

1 1 **Horizontal Roughing Filter for Reducing Emitter Composite Clogging in Drip**
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4 2 **Irrigation Systems Using high sediment water**

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10 **Abstract:** Composite clogging substance is an inevitable issue in irrigation systems that use high-
11 sediment water (HSW), consequently leading to emitter clogging, which may damage the whole
12 irrigation system. So far, settling tanks allow particle deposition before water is applied in the drip
13 irrigation systems, so they reduce particle load and therefore clogging risk is reduced. However,
14 these tanks do not always perform properly, particularly when controlling bioclogging and organic
15 matter clogging. This study proposed using a Horizontal Roughing Filter (HRF) to relieve
16 composite clogging in irrigation systems using HSW. Results revealed that HRF reduced Sediment
17 concentration (SC), Chemical Oxygen Demand (COD_{cr}), Total Organic Carbon (TOC), and
18 Biochemical oxygen demand (BOD₅) by 73.6-89.6%, 8.1-62.2%, 15.3-51.8%, and 22.8-53.1%,
19 respectively. In addition, compared with control treatment (CK), HRF decreased the clogging
20 substance of lateral and emitter by 32.4-37.6% and 25.5-29.4%, respectively, which obviously
21 alleviated the risk of emitter clogging. Finally, compared with CK, HRF increased the Christiansen
22 of Uniformity (CU) of drip irrigation system and average discharge variation ratio (Dra) 9.2-27.1%
23 and 12.3-22.5%. Moreover, the filter performance of HRF under medium thickness of 60 cm was
24 obviously higher than those with thicknesses of 20 cm and 40 m, only slightly lower than those with
25 thicknesses of 80 cm. The results demonstrated that HRF is an effective filtration treatment with
26 great potential applications for controlling the composite clogging in irrigation systems using high-
27 sediment water.

28 **Keywords:** bioclogging; clogging; filtration; micro irrigation; emitter

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1. Introduction

The shortage of freshwater resources has become one of the key factors threatening global food security and sustainable development of human society (Melo et al., 2020; Xu et al. 2020). The application of high sediment water (HSW) for agricultural irrigation in arid areas (e.g., India, China, Egypt, Sudan, Pakistan) is a potential mean to alleviate local crisis of fresh water resources (Ali and Mohammed, 2015; Khattak et al., 2011; Ren et al., 2021). Drip irrigation has been reported to be an efficient agricultural water-saving irrigation technology (Oker et al., 2020; Soliman et al., 2020). However, HSW contains suspended solid particles which inevitably foul and clog emitters and therefore reduce the irrigation uniformity, and shorten the operation life of the drip irrigation systems (Li et al., 2019b; Liu et al., 2019).

Irrigation water with high particle load will quickly overburden screen, disc and media filters, which are frequently used in drip irrigation systems (Nakayama et al., 2007). In this case, large settling tanks are common methods to remove suspended particles from water (Bajcar et al., 2011; Kadewa et al., 2010). Wang et al. (2020a) reported that the sediment removal efficiency of inclined-tube gravity sedimentation tank reaches 64.7 – 69.7%. Goula et al. (2008) found that adding a vertical baffle at the feed section of sedimentation tank led to suspended particles removal efficiency reaching 90.4 - 98.6%. These studies brought valuable insights into the solids removal ability of settling tank. However, HSW not only contains suspended particles, but also contains a high quantity of microorganisms and organic matter (resulting from industrial waste and agricultural pollution), which is easy to cause composite emitter clogging (Zhou et al., 2019a; Zhou et al., 2019b). The traditional settling tanks have low removal efficiency for microorganisms and organic matter present in HSW, and, therefore, it is difficult to inhibit the formation of biologging in the drip irrigation

1 53 system. Thus, the development of effective control for the mitigation of clogging in HWS drip
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3 54 irrigation system is in urgent need .
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6 55 Horizontal Roughing Filter (HRF) has attracted extensive interest in water treatment field,
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8 56 due to its characteristics of high efficiency, low cost, simple layout, low energy consumption, and
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10 57 easy operation (Bakare et al., 2019; Zeng et al., 2020). Anh et al. (2020) found that turbidity removal
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12 58 rate of HRF reaches 79-85%. Nkwonta (2010) strongly supported that HRF suspended solid removal
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14 59 was less than 50% for particle sizes of 5-10 μm and almost 100% for particle sizes of 50 - 100 μm .
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17 60 In addition, Nkwonta (2010) pointed out that HRF could effectively remove microorganisms and
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20 61 organic matter from water. Khazaeni et al. (2016) indicated that HRF removed the total nitrogen, total
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22 62 phosphorous, and COD_{Cr} by 50%, 54%, 68%, respectively. Adlan et al. (2008) indicated that HRF
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25 63 reduced the BOD₅ and coliform organisms content by 51% - 67% and 67% - 96%, respectively.
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28 64 Therefore, HRF is expected to constitute an effective method to control composite clogging in drip
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31 65 irrigation systems using HSW. However, the role of HRF is often used as the pretreatment of slow
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34 66 sand filter (Mushila et al., 2016; Rooklidge 2006). The use of HRF to control fouling is rather a new
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37 67 research area. Particularly, the controlling capacities of HRF on composite clogging in drip
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40 68 irrigation systems using HSW remain unknown.
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44 69 Thus, the objectives of this study were to: (i) reveal the effect of HRF on the water quality
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47 70 parameters of HSW (ii) evaluate the effect of medium different layer thickness on filter performance
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50 71 (iii) determine whether HRF would effectively control the composite clogging in drip irrigation
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53 72 systems using HSW; (iiii) elucidate the inhibition mechanism of HRF on composite clogging in drip
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56 73 irrigation systems using HSW.
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58 74 **2. Materials and methods**

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75 2.1 Experimental setup

76 The testing system was an outdoor-drip irrigation test platform (Fig. 1). The platform resembles
77 drip irrigation system, having four layers of drip irrigation laterals stacked horizontally. Each layer
78 had the same type of emitter. A total of eight types of emitters were installed , being their structural
79 parameters shown in Table. 2. The HSW used in the experiment was collected from the Yellow
80 River (located in northern Wulan Buh, Dengkou County, Bayan Nur City, Inner Mongolia, China).
81 The HSW was filtered with HRF or gravity desilting filter (CK), and then was conveyed into the
82 drip irrigation test platform. The complete experiment was lasted for a total of 90 days.

83 #Fig. 1 approximately here#

84 #Table. 1 approximately here#

85 #Table. 2 approximately here#

86 2.2 Experimental treatments

87 The experimental treatment is HRF (Fig S1), which comprised of peripheral filtering layers
88 and an internal water storage tank. Filtering layers were made with three media layers having a
89 thickness of 30 cm, from outside to inside and the layers were separated from each other by 550 μ
90 m steel mesh. These layers were filled up three different sized silica sand media i.e., 10-12 mm
91 (coarse gravel), 6-8 mm (normal gravel) and 2-4 mm (fine gravel). The internal water storage tank
92 was surrounded by filter media layer, and the bottom of the tank was sealed by steel plate. During
93 the experimental operation, HRF was placed in the HSW. Under the action of water pressure, the
94 HSW was filtered by the coarse layer, normal layer and fine layer of HRF in turn and then entered
95 into the internal water storage tank. Filtered water was pumped into the fouling cultivation platform.

96 Desilting basin (CK) was used as a control treatment. The CK was composed of inlet tank,

1 97 flow regulating plate, desilting tank pool, diversion wall, sloped tube, filter screen (150 μ m) ,
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3 98 clear water tank and fouling tank (Fig S2). HSW entered the inlet tank through the pipeline, being
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6 99 regulated by the flow adjustment board. The coarse particle settled on the bottom of the pool, while
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9 100 the HSW passed through the filter mesh, thereby entering the clear water tank. Finally, the water
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12 101 was supplied to the drip irrigation system.

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14 102 The filtration capacity of sand filter is also tested (Fig S3). The sand filter had two filtering
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17 103 layers with 2-4 and 6-8 mm media size, respectively. The operational details of the sand filter were:
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20 104 filtration cross section, 1400 cm²; inlet and outlet diameter (mm), 50mm; manufacturer, Henan
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23 105 kaiburui, China.

24 25 106 **2.3 Water quality parameters**

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27 107 Four replicated samples were taken simultaneously from raw water, HRF outlet and CK outlet.
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30 108 every 4.5 days. In addition, quadruplicated samples were also collected at filter layer thicknesses of
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33 109 20, 40, 60, 80 and 90 cm, respectively, at 36, 54 and 72 days. In order to compare the filtration
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36 110 capacity of HRF and sand filter, we supplemented the test of sand filter. Four replicated samples
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39 111 were also taken simultaneously from raw water and sand filter outlet, at 5, 10 and 15 days. These
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42 112 samples allowed determining SC (Sediment Concentration), BOD₅ (Biochemical Oxygen Demand),
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45 113 COD_{Cr} (Chemical Oxygen Demand) and TOC (Total Organic Carbon). SC was tested with the
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48 114 pycnometer Test Method according to GB/T 50159 – 2015. BOD₅ was tested using a BOD meter
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51 115 (Hach, US, rak® II) according to HJ/T 86-2002. Chemical Oxygen Deman (COD_{Cr}) was analyzed
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54 116 using a COD meter (Zhongke, China, type: MI-200K) according to SNI 06-6989.15-2006. TOC was
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57 117 measured with a TOC meter (Manufacturer: Daojing, China; type: 4100) according to GB 13193-
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61 119 **2.4 Extraction and testing of clogging substance in laterals and emitters**

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1 120 During the experiment, laterals and emitters samples in each treatment were collected total of
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3 121 nine times. At each sampling event, 18 emitters were randomly collected from irrigation laterals
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6 122 (i.e., 6 at the head, 6 at the middle and 6 at the tail). The length of the lateral is 15 m. To represent
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9 123 the whole laterals, the samples were collected in each section of lateral inlet, middle and tail parts.
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11 124 The length of laterals sample from each part of lateral was 30 cm. The laterals and emitters samples
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14 125 were placed in zip lock plastic bags and stored in refrigerator at 4 °C.
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17 126 The emitter samples were weighed using a high-precision electronic balance (manufacturer:
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19 127 Wangtai, type: FA-G; accuracy: 10^{-3} g). Hereafter, the emitter samples were put in an ultrasonic
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22 128 cleaning bath (manufacturer: Chaowei, China; type: GVS-10 L; working power: 240 W; frequency:
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25 129 60 Hz) for 60 min to remove the clogging substance, and then the samples were dried at 100°C until
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28 130 they acquired a constant weight. The difference between the weights was the weight of clogging
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31 131 substances on emitter. The same test method was applied in laterals clogging substances
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33 132 **2.5 Particle size distribution testing**

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36 133 The particle size was analyzed by using a laser particle sizer (Malvern Instruments Ltd.,
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38 134 Mastersizer 3000). The raw water, HRF and CK outlet water, laterals and emitter clogging substance
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41 135 samples were taken every 100 h. The stirrer speed of laser particle size analyzer was 2500 rpm, and
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44 136 the shading range was 10% ~ 20%. In order to describe the distribution characteristics of particle
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47 137 size, clay ($d \leq 2\mu\text{m}$), silt ($2\mu\text{m} \leq d \leq 50\mu\text{m}$) and sand ($d \geq 50\mu\text{m}$) were classified according to the
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50 138 U.S. Department of Agriculture particle size classification (Li et al., 2019a). D_5 and D_{50} were the
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53 139 corresponding particle sizes when the cumulative particle size distribution ratio reaches 5% and
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55 140 50%, respectively.
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57 141 **2.6 Evaluation of drip irrigation system performance**

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60 142 Along with operation time, the growth of clogging substance would gradually clog the emitters
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1 143 of the drip irrigation system. The average discharge variation ratio (Dra) and Christiansen
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3 144 coefficient of uniformity (CU) were used to evaluate the flow performance of the drip irrigation
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6 145 system. The detailed calculation method of Dra and CU is explained in supplementary material
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10 11 147 **2.7 Statistical analysis**

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14 148 The experimental data basic calculations were done with Microsoft Excel; and statistical
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16 149 analysis was carried out using SPSS (ver. 22.0 IBM, USA). Pearson correlation coefficient was
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19 150 applied to determine the correlation of fouling content among different groups (p adjusted <0.05).
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22 151 Structural equation modelling analysis (SEM) was performed using SPSS AMOS v.24 (AMOS,
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25 152 IBM, USA) to analyze the direct and indirect relationships among HRF, dry weight, and the flow
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28 153 performances of drip irrigation system (Dra).

29 30 154 **3 Results**

31 32 33 155 **3.1 Effect of HRF on water quality parameters**

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36 156 HRF reduced SC, COD_{cr}, TOC, and BOD₅ of HSW by 73.6-89.6%, 8.1-62.2%, 15.3-51.8%,
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38 157 22.8-53.1% ([Fig. 2](#)), respectively. Comparing with CK, HRF greater decreased SC, COD_{cr}, TOC,
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41 158 and BOD₅ by 8.9-25.9%, 6.34-54.1%, 4.1-44.4%, and 9.6-44.6%, respectively. The HRF treatment
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44 159 had better effects on D₅ and D₅₀ of particle size than the CK treatment. Compared with CK, HRF
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47 160 reduced D₅ and D₅₀ by 0.1-2.1 μ m and 2.2-15.6 μ m, respectively. Moreover, the sediment removal
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50 161 capacity of HRF was further improved after 36 days of operation and reached its maximum value
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53 162 at 72 days.

#Fig. 2 approximately here#

3.2 Effect of HRF layer thickness on water quality

The effect of HRF layer thickness on removals of SC, BOD₅, COD_{Cr} and TOC is shown in Fig. 3. The results show that SC, BOD₅, COD_{Cr} and TOC decreased with the increase of filter thickness. However, no linear decrease was observed. The values of SC, BOD₅, COD_{Cr} and TOC showed a gradual decline when the HRF layer thickness was lower than 60 cm. Compared with removal efficiency with filter thickness of 20 cm, filtration capacity of 40 cm filter layer was slightly improved, and the removal efficiency of SC, COD_{Cr}, TOC and BOD₅ was increased by 12.5-19.3%, 3.2-4.7%, 4.1-7.1%, 1.9-5.3%. However, the filtration performance was obviously increased when the filter layer thickness reached 60 cm.. Compared with the removal efficiency with the thickness of 40 cm, removal efficiency of 60 cm filter layer was obviously improved, and the removal efficiency of SC, COD_{Cr}, TOC and BOD₅ was increased by 35.4-51.2%, 18.9-27.8%, 10.3-20.8%, 17.5-29.9%. However, the removal efficiency of HRF with thickness of 80 cm were increased slightly compared with thickness of 60 cm and the removal efficiency of SC, COD_{Cr}, TOC and BOD₅ was only increased by 5.3-9.6%, 1.6-5.1%, 3.5-8.3%, 1.9-4.2%.

#Fig. 3 approximately here#

3.3 Effect of HRF on composite clogging substance in lateral and emitter

The dynamic change of composite clogging substance (Fig. 4,5) shows that HRF controlled the contents of composite clogging substance within laterals and emitters. Compared with CK, HRF significantly ($p < 0.05$, Table S1) decreased the composite clogging substance of lateral and emitter by 32.4-37.6% and 25.5-29.4%, respectively, which obviously alleviated the risk of emitter clogging. Moreover, HRF treatments had higher control efficiencies of clay, silt and sand contents in laterals

185 and emitter than CK. Compared with CK treatment, HRF significantly ($p < 0.01$, Table S1) decreased
186 the contents of silt, sand and clay in laterals by 23.1-27.4%, 31.8-39.5% and 27.6-39.8%,
187 respectively, and significantly ($p < 0.05$, Table S1) decreased the contents of silt, sand and clay in
188 emitter by 24.8-27.4%, 19.3-26.4%、38.1-42.9%.

#Fig. 4 approximately here#

190 3.4 Influence path of HRF on composite clogging substance in drip irrigation systems

191 SEM was used to further reveal the influence path of HRF on composite clogging substance in
192 drip irrigation systems (Fig.6). The fitted model ($\chi^2/df=1.76$, $p=0.052$) met the significance criteria.
193 SEMA revealed that HRF presented strongest correlations ($\beta = 0.74, 0.66, 0.54, 0.51$; $p < 0.01$) with
194 CS, COD, BOD₅ and TOC. Moreover, SEMA also further showed that water quality parameters (CS,
195 COD, BOD₅, TOC) were significantly correlated ($p < 0.05$) with dry weight of laterals (LDW) and
196 emitters (EDW). In addition, the results showed that there were synergistic interactions between
197 LDW and EDW. Finally, EDW directly affected Dra of the drip irrigation system.

#Fig. 5 approximately here#

200 4. Discussion

201 4.1 Filtration mechanism of HRF on high sediment water

202 Desilting basin represents an effective means to remove coarse suspended particles from HSW
203 (Lak et al., 2020). However, due to that fine suspended particles are not always easy to settle (Ma
204 et al., 2019), the removal efficiency of these fine particles in the desilting basin is poor. Therefore,
205 it is necessary to develop a filtration technology which allows removing those fine sediment
206 particles for preventing emitter clogging in drip irrigation system. This study found that HRF can

1 207 effectively remove the fine sediment particles in HSW (Fig 2). One possible reason is that the filter
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3 208 media of HRF has both the functions of mechanical screening and contact flocculation (Mackiewicz
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6 209 1983, Wang et al. 2020c). When the HSW reaches the surface of the filter layer, the filter medium
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9 210 uses its screening function to remove the large size sediment particles from HSW (Egemose 2018).
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11 211 Then, HSW flows into the filter layer that could adsorb the fine particles relying on electric double-
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14 212 layer power, van der Waals forces and chemical bonds (Chen et al., 2019). Moreover, due to the
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17 213 lower filtration rate of HRF, the residence time of HSW in the filter layer became longer, which
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20 214 directly increased the chance of collision and adsorption between filter media and fine particles
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22 215 (Nkwonta 2010), and further improved removal capacity of HRF for fine particles. On the other
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25 216 hand, with the increase of HRF operation time, the filter medium is wrapped by microorganisms.
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28 217 These microorganisms will secrete viscous substances and adsorb fine particles from the water
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31 218 (Rooklidge et al., 2002), which also greatly improves HRF's filtration capacity for fine particles. In
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34 219 addition, it is found that the sediment removal capacity of HRF will be improved after 36 days of
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37 220 operation. The reason may be that the microorganisms in the filter media will gradually form biofilm
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40 221 after 36 day of operation, and mature biofilm will be formed after 72 day of operation. Therefore,
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42 222 HRF also reaches the maximum sediment removal capacity after 72 day of operation.

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44 223 This study also found that HRF effectively reduced CS, BOD₅, COD and TOC in HSW (Fig
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47 224 2). The reason may be that with the increase of HRF operation time, microorganisms adhered to the
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50 225 filter media gradually grow into mature biofilm, which will capture organic matter and
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53 226 microorganisms from the water as nutrients for growth and reproduction (Hashimoto et al., 2019).
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56 227 Finally, HRF can remove microorganisms and organic matter from the water by the predation,
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59 228 scavenging, adsorption and bio-oxidation of microorganisms adhering to the filter media. Moreover,
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1 229 this paper also found that the filtration capacity of HRF under the thickness of 60 cm was higher
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3 230 than that with 20 cm and 40 cm. The reason is that the HRF under 0-30 cm and 30-60 cm filter
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6 231 layers were filled with coarse gravel media and normal gravel media, respectively (Fig 1). Due to
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9 232 the large gap of the filter media, it is difficult to remove fine particles, microorganisms and organic
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12 233 matter by mechanical screening (Khiari et al., 2020), while the filter media with large particle sizes
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15 234 did not favor biofilm growth (Wang et al., 2014). Thus, HRF under 0-30 cm and 30-60 cm filter
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18 235 layers only could rely on a small number of microorganisms on the surface of the filter media to
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21 236 remove fine particles, microorganisms and organic matter. However, the HRF under 60-90 cm filter
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24 237 layers were filled with fine gravel media with small gap, so it was easy to form biofilm on the
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27 238 surface of the filter media (de Oliveira and Schneider 2019).

28 239 **4.2 Effect of HRF on composite clogging substance in drip irrigation system**

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31 240 This study further found that HRF could reduce the risk of clogging of emitters. Compared
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34 241 with CK treatment, HRF reduced the clogging substance of emitters by 25.5-29.4%. The reason is
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37 242 that HRF treatment has better water treatment capacity than CK treatment, and therefore greatly
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40 243 reduced the content of fine sediment particles, microorganisms and organic matter in HSW. At the
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43 244 same time, the water quality parameters are directly related to the clogging substance of emitter
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46 245 (Bucks et al., 1979). Thus, HRF directly reduces the content of composite clogging substance
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49 246 formation in the emitter of drip irrigation systems by improving the water quality. On the other hand,
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52 247 some scholars reported that there was a significant correlation between clogging substance of
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55 248 laterals and emitter (Han et al., 2018; Li et al., 2015). Therefore, HRF could also decrease the
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58 249 clogging substance of laterals by affecting the water quality, thereby reducing the risk of particles
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61 250 settled on laterals entering the emitter, and indirectly affect the content of clogging substance of
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1 251 emitter. Moreover, HRF has better removal ability of microorganisms and organic matter than CK,
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3 252 and microorganisms were easy to adsorb particles and organic matter in the emitter to form large
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6 253 particle size clogging substance (Feng et al., 2019). Therefore, HRF can reduce the formation of
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9 254 large size particle clogging substance in the emitter through water quality control. Compared with
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11 255 CK treatment, the content of sand in the clogging substances was reduced by 19.3-26.4%. In this
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14 256 sense, HRF directly affected the CU and Dra of drip irrigation system by reducing the formation of
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17 257 emitter clogging. Compared with CK, HRF increased the Christiansen of Uniformity (CU) and
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20 258 average discharge variation ratio (Dra) of drip irrigation system by 9.2-27.1% and 12.3-22.5% (Fig
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25 260 **4.3 Engineering implications of HRF**

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28 261 Although the results proved that HRF effectively controlled the composite clogging in drip
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31 262 irrigation system, it is necessary to evaluate the engineering implications of the results for its
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34 263 successful application of HRF. Desilting basin is the most common method for controlling clogging
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37 264 in HSW drip irrigation systems(Wang et al., 2020b), compared with HRF in terms of filtration
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40 265 performance, costs, and safety using similar testing devices. In addition, HRF treatment can remove
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43 266 not only bacteria, and pathogenic microorganisms, but also synthetic organic matter, natural organic
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46 267 matter, humus and heavy metal ions (Dalahmeh et al., 2019; Dashti et al., 2019; Jiang and Tay,
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49 268 2010), avoiding pollutants in water entering into soil through agricultural irrigation. Moreover,
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52 269 capital cost is another major factor closely related with the successful implications of methods.
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55 270 Because of its simple structure and modularization, HRF has low initial cost and no additional
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58 271 operating costs are needed (Zahiruddin and Rahimuddin, 2011). Besides, we also compared the
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61 272 capacity, rate and efficiency of sand filter with HRF. This part is shown in s shown in supplementary
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1 273 material, section 3. The results show that the removal capacity of HRF for CS, COD, BOD₅ and
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3 274 TOC is significantly higher than that of sand filter (Fig.S4). The HRF has relatively lower
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6 275 installation cost than sand filter (Fig.S5). And, the filtration rate of HRF was also lower than sand
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9 276 filter. Hence, the HRF could be more suitable for small scale agricultural irrigation systems (Fig.S5).
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11 277 Based on these results, the HRF is a promising method of clogging substance control in agricultural
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14 278 drip irrigation system.

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17 279 In addition, HRF can be used in high salinity seawater, reclaimed water, surface lake water and
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20 280 deep groundwater (Khazaei et al., 2016; Kim et al., 2020; van Afferden et al., 2011). HRF has been
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23 281 used in many fields, such as the pretreatment of slow filtration in drinking water engineering
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25 282 (Dastanaie et al., 2007), the treatment of wastewater in industrial field (Khazaei et al. 2015), and
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28 283 the pretreatment of ultrafiltration membrane in seawater desalination field (Naidu et al., 2013).
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31 284 However, HRF filtration rate is slow, suitable for small farmers with small agricultural area and
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34 285 small water demand, and it is best used with water-saving irrigation technology. In addition, other
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36 286 multiple factors are involved which obviously affect the HRF. At present, there is a lack of
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39 287 quantitative relationship between filter layer thickness, filter material, filtration rate and filtration
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42 288 flow and filtration capacity. It is suggested that HRF performance test with different structural
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45 289 parameters should be carried out in the future under different water quality conditions, so as to
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48 290 provide theoretical reference for obtaining the most suitable configuration conditions, engineering
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51 291 design method and optimized operation mode of HRF.

52 292 **5 Conclusions**

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56 293 (1) Horizontal roughing filter (HRF) reduced SC, COD, TOC, and BOD₅ regarding high
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59 294 sediment water (HSW) by 73.6-89.6%, 8.1-62.2%, 15.3-51.8%, and 22.8-53.1%,
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1 295 respectively.

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4 296 (2) Compared with desilting filter (CK), HRF decreased the clogging substance of laterals
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6 297 and emitters by 32.4-37.6% and 25.5-29.4% respectively, which obviously alleviated the
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9 298 risk of emitter clogging.

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11 299 (3) The filtration performance of HRF under the thickness of 60 cm was obvious higher than
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14 300 that under the thickness of 20 cm and 40 cm.

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16 301 **Acknowledgements**

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Captions for Figures and Tables in the Paper

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3 457 Fig. 1 Layout of experiments system

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6 458 Fig. 2 Effects of HRF on water quality parameters

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9 459 Fig. 3 Effect of filter layer thickness on the water quality parameters

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11 460 Fig. 4 Effects of HRF on clogging substances in laterals of drip irrigation system

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14 461 Fig. 5 Effects of HRF on clogging substances in emitter of drip irrigation system

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17 462 Fig. 6 Controlling pathway of HRF on composite clogging substance in drip irrigation system

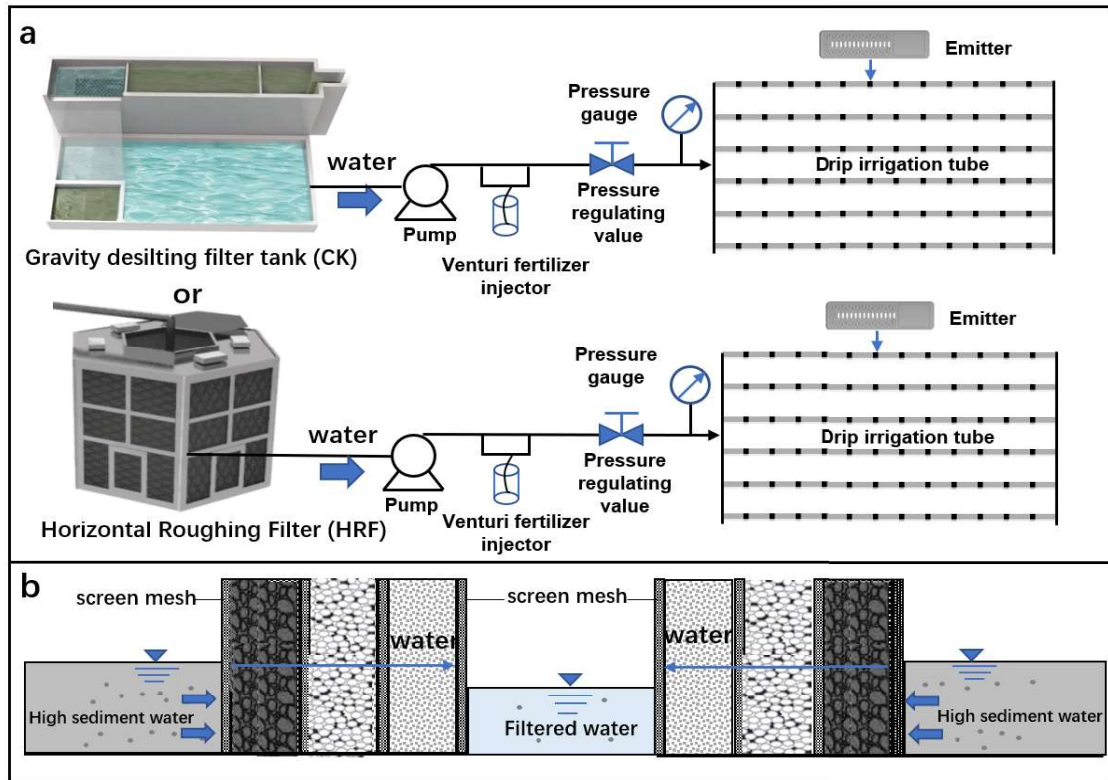
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20 463 Fig. 7 Effect of HRF on Dra and CU of Drip irrigation system

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22 464 Table 1 Water quality parameters of the high-sediment water

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25 465 Table 2 Characteristic parameters of emitters

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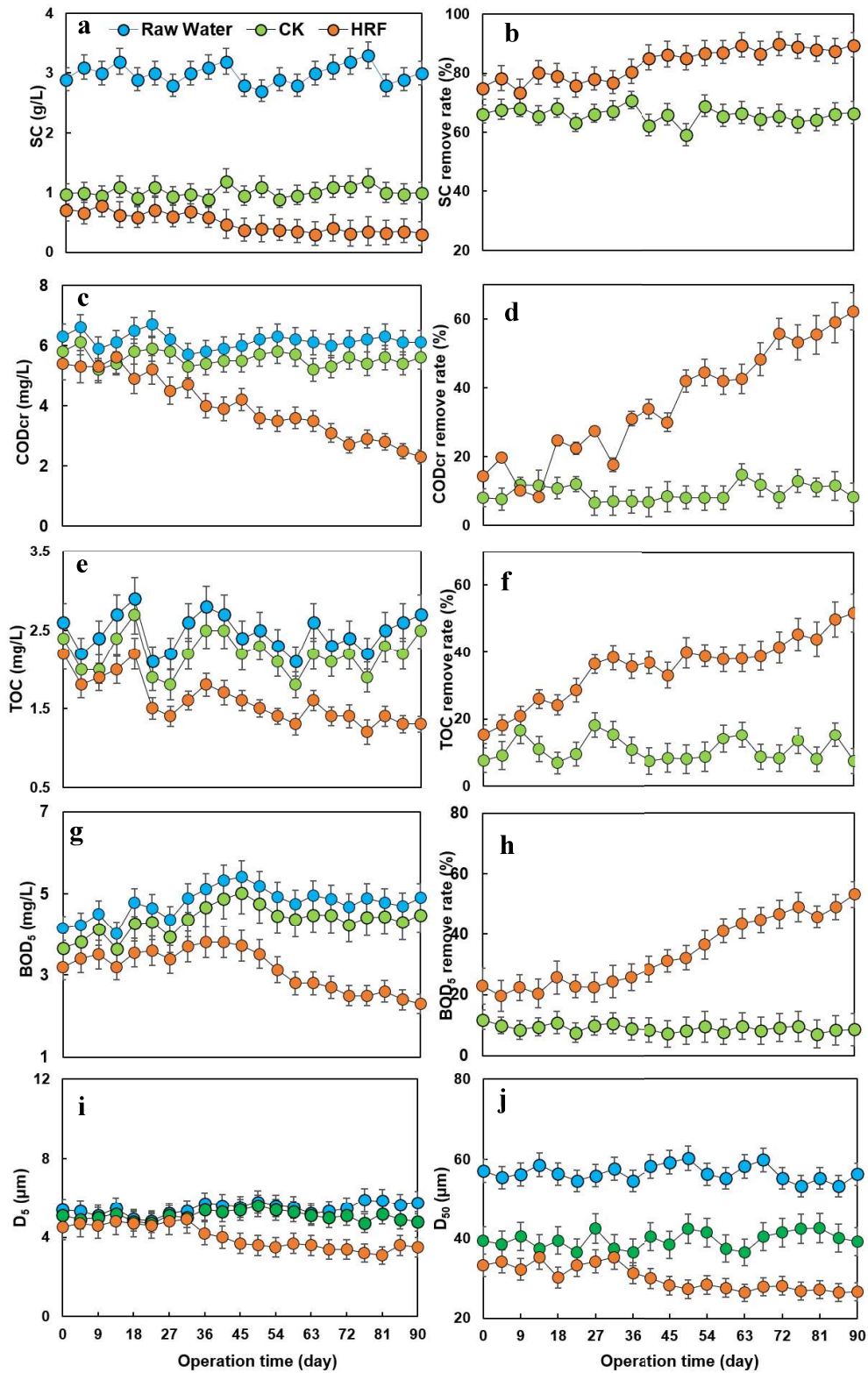
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Fig. 1. Layout of experiments system. (a) Layout of the test system platform; (b) Filtration principle of HRF

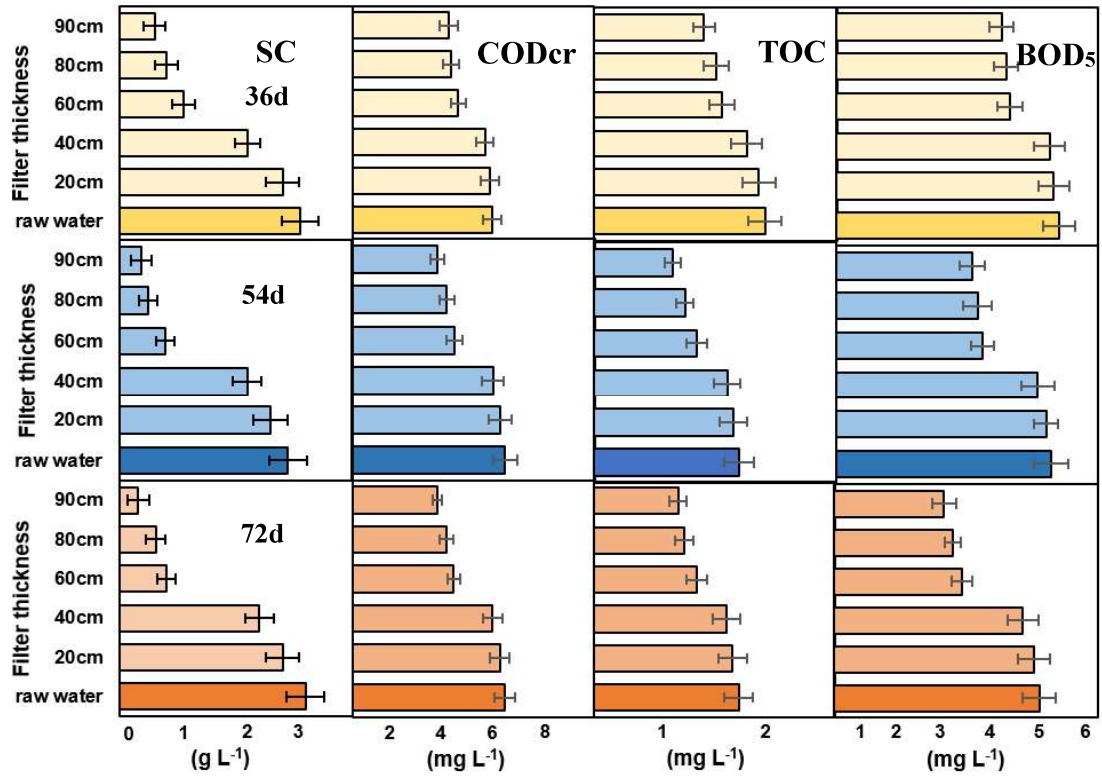
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471 **Fig. 2.** Effects of HRF on water quality parameters. (a) and (b) SC, Sediment Concentration; (c) and (d)
 472 CODcr, Chemical Oxygen Demand; (e) and (f) TOC, Total Organic Carbon; (g) and (h) BOD₅,
 473 Biochemical Oxygen Demand; (i) and (j) D₅ and D₅₀, cumulative particle size distribution ratio reaches
 474 5% and 50%. HRF, Horizontal Roughing Filter; CK, Gravity desilting filter.

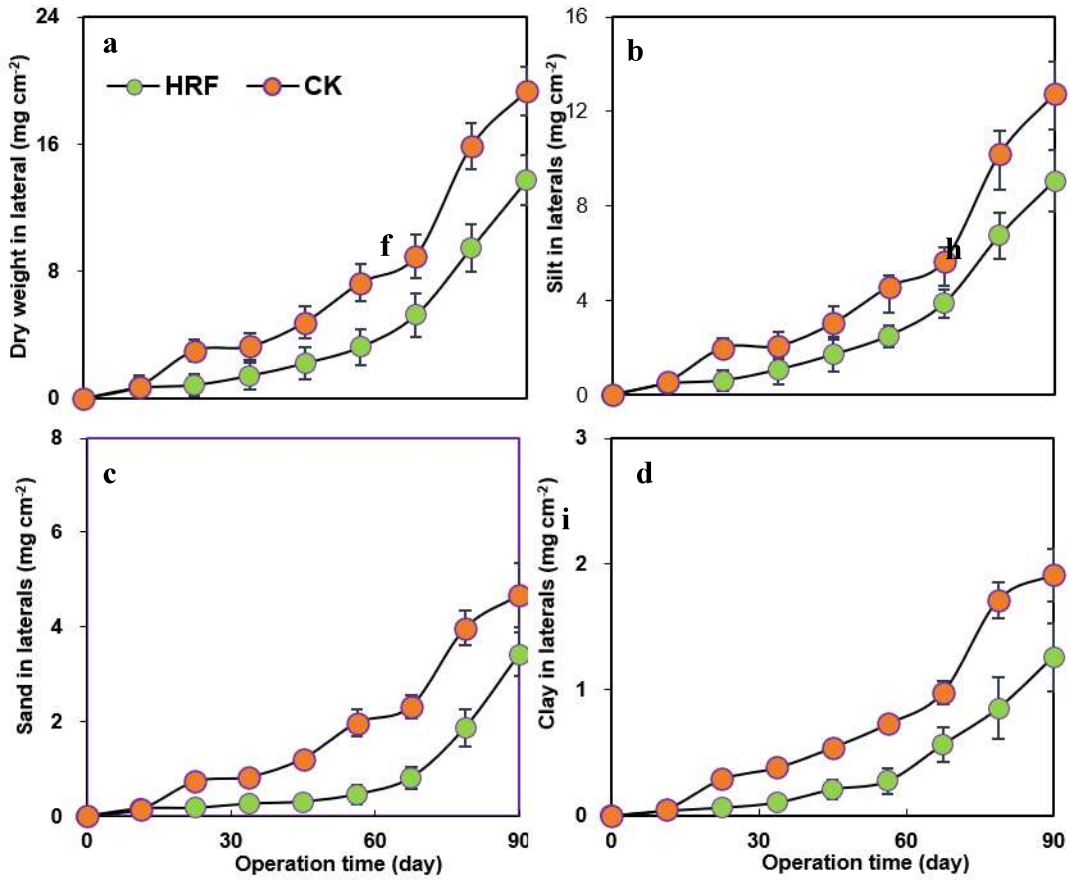
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476 **Fig. 3.** Effect of filter layer thickness on the water quality parameters. Sampling point at different run
 477 times: 36 day (Yellow), 54 day (Blue) and 72 day (Orange). SC, Sediment Concentration; COD_{cr},
 478 Chemical Oxygen Demand; TOC, Total Organic Carbon; BOD₅, Biochemical Oxygen Demand.

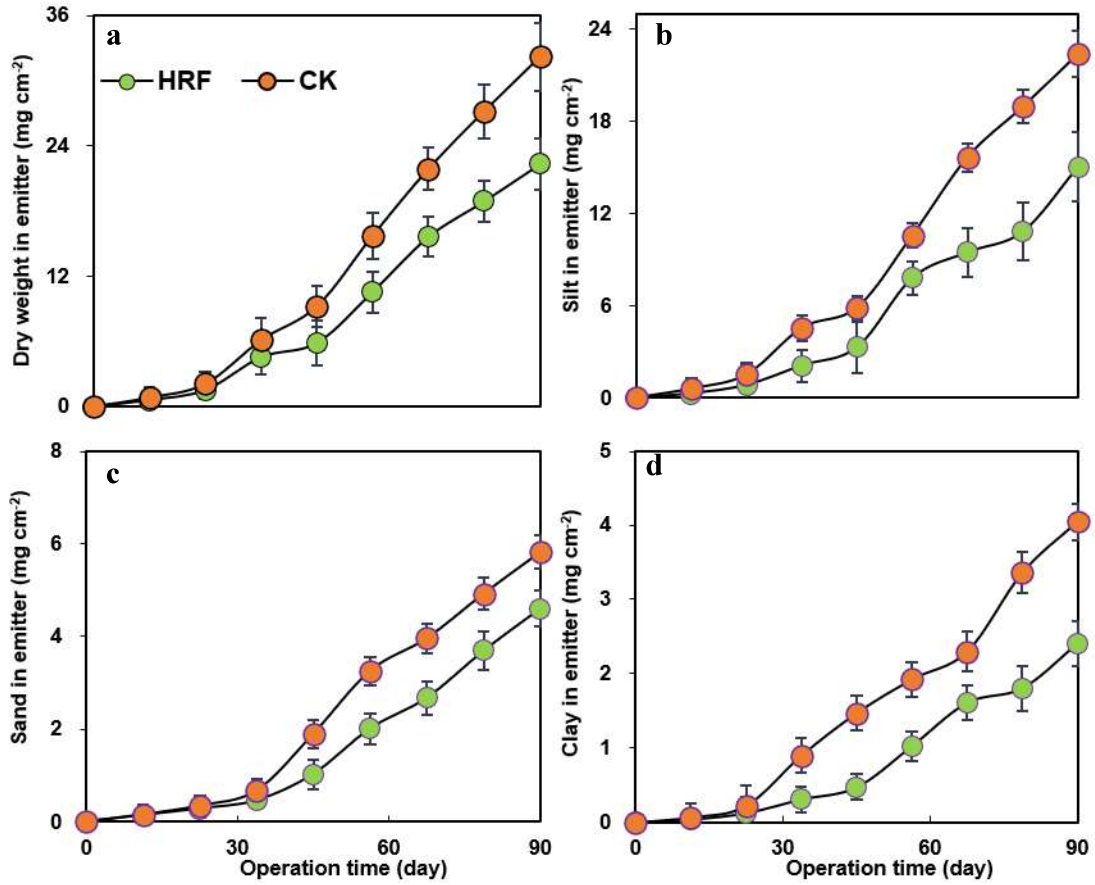
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480 **Fig. 4.** Effects of HRF on clogging substances in laterals of drip irrigation system. (a) Dry weight
 481 represents total clogging substance; (b) represent the content of silt of clogging substance; (c) represent
 482 the content of sand of clogging substance; (d) represent the content of clay of clogging substance. HRF,
 483 Horizontal Roughing Filter; CK, Gravity desilting filter.

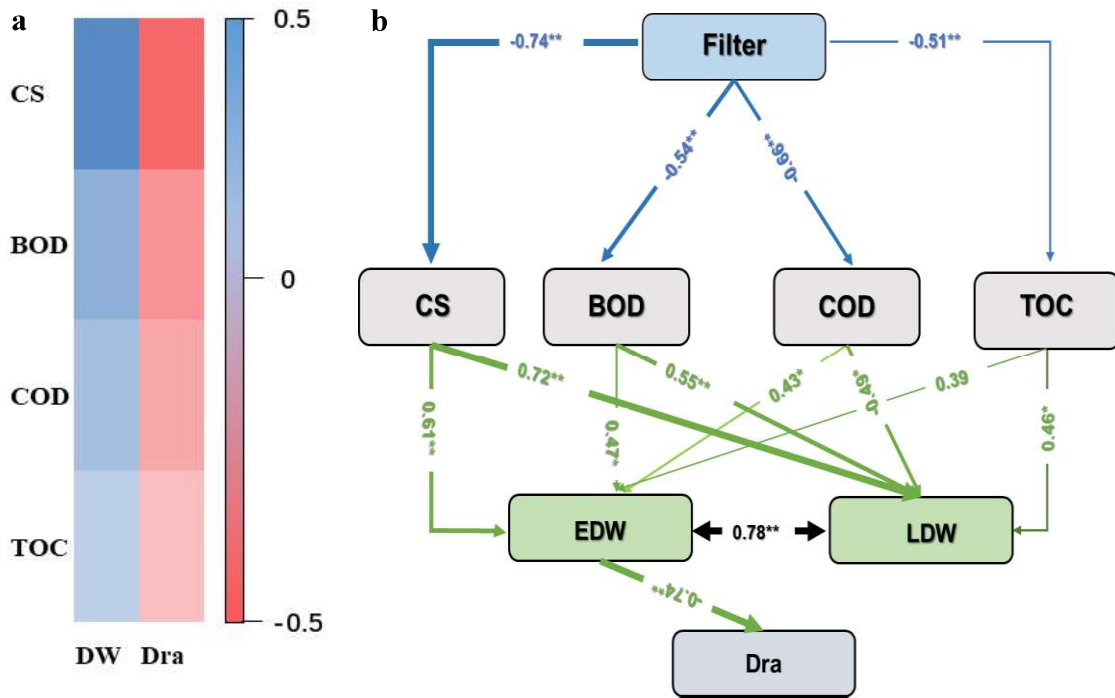
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485 **Fig. 5** Effects of HRF on clogging substances in emitter of drip irrigation system. (a) Dry weight
 486 represents total clogging substance; (b) represent the content of silt of clogging substance; (c) represent
 487 the content of sand of clogging substance; (d) represent the content of clay of clogging substance. HRF,
 488 Horizontal Roughing Filter; CK, Gravity desilting filter.

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490 **Fig. 6** Controlling pathway of HRF on composite clogging substance in drip irrigation system. (a)
 491 Spearman correlation of water quality, DW (Dry Weight) and Dra; (b) is the structural equation model
 492 analysis (SEMA). The SEMA shows the relationship between the HRF treatment, water quality
 493 parameters (CS, BOD₅, COD, TOC), emitter dry weight (EDW), laterals dry weight (LDW) and the
 494 Dra. Green and blue radial lines respectively represented significant positive correlation ($p < 0.05$) and
 495 significant negative correlation ($p < 0.05$). The blue and green single-headed arrows represent positive
 496 and negative interactions, respectively, and the thickness of the arrow represents the strength of the
 497 correlation. The number on the arrow represents the standard path coefficient (β).

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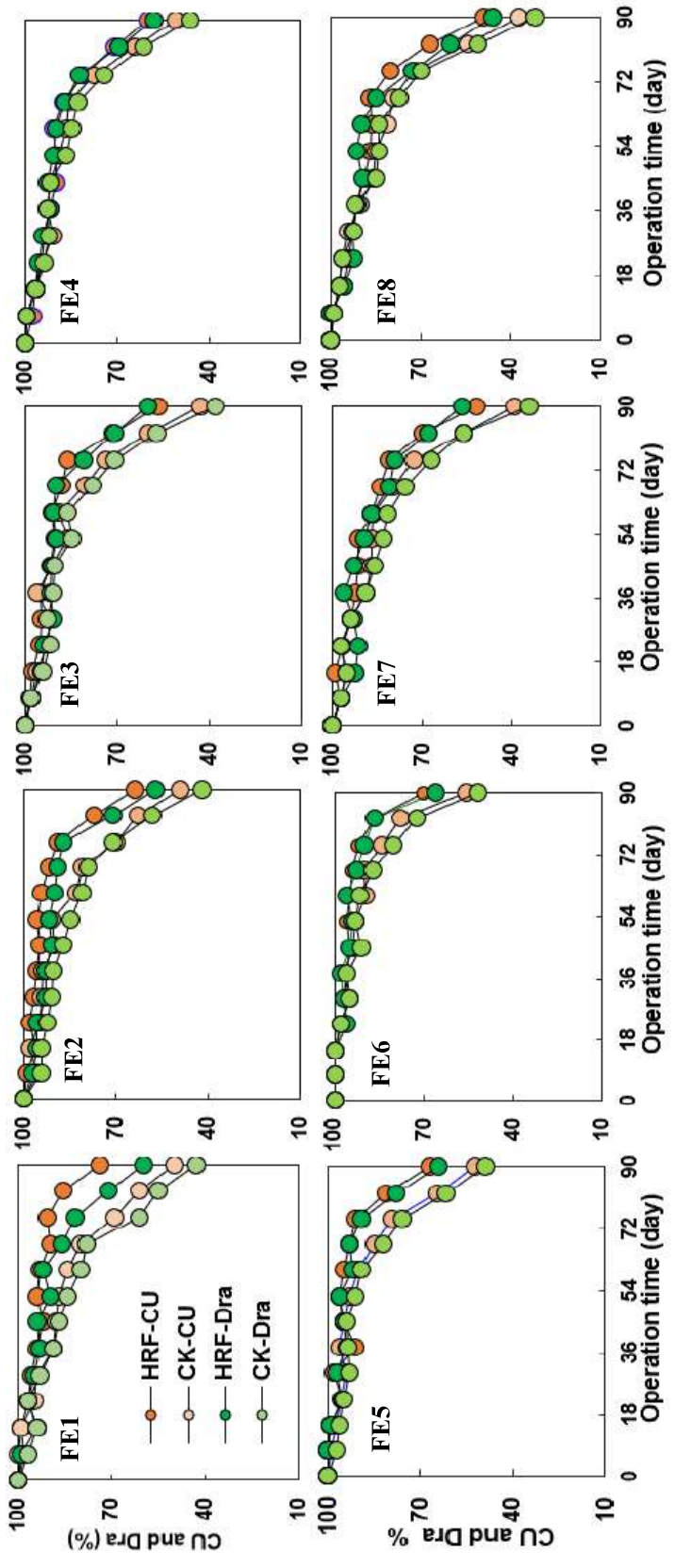


Fig. 7. Effect of HRF on Dra and CU of Drip irrigation system. HRF, Horizontal Roughing Filter; CK, Gravity desilting filter. CU, Christiansen coefficient of uniformity; Dra, average discharge variation ratio.

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Table 1 Water quality parameters (average \pm standard deviation) of the high-sediment water

Parameter	Results	Parameter	Results
pH	7.3 \pm 0.6	Bicarbonate (HCO_3^-) (mg L^{-1})	152 \pm 21
Suspended solids SS (mg l^{-1})	73.7 \pm 5.2	Phosphate (PO_4^{3-}) (mg L^{-1})	0.25 \pm 0.08
Electrical conductivity EC ($\mu\text{S cm}^{-1}$)	740 \pm 52	Phosphorus (P) (mg l^{-1})	0.04 \pm 0.01
Nitrogen (N) (mg l^{-1})	1.2 \pm 0.3	Calcium (Ca^{2+}) (mg l^{-1})	53.6 \pm 8.4

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Table 2 Characteristic parameters of the tested emitters

Emitter	Initial outflow Q (L/h)	Flow path length L (mm)	Flow path width W (mm)	Flow path depth D (mm)	Flow index x
FE1	0.8	21.52	0.50	0.45	0.51
FE2	1.0	23.06	0.50	0.52	0.51
FE3	1.2	23.02	0.63	0.52	0.50
FE4	1.4	25.07	0.63	0.52	0.51
FE5	1.6	29.74	0.63	0.52	0.51
FE6	2.8	41.13	0.67	0.56	0.50
FE7	1.1	17.71	0.56	0.61	0.51
FE8	2.0	26.41	0.71	0.68	0.56

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