  $\mu\text{m}$  entering the emitter can be discharged from it, the  
305 sediment discharge particle size control threshold rises with an increase in the water source particle  
306 size. However, as the water source concentration decreases, the sediment discharge rate, and the  
307 control threshold of sediment discharge particle size of the emitter decrease while the sediment  
308 deposition discharge ratio increases. This is because the sediment concentration in the water source  
309 increases, and the chance of collision between the particles and between the wall and its particles  
310 increases as well, which increases the chance of adhesion between the sediment particles and the

311 emitter wall and each other (Yao et al, 2016;Wu et al, 2014), thereby exacerbating the risk of emitter  
312 clogging, and eventually leading to the decrease of the emitter sediment discharge rate and the  
313 control threshold of the sediment discharge particle size, and the increase of the sediment deposition  
314 discharge ratio.

#### 315 **4.2 Selection of the emitter self-drainage sediment capacity indicators**

316 It is hereby discovered that the variation in water source particle size has a much greater impact  
317 on discharged particle size than the variation in concentration, which is mainly because the water  
318 source particle size determines the internal particle size distribution into the emitter. At the same  
319 time, the critical threshold of discharge particle size is more influenced by the emitter flow path  
320 internal water flow rate. The fine sediment particles are conveyed better with the water flow and  
321 can be directly discharged with the water, and they are therefore less affected by the concentration.  
322 The water source particle size and water source concentration have the same degree of impact on  
323 the sediment discharge rate  $\varphi_e$ , mainly because large particles of sediment are more difficult to  
324 discharge with the water due to the increase in water source particle size. Besides, the change in the  
325 water source concentration exercises a much greater influence on the sediment deposition discharge  
326 ratio  $\varphi_e$  than that in particle size, which is primarily attributed to the poor flowing performance of  
327 coarse sediment particles with the water, and most of the particles will be deposited in the capillary  
328 internal, without flowing into the emitter. When fine sediment particles of higher concentration flow  
329 into the emitter, the probability of its collision and adhesion with the wall of the emitter channel is  
330 doubled (Zhou et al, 2021), thereby leading to the sediment accumulation.

331 Fitting analysis was conducted on the sediment self-discharge capacity of the three indicators  
332 under identical working conditions (Fig. 9). Significant linear correlations ( $p<0.05$ ) were found



333 among the sediment deposition and discharge ratio, the sediment discharge rate, and the control  
334 threshold for particle size, indicating that the trend of each indicator was consistent. In this case,  
335 any indicator can represent the relatively high or low sediment discharge capacity of the emitter.  
336 Given that the control threshold of the discharge particle size can be used to direct the control  
337 particle size of the first filtration device, it is considered the primary indicator for determining the  
338 sediment discharge capacity of the emitter.

339 # Fig. 9 approximately here #

### 340 **4.3 Emitter selection**

341 It is hereby found that, among different emitters, PCE perform better than NPCE, while among  
342 the NPCE, the NPCW emitters perform better than the NPCL emitters. The elastic diaphragm in the  
343 pressure-compensating emitter can alter the outflow path's cross-sectional area, thus making  
344 impurity particles easier to flush out under variable flow path conditions (El Bouhali et al., 2020;  
345 Wei et al., 2014), Therefore, the pressure-compensating emitters are provided with a relatively high  
346 sediment discharge capacity. However, in non-pressure compensating emitters, the flow path  
347 structure parameters are different. Besides, it is also observed that the flow path length of the emitter  
348 ( $L$ ), the ratio of the flow path cross-sectional area opening to length ( $\sqrt{A}/L$ ), section average flow  
349 velocity ( $v$ ), and rated flow rate ( $Q$ ) have a significant effect on the self-discharge sediment capacity  
350 of the emitter. The main reason is that the longer the flow path ( $L$ ) is, the sediment-discharging  
351 ability of the emitter becomes weaker, and the collision time of solid particles becomes longer.  
352 Besides, the friction with the flow path wall is larger, and it gets easier to silt in the flow path.  
353 Additionally,  $\sqrt{A}/L$  reflects the characteristics of the cross-sectional area and length of the flow  
354 path, with a larger value indicating a stronger relative sediment-carrying capacity of the internal

355 water flow. A greater  $Q$  implies a higher flow rate in the pipe lumen, a higher sediment-carrying  
356 capacity, and a better sediment discharge effect, being the shear force in the flow path higher with  
357 the increase of the average flow velocity ( $v$ ) of the section. As a result, more sediment is discharged  
358 from the emitter and less clogging material is deposited in the flow path when the sediment particles  
359 are stripped and flushed out (Feng et al., 2018; Ustun et al., 2012; Wang et al., 2009).

360 It can be seen from Fig. 8 that there is no relationship between the self-discharge sediment  
361 capacity and flow index ( $x$ ) of the emitter in this study, but some studies have proposed that the anti-  
362 clogging performance of the emitter has a relationship with the flow index ( $x$ ) because the flow  
363 index can reflect the degree of fluid turbulence in the labyrinth channel of the emitter to a certain  
364 extent (Wei et al., 2008; Zhou et al., 2019), this is mainly due to the fact that the flow indices of the  
365 different emitters are in the range of 0.50-0.53, and did not test for changes in flow indices with  
366 running time. Therefore, there is no relationship between the self-discharge sediment capacity and  
367 flow index ( $x$ ).

368 The forecast model for the control threshold of the emitter sediment discharge particle size is  
369 hereby developed as shown in Equations 5-7, which can serve as a theoretical foundation for the  
370 design of high sediment self-discharge capacity emitters and guide the initial filter equipment  
371 arrangement. However, this paper only analyzes the self-discharge capacity of a sole source using  
372 the Yellow River water, but fertilization and other factors will also have an impact on the sediment  
373 movement within driplines and emitters. To this end, differences in the self-discharge capacity of  
374 the emitters still need to be further explored under fertilized conditions.

## 375 **5. Conclusions**

376 Based on the findings of this study, the main conclusions are drawn as follows:

377 (1) The majority (>99%) of the fine particles (<100  $\mu\text{m}$ ) of sediment entering the drip irrigation  
378 emitter can be discharged through the flow path, indicating the effectiveness of the emitter in  
379 removing sediment. Among them, 36%-52% of the water source sediment is discharged from the  
380 drip irrigation system through the emitter, while the remaining 48%-64% sediment is discharged  
381 through the drip irrigation belt flushing or siltation in the belt.

382 (2) Under the same flow conditions, PCE had higher  $\mu_0$  than NPCE. Overall,  $\mu_0$  of PCE was  
383 improved by 1.4%-21.3% compared with the NPCL emitters, and it was 0.2%-7.61% when  
384 compared with the NPCW emitters. Among NPCE, the  $\mu_0$  of the NPCW emitters was larger than  
385 that of the NPCL, with an average improvement rate of 0.9%-14.2%.

386 (3) The self-discharge sediment capacity of NPCE was mainly affected by the emitter flow  
387 path length (L) and the ratio of the flow path cross-sectional area open square to length ( $\sqrt{A}/L$ ). The  
388 SDC of the emitter can be improved by enhancing the average flow velocity of the section (v) and  
389 rated flow rate (Q).

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## 393 **Compliance with ethical standards**

394 Conflict of interest: On behalf of all authors, the corresponding author states that there is no  
395 conflict of interest.

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499



## Captions for figures involved in this paper

500

501 **Fig. 1** Layout of the experimental system.

502 **Fig. 2** Structure of different drip irrigation emitters tested.

503 **Fig. 3** Control threshold for the particle size of the high-sediment water.

504 **Fig. 4** Average discharge variation rate ( $D_{ra}$ ).

505 **Fig. 5** Control threshold for particle size ( $\mu_0$ ).

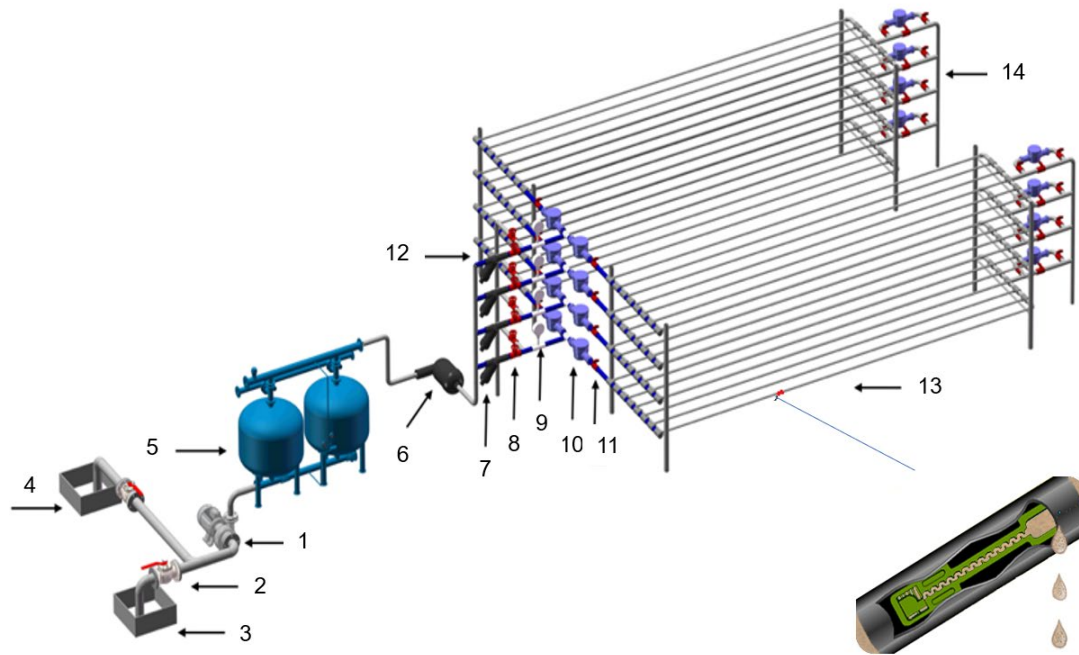
506 **Fig. 6** Sediment discharge rate ( $\varphi_e$ ).

507 **Fig. 7** Sediment deposition and discharge ratio ( $\varphi$ ).

508 **Fig. 8** Correlation between indicators of emitter self-discharge sediment capacity and

509 structural parameters.

510 **Fig. 9** Emitter self-discharge sediment indicator selection.



511

512 **Fig. 1. Layout of the experimental system.** The experimental setup is consistent with Muhammad

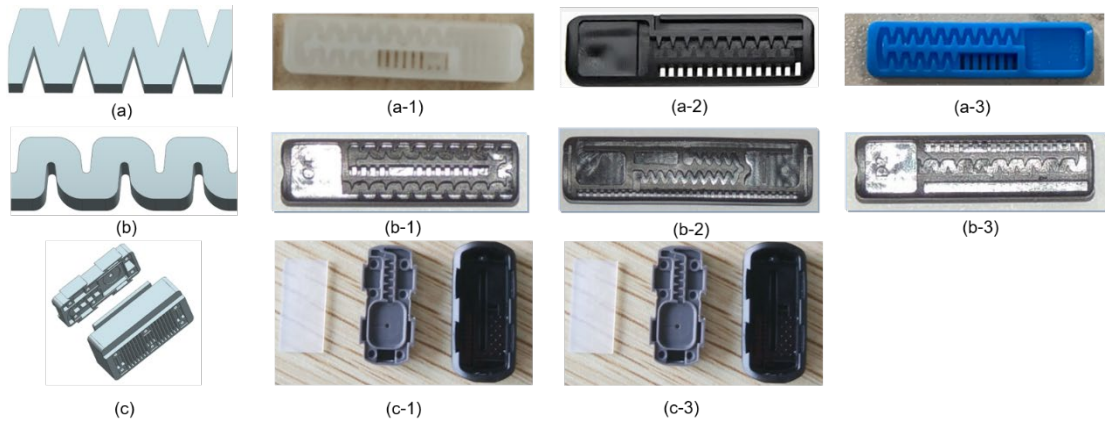
513 et al. (2021), 1. Water pump; 2. Butterfly valve; 3, 4. Reservoir; 5. Sand filter; 6. Disc filter (100

514 mesh); 7. Small disc filter (100 mesh); 8, 11. Fine adjustment valve; 9. Pressure gauge; 10. Water

515 meter; 12. Return pipe; 13. Drip irrigation pipe; 14. Flushing device

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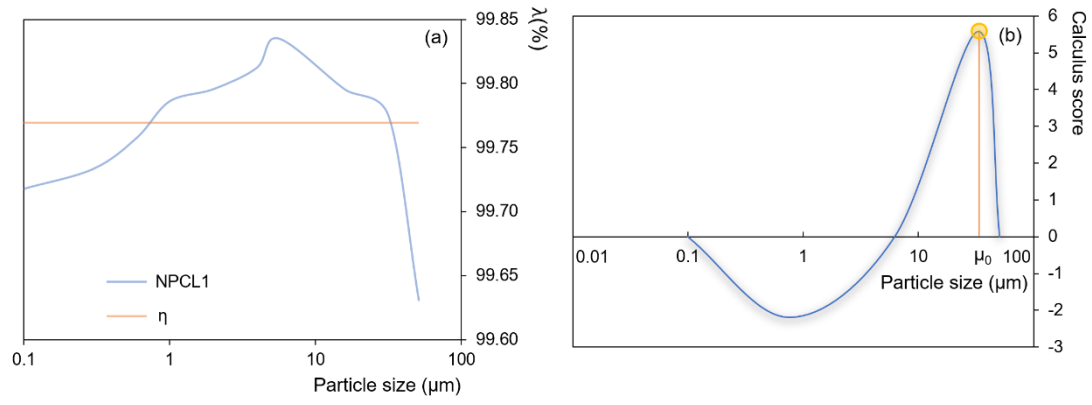


518

519 **Fig. 2. Structure of the different emitters tested.** (a) NPCL structure, (a-1) NPCL1, (a-2) NPCL2, (a-3)

520 NPCL3, (b) NPCW structure, (b-1) NPCW1, (b-2) NPCW2, (b-3) NPCW3, (c) PC structure, (c-1) PC1, (c-2) PC2.

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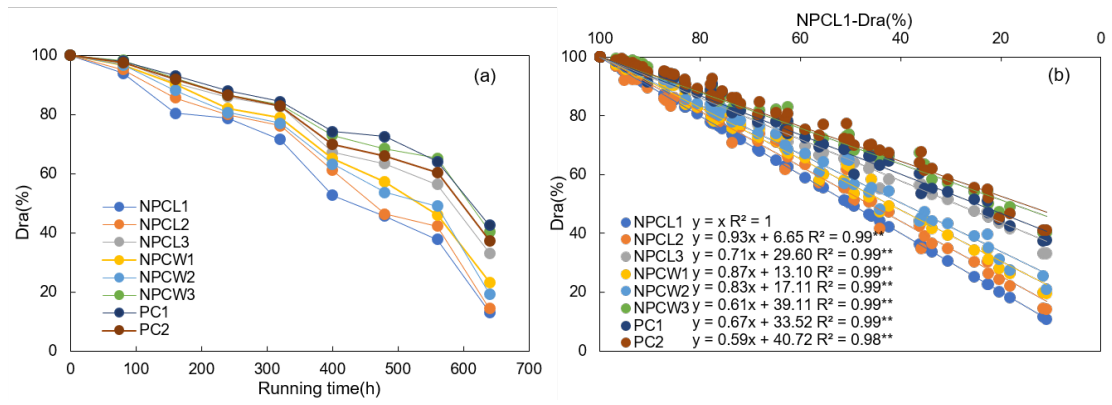


522

523 **Fig. 3. Control threshold for particle size,** (a) the distribution curve  $\lambda$ ,  $\eta$  is total sand discharge,

524 (b) Integrating the difference between  $\lambda$  and  $\eta$ ,  $\mu_0$  is control threshold for particle size.

525



526

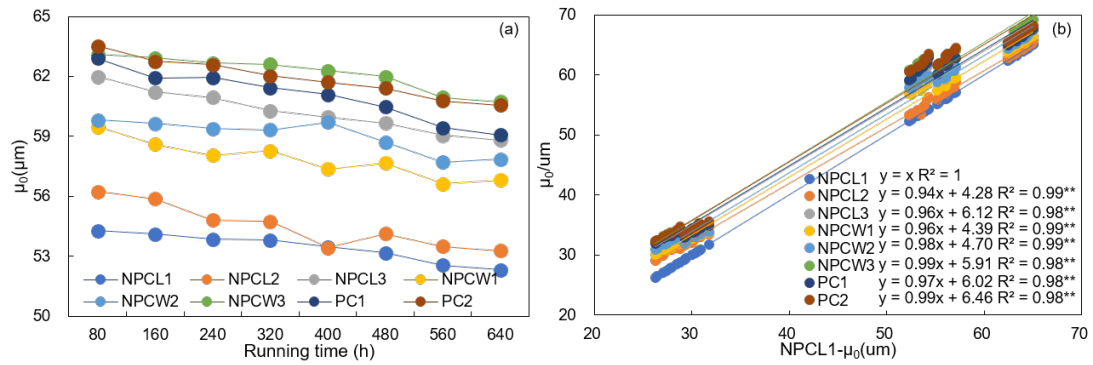
527 **Fig. 4. Average discharge variation rate (Dra).** Evolution of average discharge variation rate (Dra)

528 under the sediment diameter of 0-75  $\mu\text{m}$  and sediment concentration of 3.0 g/L is shown in (a), while

529 the rest of the working conditions are shown in the Supplementary Material Fig. S1. Regression

530 analysis of Dra for each type of emitters regarding of NPCL1 is shown in (b), and **\*\*** represents

531 significant level  $p < 0.01$ .



532

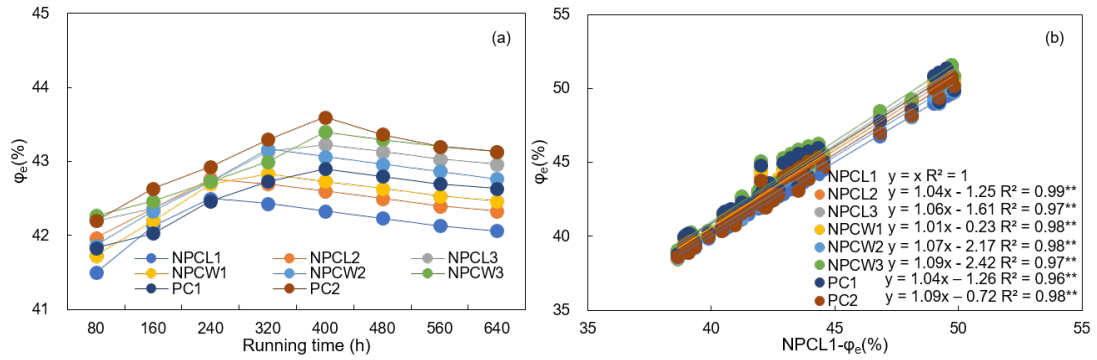
533 **Fig. 5. Control threshold for particle size ( $\mu_0$ ).** Evolution of the control threshold for particle size

534 ( $\mu_0$ ) under the sediment diameter of 0-75  $\mu\text{m}$  and sediment concentration of 3.0 g/L is shown in (a),

535 while the rest of the working conditions are shown in the Supplementary Material Fig. S3.

536 Regression analysis of  $\mu_0$  for each type of emitters regarding of NPCL1 is shown in (b), and **\*\***

537 represents significant level  $p < 0.01$ .



538

539 Fig. 6. Sediment discharge rate ( $\phi_e$ ). Evolution of the sediment discharge rate ( $\phi_e$ ) under the

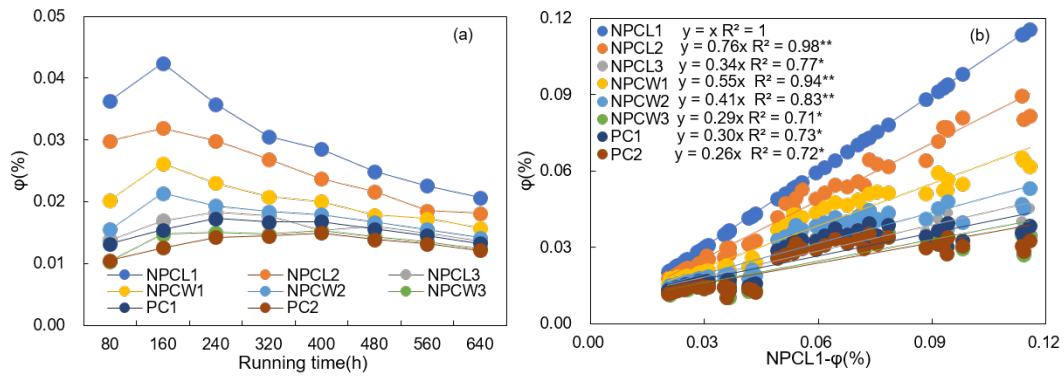
540 sediment diameter of 0-75  $\mu\text{m}$  and sediment concentration of 3.0 g/L is shown in (a), while the

541 rest of the working conditions are shown in the Supplementary Material Fig. S4. Regression

542 analysis of  $\mu_0$  for each type of emitters regarding of NPCL1 is shown in (b), and **\*\*** represents

543 significant level  $p < 0.01$ .

544



545

546 **Fig. 7. Sediment deposition and discharge ratio ( $\phi$ ).** Evolution of the sediment deposition and

547 discharge ratio ( $\phi$ ) under the sediment diameter of 0-75  $\mu\text{m}$  and sediment concentration of 3.0 g/L

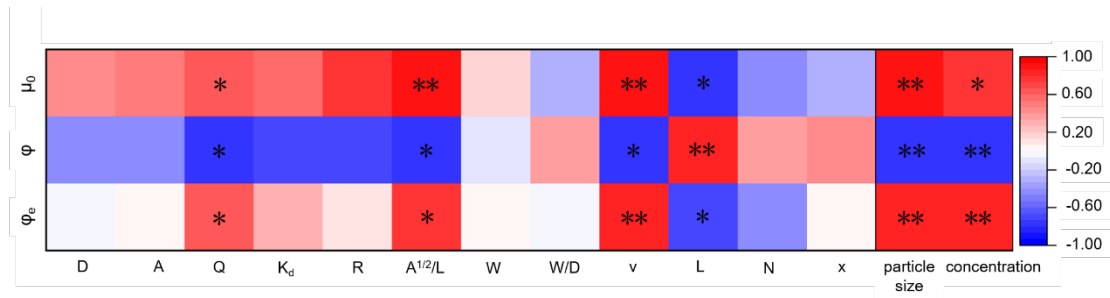
548 is shown in (a), while the rest of the working conditions are shown in the Supplementary Material

549 Fig. S5. Regression analysis of  $\mu_0$  for each type of emitters regarding of NPCL1 is shown in (b),

550 and **\*\*** represents significant level  $p < 0.01$ .

551





552

553 **Fig. 8 Correlation between indicators of emitter self-discharge sediment capacity and**

554 **structural parameters. L, W, D represents flow path length, width and channel depth, respectively,**

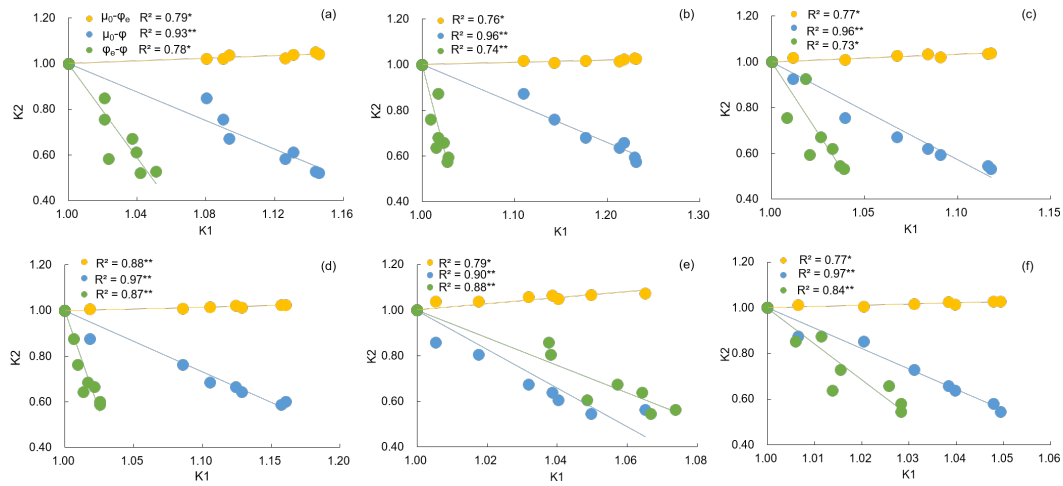
555 **mm; A represents cross-sectional area of channel, mm<sup>2</sup>; Q represents emitter flow rate, L/h;  $K_d$**

556 **represents flow rate coefficient; R represents channel wetted perimeter, (mm) ; v represents flow**

557 **velocity, (m/s) ; N represents number of channel units; x represents flow index. \*\* represents  $p$**

558 **< 0.01, and \* represents  $p < 0.05$ .**

559



560

561 **Fig. 9. Emitter self-discharge sediment indicator selection.** K1 and K2 are the index ( $\mu_0$ ,  $\varphi$ ,  $\varphi_e$ )

562 ratio of different emitters to NPCL1 emitter. (a-f) are the results under the working conditions of 0-

563 41  $\mu\text{m}$  and 1.0 g/L, 0-41  $\mu\text{m}$  and 3.0 g/L, 0-75  $\mu\text{m}$  and 1.0 g/L, 0-75  $\mu\text{m}$  and 3.0 g/L, 0-100  $\mu\text{m}$  and

564 1.0 g/L, 0-100 $\mu\text{m}$  and 3.0 g/L, respectively.

565

566

567

**Table 1 Characteristics of drip irrigation emitters applied**

No.	Flow rate (L/h)	flow rate coefficient	flow index	channel wetted perimeter	flow velocity	number of channel units	Geometrical parameters of the flow path			Wall thickness (mm)	Manufacturer location	Abbreviation
							Length (mm)	Width (mm)	Depth (mm)			
1	1.0	3.39	0.53	3.33	0.25	9	47.13	0.91	1.21	0.20	China	NPCL1
2	1.4	4.64	0.52	2.17	0.68	9	35.52	0.89	0.64	0.20	China	NPCL2
3	1.6	5.06	0.5	1.98	0.93	14	22.83	0.82	0.58	0.20	Israel	NPCL3
4	1.0	3.16	0.5	2.16	0.54	18	40.36	0.72	0.72	0.15	China	NPCW1
5	1.4	4.74	0.53	2.17	0.76	14	37.79	0.69	0.74	0.15	China	NPCW2
6	1.6	5.3	0.52	1.96	1.54	9	23.50	0.36	0.80	0.15	China	NPCW3
7	1.0	1.05	0.02	3.05	0.32	5	14.42	0.77	1.14	0.38	Israel	PC1
8	1.6	1.68	0.02	2.65	0.63	5	18.17	0.73	0.96	0.38	Israel	PC2

568

Note: PC is pressure compensating emitter, NPCL is non-pressure compensating emitters (NPC) with toothed flow path, NPCW is non-pressure compensating emitters with vortex wash wall optimized.

569