

1 **Using Phosphate Fertilizer to Reduce Emitter Clogging of Drip**
2 **Fertigation Systems with High Salinity Water**

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9 **ABSTRACT:** Phosphorous (P) fertigation with high salinity water (HSW) drip irrigation would be an
10 effective measure to relieve soil and water pollution caused by the excessive application of P fertilizer, and
11 achieve synergistic saving of both limited fresh water and non-renewable P resources. However, the
12 emitter clogging issues of drip fertigation systems seriously restricts the utilization of this technology. This
13 study proposes an approach to reduce emitter clogging in HSW drip fertigation systems by choosing the
14 appropriate type and concentration of P fertilizer. The effects of two new types of P fertilizers (ammonium
15 polyphosphate, APP; urea phosphate, UP), and a traditional P fertilizer (monopotassium phosphate, MKP),
16 were assessed at three fertilization concentrations (0, 0.15, and 0.30 g/L) on the clogging behavior of four
17 types flat emitters. The results indicated that the application of MKP aggravated the clogging of emitters in
18 comparison with non-fertilization. While the addition of two new types of P fertilizers (APP and UP)
19 effectively alleviated emitters clogging (the irrigation uniformity of systems increased by 26.2% - 74.6%)
20 by inhibiting the formation of carbonate, although precipitation of phosphate, silicate, and quartz increased.
21 Moreover, under the equal application amount of P fertilizer, UP and APP were more effective in relieving
22 clogged when applied at a low-concentration with long-term running and high-concentration with
23 short-term running mode. The results could pave a way for reducing the pollution in agricultural
24 production and conserving freshwater and non-renewable P resources.

25 **Keywords:** brackish water; fertigation; drip irrigation; emitter discharge

26

27 **1. Introduction**

28 Effective irrigation and fertilization managements in agricultural production are the most fundamental
29 supports to ensure global food security and sustainable development of human society (Qin et al., 2019; Yu,
30 et al., 2019). Over the past decades, the scale and intensity of agricultural production have been expanded
31 rapidly. At present, agricultural irrigation accounts for 69% of global freshwater consumption (FAO, 2016),
32 and nearly 1/5 of the world's population is living in water-scarce areas. Meanwhile, fertilizers are often
33 excessively inputted in agricultural production due to its low utilization efficiency, which caused a serious
34 agricultural non-point source pollution and water eutrophication (Vaneeckhaute et al., 2016; Chien, et al.,
35 2009). In particular, the seasonal utilization efficiency of P always less than 25% (Wang et al., 2015)
36 because P is easily immobilized by soil (Roberts, 2015). Moreover, the raw material of P fertilizer, e.g.,
37 phosphate rock as a non-renewable resource, is expected to be exhausted within 50 years based on current
38 mining intensity (Natasha, 2009). Therefore, the scarcity of freshwater and P resources associated with
39 water and soil pollution, and food security has become one of the important challenges in the 21st century
40 (Li et al., 2019a; Scholz and Wellmer, 2015). Thus, there is a need for reducing the consumption of
41 freshwater and P fertilizer and increasing their utilization efficiency in agricultural production.

42 The utilization of widespread high salinity water (HSW) may offer an effective measure to cope with
43 water scarcity. However, irrigation with HSW can easily cause salt stress in the crop root zone, inhibiting
44 its applications in agricultural irrigation (Wei et al., 2019). Drip irrigation is considered the most reliable
45 and effective ways to utilize HSW (Karlberg et al., 2007), as salts usually accumulate at the edge of the
46 wetting front, thus reducing the salt stress in the root zone (Kang et al., 2010). On the other hand,
47 compared with the traditional application of P fertilizer (i.e. directly broadcast P into the soil), the
48 application of dissolved P fertilizer through drip irrigation system can greatly increase the movement of P

49 and reduce the adsorption by soil, thereby improving the utilization efficiency of P fertilizer (Ayars et al.,
50 2017). Therefore, drip fertigation technology (i.e. integration of water and fertilizer) is expected to be a
51 promising way to cope with the soil and water pollution caused by the excessive input of P fertilizer and
52 save limited freshwater and P resources.

53 However, drip fertigation with HSW is currently not popular. The main reason is that the channel of
54 emitter in a drip irrigation system is very narrow (0.5 - 1.2 mm) (Goyal and Mansour., 2015), and many
55 salt ions in HSW can easily recombine and precipitate inside the channel, which induces emitter clogging
56 (Zhangzhong et al., 2016). Furthermore, the emitters clogging becomes more complex with addition of P
57 fertilizer. Zhou et al. (2019) found that the application of MKP greatly increased emitter clogging. Overall,
58 emitter clogging has become the main obstacle to the integrated application of drip fertigation with HSW
59 and P fertilizer, which would directly reduce the irrigation and fertilization uniformity in drip irrigation
60 systems, and greatly reduce the replacement cycle of drip lines of irrigation system. The appropriate
61 application mode of P fertilizer could relieve the clogging issue. Yang et al. (2019) observed that the rate of
62 drip emitters clogging obviously differed with different P fertilizers. Li et al. (2015) reported that the
63 concentration of fertilizer affected the clogging of drip emitters. In recent years, two new types of
64 phosphate fertilizers (UP and APP) have been identified might could alleviate emitter clogging. Every
65 kilogram of dissolved UP produces 6.3 moles of H^+ , which makes it a high concentration acidifier (Goyal,
66 2015) to avoid the mineral precipitation (e.g. calcium carbonate). Polyphosphate does not easily react with
67 calcium and magnesium ions in water under specific conditions, and it is often used as scale inhibitor (Noy
68 and Yoles, 1979). However, effect of the two new phosphate fertilizers on the clogging of emitters in drip
69 irrigation system using HSW have not been investigated yet.

70 Accordingly, this study evaluated the effects of two new types of phosphate fertilizer (UP and APP),
71 one traditional phosphate fertilizer (MKP) on the clogging behavior of four flat emitters at three
72 fertilization concentrations level (0, 0.15 and 0.3 g/L). Hence, the objects of this study were threefold: 1)
73 determine the effectiveness of two new types of phosphate fertilizers (UP and APP) to alleviate the emitter
74 clogging with HSW; 2) clarify the mechanisms emitters clogging using phosphate fertilizer; and 3) identify
75 suitable application mode (i.e. the type and concentration of P fertilizer) of HSW phosphate drip fertigation
76 systems.

77 **2. Materials and methods**

78 **2.1. Experimental setup**

79 The experiment was conducted at Tongzhou Experiment Station of China Agricultural University (116°
80 41'2. 31 " E, 39° 42'6. 93 " N) in 2018. The saline water source was a well located at the station (Table
81 A1). The drip irrigation with HSW testing system shown in Fig. 1 was divided in four layers, each layer
82 was equipped with one type of emitter and each emitter type facilitated with eight replicates. Four types of
83 flat non-pressure compensating emitters were subjected for the experiment, the detailed physical
84 parameters are as listed in Table A2. The length of each drip lateral was 18 m, the emitters on it with a
85 consistent spacing of 0.33 m in between, thus altogether 55 emitters from inlet to outlet were used. The
86 system operating pressure during the operation was kept as 0.1 MPa, and the amount of water and fertilizer
87 was monitored with a water meter. In this experiment, the phosphate fertilizers were: MKP, UP and APP;
88 fertilizer concentrations were: 0 g/L, 0.15 g/L and 0.30 g/L. Overall, there were 7 treatments, i.e.,
89 MKP_0.30, MKP_0.15, UP_0.30, UP_0.15, APP_0.30, APP_0.15 and CK (non-fertilization). The system
90 was operated once a day, representing the actual field irrigation or fertilization conditions. Fertilization was

91 carried out every other day at the center of the whole operation time. The quantity of applied fertilizer and
92 irrigation water for each drip irrigation lateral was 33.75 g/day and 0.45 m³/day. The fertilization/irrigation
93 plans (Fig. A1) included low concentration/long term (LCLT), high concentration/short term (HCST) and
94 CK treatments.

95 #Fig. 1 approximately here#

96 **2.2. Testing method of emitter discharge evaluation**

97 The weighing method (Zhou et al., 2019) was adopted to calculate the emitters' discharge. The
98 multi-layer flow-measuring trolley, which had a 4-layer structure, was used to measure the flow of emitters
99 by placing small buckets (internal diameter of 0.15 m) underneath each tested emitter. A stopwatch (with
100 an accuracy of 0.01 s) was used to record measuring time of 5 min. Finally, the weight measured by a
101 high-precision electronic balance (with an accuracy of 10⁻³ g) together with measuring time allowed
102 calculating the flow rate of each emitter.

103 **2.3. Evaluation parameters of emitter performance**

104 Average discharge variation rate (*Dra*, Li et al., 2019b) was computed to determine the clogging
105 degree of emitters and Christiansen uniformity (*CU*, Christiansen., 1942) was used to quantify the
106 irrigation uniformity of several emitters along a lateral (Section 1.5 of the supplementary materials).

107 **2.4. Extraction and evaluation of clogging substances in emitters**

108 During the whole experiment, each treatment was sampled 8 times. At each sampling event, drip
109 lateral was destructively fetched, hereafter 5 samples out of the 15 emitters in head, middle and tail were
110 selected. The samples were placed in centrifuge tubes and stored in refrigerators at 4°C.

111 Dry weight (*DW*) of substances inside emitters determined the total clogging. Fifteen emitter samples
112 were placed in zip lock bags, added 20 mL of deionized water to remove the clogging substances for 60
113 min using the ultrasonic cleaner (manufacture: Chaowei; type: GVS-10 L). The mixed solid phase of 15
114 emitter samples acquired at the bottom was dried to a constant weight and then weighed using a
115 high-precision electronic balance.

116 The dried solid phase was ground and X-ray diffractometer (manufacture: Bruker, Germany; type:
117 D8-Advance) was used to get the polycrystalline diffraction patterns. Basic test conditions for the scanning
118 process were: voltage 40 kV, current 40 mA, Cu target, wavelength $\lambda=1.5406 \text{ \AA}$. Then, the patterns were
119 analyzed by the Topas software (Bruker Corp) to obtain the mineral contents and components of the
120 clogging substances. The polycrystalline diffraction patterns were as Fig. A2 (E1 as a sample).

121 In fertilization treatments, amorphous components were found. The component of amorphous
122 components was tested by Fourier transform infrared spectrometer (FTIR) and scanning electron
123 microscope with an energy dispersive spectrometer (SEM-EDS). The component of amorphous
124 components was phosphate.

125 **2.5. Statistical analysis**

126 The Pearson analysis was applied to study the correlations among the *Dra*, *CU* and mineral contents.
127 Paired t-test was used to analyze the differences between different treatments. During these processes, the
128 significance thresholds of the independent variables were determined at $p < 0.05$ and $p < 0.01$. The
129 regressions and statistical analyses were carried out using SPSS (ver. 20.0, IBM Analytics).

130 **3. Results**

131 **3.1. Effect of phosphorous fertigation on emitter performance (*Dra* and *CU*)**

132 The system *Dra* (Fig. A3) and *CU* (Fig. A4) indicated that emitters' performance across all treatments
133 decreased over time. The performances showed a slow decline during the early stage (0 - 16 d) and a rapid
134 decline during the later stages (16 - 64 d). Moreover, emitters' performance varied greatly among different
135 treatments. The correlations of *Dra* and *CU* between different treatments are shown in Fig. 2. Compared to
136 CK, UP and APP significantly ($p < 0.05$, Table A3) alleviated the emitter clogging. The *Dra* and *CU* of UP
137 treatments were increased by 25.0% - 45.0% and 26.2% - 44.5% and APP treatments increased by 46.3% -
138 73.6% and 46.1% - 74.6%, respectively. Conversely, *Dra* and *CU* of MKP decreased by 14.3% - 34.7%
139 and 10.8% - 38.6%, respectively, meaning that emitter clogging was worsened. Fertigation concentrations
140 also exhibited a significant impact on the emitter clogging (Table A3). APP significantly alleviated the
141 clogging of the emitter under the high-concentration (0.30 g/L) and short-term (HCST) fertilization mode,
142 which increased *Dra* and *CU* by 50.9% and 52.7% than under low-concentration (0.15 g/L) and long-term
143 (LCLT) fertilization mode. But UP and APP treatments showed opposite results. Both *Dra* and *CU* of UP
144 under HCST fertilization mode were significantly lower than LCLT fertilization mode by 36.3% and
145 33.1%, respectively. For MKP, the reduction ratio of *Dra* and *CU* were 17.9% and 25.1%, respectively.

146 #Fig. 2 approximately here#

147 **3.2. Total dry matter (*DW*) and mineral components of emitter clogging substances**

148 Total *DW* of clogging substances across each treatment increased gradually over time. Moreover, the
149 type and concentration of fertilization directly affected the accumulation of *DW* (Fig. A5). Compared to
150 CK, UP and APP significantly ($p < 0.05$) decreased the *DW* of clogging substances (Table A4) by 21.1% -
151 28.6% and 32.2% - 42.0% (Fig. 3). After the application of MKP, the *DW* increased by 3.0% - 18.7%.
152 Significant effect of fertilization concentrations on *DW* was also observed (Table A4). With the increase of

153 fertilizer concentration, APP significantly alleviated more the *DW* of the emitter under the HCST
154 fertilization mode, which decreased *DW* by 14.7% than LCLT fertilization mode. However, the *DW* of UP
155 and MKP under HCST fertilization mode were significantly higher than LCLT fertilization mode by 9.7%
156 and 15.5%.

157 The mineral components inside emitters are shown in Fig. 4 (taken E1 as an example, at the end of the
158 experiment) and Fig. A6 (all emitters and all periods). The results indicated that mineral components
159 mainly included muscovite $[K(Mg,Al)_{2.04}(Si_{3.34}Al_{0.66})O_{10}(OH)_2]$, clinocllore $[(Mg_5Al)(Si_3Al)O_{10}(OH)_8]$,
160 anorthite $[CaAl_2Si_2O_8]$, monohydrocalcite $[CaCO_3 \cdot H_2O]$, dolomite $[CaMgCO_3]$, aragonite $[CaCO_3-O]$,
161 calcite $[CaCO_3-R]$, quartz $[SiO_2]$, and phosphate (the determination process of phosphate is shown in
162 Section 2.5 of the supplementary materials). The nine primary mineral components can be divided into
163 carbonate, phosphate, silicate, and quartz according to the main chemical elements. The mineral
164 component of CK was mainly carbonate, and the mineral components for fertilization treatments were
165 mainly a mixture of carbonate and phosphate. The ratios of the four types minerals across all treatments for
166 emitter E1 (Fig. A9) were: 18.5% - 94.1% (carbonate), 34.6% - 60.1% (phosphate, except CK), 5.0% -
167 15.9% (silicate), and 0.9% - 8.2% (quartz), respectively.

168 #Fig. 3 approximately here#

169 #Fig. 4 approximately here#

170 3.3. Correlation of mineral components among different treatments

171 The variation of average carbonate, phosphate, silicate, and quartz content (Fig. A10) indicated that
172 all mineral components showed a slow increase during early stage (0 - 16 d) and a rapid increase during
173 the later stages (16 - 64 d). Moreover, mineral content varied greatly across treatments. Compared to CK,

174 UP, APP and MKP all significantly ($p < 0.05$, Table A5) inhibited the formation of carbonate (Fig. A10, Fig.
175 5a). The carbonate content in three fertilizer treatments (UP, APP and MKP) were decreased 50.4% -
176 59.2%, 66.0% - 81.5%, and 74.1 - 76.2%, respectively. Fertilizer concentration had a significant effect ($p <$
177 0.05, Table A5) on carbonate content. Thus, the carbonate content in MKP_0.30 was significantly lower
178 than MKP_0.15 by 17.7%, UP_0.30 was significantly lower than UP_0.15 by 45.5%, but APP_0.30 was
179 significantly lower than APP_0.15 by 8.8%.

180 Significant differences ($p < 0.05$, Table A5) were observed in phosphate contents among different
181 treatments (Fig. 5b). The phosphate contents of UP_0.15 and APP_0.15 were lower than MKP_0.15 by
182 18.0% and 5.9%, and UP_0.30 and APP_0.30 were lower than MKP_0.30 by 36.5% and 43.9%. Fertilizer
183 concentration had an evident effect on phosphate content. The phosphate contents in HCST fertilization
184 mode of UP, APP, and MKP were significantly ($p < 0.05$) increased by 40.0%, 7.5% and 80.7%,
185 respectively.

186 Compared to CK, the three P fertilizers significantly ($p < 0.05$, Table A5) promoted the formation of
187 silicate (Fig. 5c). The silicate content of the UP, APP, and MKP increased 46.6% - 102.8%, 21.3% - 75.8%
188 and 56.1% - 234.9% regarding CK, respectively. Fertilizer concentrations also had a significant ($p < 0.05$)
189 effect on silicate content. The silicate content of MKP_0.30 was lower than MKP_0.15 by 53.4%, UP_0.30
190 was lower than UP_0.15 by 31.0%, and APP_0.30 was lower than APP_0.15 by 27.8%.

191 The quartz content in different treatments (Fig. 5d) was also significantly different ($p < 0.05$, Table
192 A5). The quartz content of the UP, APP, and MKP increased 218.3% - 462.2%, 146.1% - 396.3% and 448.2%
193 - 657.6%. The quartz content of MKP_0.30 was 38.2% higher than MKP_0.15, UP_0.30 was 76.6% lower
194 than UP_0.15, but APP_0.30 was 50.4% lower than APP_0.15.

195 #Fig. 5 approximately here#

196 **3.4. Correlation between the content of mineral components and *CU***

197 A linear relationship between *Dra* and *CU* were found (Fig. A11). The results shown in Fig. 6 (a) - (d)
198 indicated that the contents of carbonate, phosphate, silicate and quartz in all treatments were significantly
199 negatively correlated ($p < 0.05$, $R^2 > 0.82$) with their *CU*, and their fitting parameter *K* (regression line
200 slope coefficient) for carbonate, phosphate, silicate and quartz ranged -5.28 - -0.96, -5.53 - -0.66, -27.01 -
201 -6.89 and -124.34 - -15.19.

202 #Fig. 6 approximately here#

203 **4. Discussion**

204 **4.1. Mechanism of phosphorous fertilizer on emitter clogging**

205 The results of this experiment (Fig. 2) showed that the application of UP and APP could effectively
206 relieve the emitter clogging in drip irrigation system with HSW. UP alleviated the emitter clogging by
207 reducing the content of carbonate, although the increased content of phosphate, silicate, and quartz in
208 mineral components of emitter clogging substances (Fig. 4). The decrease of carbonate is attributed to the
209 acidic nature of the UP solution, as produced of 6.3 mol H^+ for 1 kg of dissolved UP, which promotes the
210 transformation of CO_3^{2-} to HCO_3^- and thus inhibits the formation of carbonate. In addition, the hydrolysis
211 of UP produced a large amount of PO_4^{3-} , which competed with CO_3^{2-} for Ca^{2+} and Mg^{2+} . Therefore, the
212 production of calcium phosphate precipitate was promoted (Fig. 4), showing a power function growth
213 trend, and the production of carbonate precipitate was further inhibited (Hammes and Verstraete, 2002).
214 Moreover, the application of P reduces the pH (1% UP aqueous solution has pH 1.89) of HSW, resulting in
215 a significant increase in silicate contents (Table A5). Actually, pH decrease promoted the condensation of
216 silanol structure, and impelled the polymerization of silicate gel (Neofotistou and Demadis, 2004), and

217 thus exacerbated silicate deposition. The increase in quartz was probably due to the negative charge of
218 particulate matter such as quartz in water source. While the addition of UP fertilizer induced a lot of
219 positive charge to compress the electric double layer by electrostatic attraction and became thinner when
220 the cations increased and zeta potential decreased (Zhou et al., 2019), leading to significant increase in the
221 solid particulates' flocculation and sedimentation strength (Liu et al., 2017). Since the experiments were
222 carried out at room temperature and 100 kPa pressure, it is difficult to form SiO_2 in the emitter at these
223 conditions. Therefore, the SiO_2 found in clogging substances were mainly induced from the water (Zhou et
224 al., 2018). Taking quartz as an independent variable, the accumulation processes of phosphate, carbonate
225 and silicate (as dependent variables) are plotted in Fig. A12. The results showed that there was a high
226 linear relationship between silicate and quartz, which indicated that the variation rate of silicate was
227 relatively stable along with system operation. The stable variation further revealed that silicate and quartz
228 are basically homologous, originated from water, rather than resulted from a chemical reaction during
229 process of system operation. The carbonates and phosphates showed a power-function growth, which
230 indicated that not only came with water source but also resulted from chemical reactions.

231 APP treatment also significantly reduced the emitter clogging. Similar to UP, the content of carbonate
232 in the emitter clogging substances when using APP decreased significantly, while silicate and quartz
233 increased, and phosphate component were appeared at the same time. APP also produced competitive
234 adsorption to form phosphate, which reduced the content of carbonate (Fig. A10). However, APP did not
235 significantly change the pH of fertigation water (Table A5). The reason why the content of carbonate
236 decreases greatly is APP is usually a mixture of different chain lengths (Waerstad and McClellan, 1976).
237 This special structure results in that APP can chelate Ca^{2+} and Mg^{2+} and other metal ions at a certain
238 concentration, will shield Ca^{2+} and Mg^{2+} (Noy and Yoles, 1979; Hagin et al., 2002), thus reducing the

239 probability of carbonate reacting with Ca^{2+} and Mg^{2+} , and greatly reducing the formation of carbonate. The
240 formation of phosphate mainly due to the large amount of PO_4^{3-} brought by APP, that inevitably react with
241 calcium ions in water to form insoluble calcium phosphate compounds (Ryan and Saleh., 2000). The
242 formation mechanism of silicate and quartz were similar to UP. Fig. A12 (d) indicated a linear growth trend
243 of both silicate and quartz, while carbonate and phosphate showed a quadratic function growth trend with a
244 gradual slowed-down growth rate, which indicated that APP could inhibit the formation of salt substances.

245 After the application of MKP, emitter clogging drastically increased, while the content of carbonate
246 noticeably reduced. Similar to UP, this was mainly due to the formation of phosphate precipitate by
247 reducing water pH and competitive adsorption of calcium and magnesium ions. Besides phosphate
248 precipitations, MKP increased the silicate and quartz levels in clogging substances (Figs. 4 and 5). During
249 the application of MKP in drip irrigation, large amount of Ca^{2+} and Mg^{2+} in high saline water consumed
250 the HCO_3^- to form a large amount of carbonate, and then the remaining Ca^{2+} , Mg^{2+} , and PO_4^{3-} produced by
251 the electrolysis of MKP reacted to form phosphate. Dicalcium phosphate was considered to be the main
252 precipitate formed by the reaction of PO_4^{3-} and Ca^{2+} in irrigation water (Chow and Eanes, 2001). Then,
253 dicalcium phosphate hydrolyzed as hydroxyapatite or dicalcium phosphate quickly transformed to
254 octacalcium phosphate and further transformed to hydroxyapatite (Tung and Skrtic, 2001). On the other
255 hand, CaCO_3 absorbed PO_4^{3-} and formed insoluble compounds (Zhou et al., 2018). Therefore, under MKP
256 application in high salinity groundwater, the formation of phosphate in water mainly depended on the
257 adhesion of attachment of PO_4^{3-} on CaCO_3 surface and ion reaction (Bertrand et al., 2006). At the same
258 time, the deposition of phosphate and carbonate greatly increased the surface area of clogging substances
259 on the inner surface of the emitter, which further promoted the deposition of clogging substances on the
260 surface of flow channel (Zhou et al., 2019). The two effects together resulted in the exponential growth

261 trend of carbonate and phosphate, while the content of silicate and quartz increased linearly (Fig. A12 b),
262 which together aggravated the clogging of emitters.

263 It was found that the concentration of phosphorus fertilizer would affect the clogging rate of the
264 emitter under the same amount of fertilizer. UP and APP could effectively alleviate the clogging of emitter
265 under the mode of LCLT and HCST, respectively. For UP treatment, the clogging degree of HCLT
266 fertilization treatment was significantly higher than LCLT fertilization treatment. This was mainly because
267 the phosphate and quartz precipitation were significantly increased under HCLT fertilization mode. The
268 increase of phosphate may be related to time factors, the longer the reaction time was, the more phosphate
269 formed (Bremner and Douglas, 1971). The higher the concentration of UP, the more noticeable the
270 flocculation and sedimentation of quartz, and the higher the content of quartz (Liu et al., 2017). For APP
271 treatment, the higher the fertilizer concentration, the lower the risk of emitter clogging. With the increase
272 of APP concentration, the chelating effect gradually increased, and the effect of reducing carbonate
273 precipitation gradually appeared. APP also reacted with Ca^{2+} and Mg^{2+} at a certain concentration to form a
274 colloidal suspension clogging the emitter, which is related to the content of Ca^{2+} in the water source and
275 the concentration of ammonium polyphosphate (Noy and Yoles, 1979). Hagin and Tucker (1982) indicated
276 that injection of small quantities of ammonium polyphosphate solution into water high in dissolved
277 calcium resulted in precipitation of calcium ammonium pyrophosphate, while injection of large quantities
278 of polyphosphate caused the precipitate to disappear due to the sequestering ability of the polyphosphate.
279 Duis and Burman (1969) found that for ammonium polyphosphate (11-37-0) in a water containing up to
280 100 mg/L Ca no precipitate will form regardless of the ammonium polyphosphate added to supply a high or
281 low concentration in the irrigation water, whereas in a water containing 200 mg/L Ca the polyphosphate in
282 a 1:300 dilution in water will form precipitates, but a 1:200 dilution will prevent their formation.

283 4.2. Selection of phosphate fertilizer application mode

284 Although demonstrated the effect of phosphorus fertilizer application on the clogging of drip
285 irrigation emitter, the effects of soil texture, fertilizer price and availability need to be considered in the
286 practical application of phosphate fertilizer at farm level (Hagin and Tucker, 1982; Goyal and Mansour.,
287 2015b).

288 Firstly, in addition to alleviating emitter clogging, low concentration UP can effectively reduce soil
289 pH which is suitable to apply UP in alkaline soil (Mikkelsen and Jarrell, 1987). Secondly, UP can promote
290 the conversion of phosphate to H_2PO_4^- form, thus enhance phosphorous availability and use efficiency
291 (Kafkafi and Tarchitzky, 2011). Thirdly, the price of UP is relatively low, the purchasing prices of UP, PPM
292 and APP mainly ranged \$650 - 840 /t, \$870 - 1090 /t and \$945 - 1310 /t (China fertilizer website, 2019),
293 respectively. Finally, UP can promote the early flowering and fruiting of crops (Becker et al., 2004), as
294 early market entry is of great benefit to raising the price of agricultural products. However, due to
295 excessive fertilization and other reasons, the soil in many areas presents the risk of continuous acidification
296 (Tian and Niu, 2015).

297 Continuous application of UP may further reduce soil pH (Mikkelsen, 1989), thereby threatening the
298 crop growth. Therefore, for acidic and neutral soils, APP might be more suitable through drip irrigation
299 systems with HSW (Kafkafi et al., 2011). The price of fertilizer is also one of the main factors to be
300 considered since the price of APP is comparatively higher. Improper application of APP may lead to the
301 situation of increasing production while not increasing income (Noy and Yoles, 1979). In the case of
302 low-volume drip irrigation of phosphate fertilizer, because of its lower cost and higher fertilizer efficiency,
303 APP fertilizer is more affordable than top-grade packaged monoammonium phosphate (Ottman et al.,
304 2006). However, at present, there are still few agricultural ammonium polyphosphate manufacturers on

305 several agricultural markets such as China, the price is also relatively expensive and the product quality is
306 not very stable (Yin et al., 2018). Therefore, it is urgent to optimize the APP production process and reduce
307 the price.

308 In general, low concentration UP treatment and high concentration APP treatment significantly
309 reduced the risk of emitter clogging. The mechanism of these two new phosphate fertilizers was clarified
310 for reducing emitter clogging using HSW, and put forward the suitable fertilization mode of UP and APP.
311 However, the effects of local soil type, fertilizer cost and availability should also be considered.
312 Meanwhile, there are two aspects worth exploration in the future: (1) The effects of different phosphorus
313 fertilizer types on-site soil conditions and crop growth under drip irrigation with HSW, (2) Both UP and
314 APP slow down the emitter clogging by inhibiting the formation of carbonate and increase the risk of
315 silicate. Therefore, different results may be produced for water sources with different compositions, e.g.,
316 more silicates, less calcium and magnesium, etc.

317 **5. Conclusions**

318 (1) The application of UP and APP can effectively alleviate the emitter clogging in drip fertigation
319 systems with HSW. Compared with non-fertilization, *Dra* was increased by 25.0% - 45.0% and 46.3% -
320 73.6%, *CU* increased by 26.2% - 44.5% and 46.1% - 74.6%, and *DW* decreased by 21.1% - 28.6% and
321 32.2% - 42.0% with UP and APP, respectively. In contrast, MKP accelerated emitter clogging issues.

322 (2) Phosphate fertilizer significantly changed the content of different minerals inside emitters.
323 Compared with non-fertilization, the carbonate content of MKP, UP and APP decreased by 50.4% - 59.2%,
324 66.0% - 81.5% and 74.1 - 76.2%, silicate increased by 56.1% - 234.9%, 46.6% - 102.8% and 21.3% -

325 75.8%, quartz content increased by 448.2% - 657.6%, 218.3% - 462.2% and 146.1% - 396.3%,
326 respectively. Phosphate precipitation was found in all the clogging materials treated by fertilization.

327 (3) Different fertilization concentration significantly affected emitter clogging. Compared with the
328 UP_0.15, *Dra* and *CU* of UP_0.30 decreased by 36.3% and 33.1%, *DW* increased by 9.7%. The *Dra* and
329 *CU* of APP_0.30 increased by 50.9% and 52.7% and *DW* decreased by 14.7%. It is recommended that UP
330 should choose low concentration and long term (LCLT) and APP should choose high concentration and
331 short term (HCST) as the fertilization mode of high saline drip irrigation system.

332 **Acknowledgements**

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334 and the National Natural Science Fund of China (51790531, 51621061). Authors thank New Mexico State
335 University Agricultural Experiment Station for support.

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Captions for Figures and Tables in the Paper

457 Fig. 1. Layout of HSW drip irrigation experimental system.

458 Fig. 2. Correlation of emitter performance parameters between CK and fertilization treatments.

459 Fig. 3. Correlation of *DW* between CK and fertilization treatments.

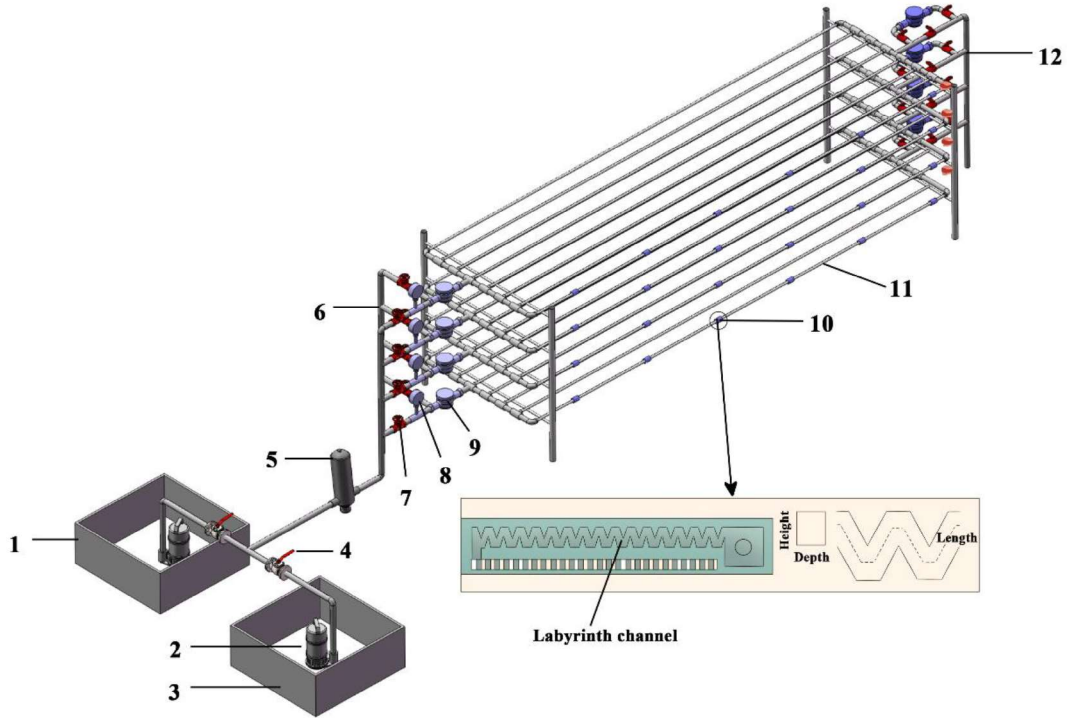
460 Fig. 4. Mineral components in each treatment obtained at the end of the experiment (E1).

461 Fig. 5. Correlation of mineral constituent treatments.

462 Fig. 6. Correlation between the mineral composition and *CU* for the different emitters.

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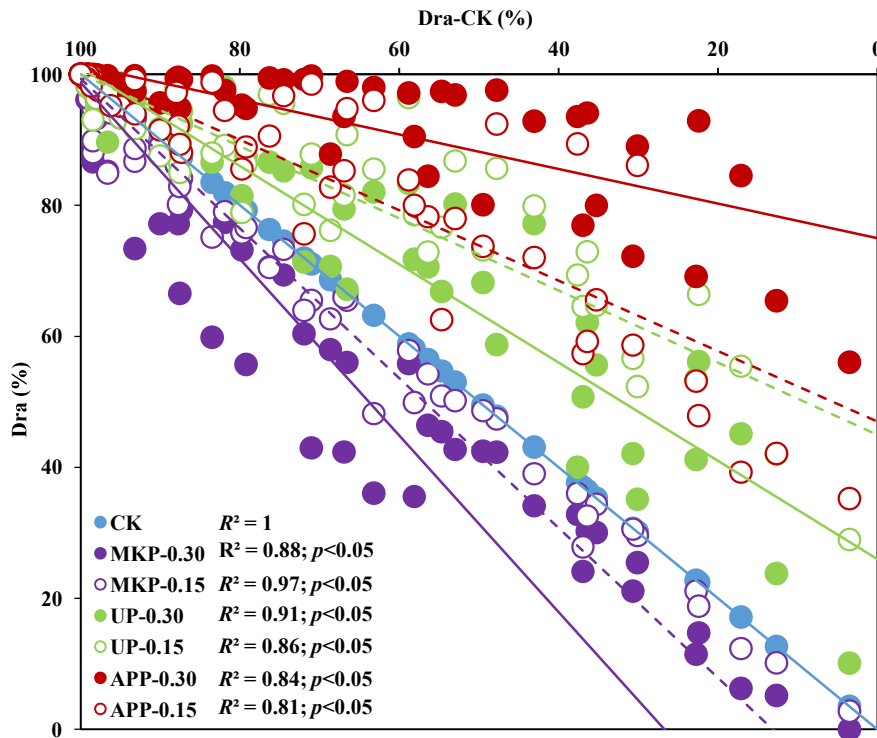
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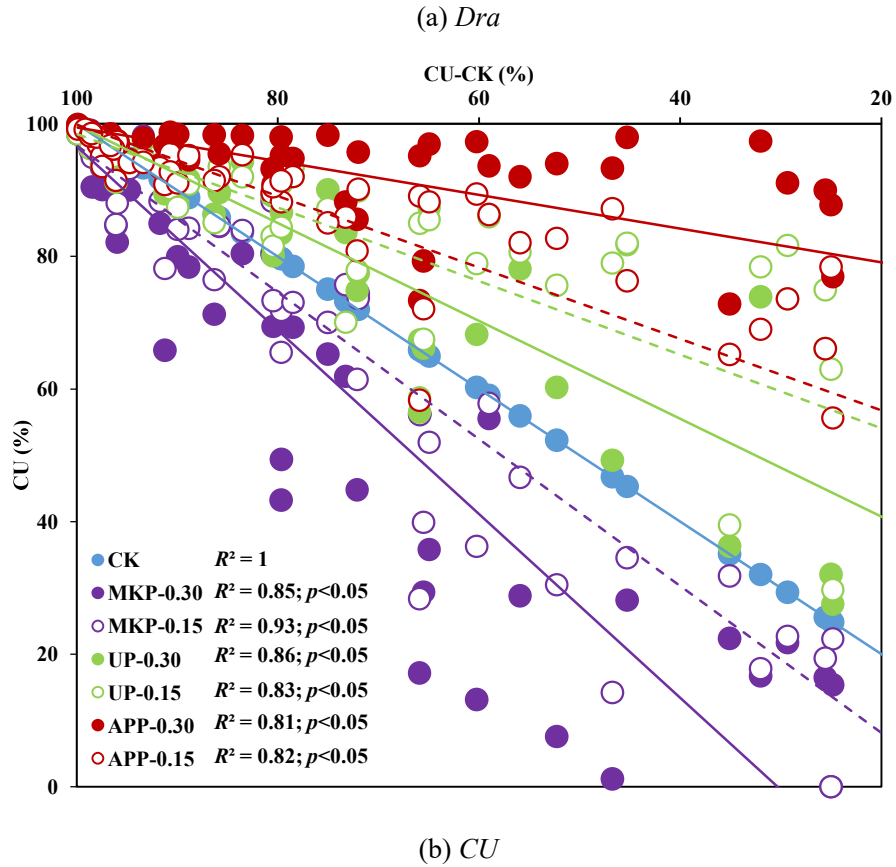
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467 1 - Water tank, 2 - Water pump, 3 - Fertigation tank, 4 - Butterfly valve, 5 - Disc filter, 6 - Pipes, 7 - Sub
468 valve, 8 - Pressure gauge, 9 - Flowmeter, 10 - Drip emitter, 11 - Drip lateral, 12 - Flushing devices.

469 **Fig. 1.** Layout of HSW drip irrigation experimental system.



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Fig. 2. Correlation of emitter performance parameters between CK and fertilization treatments.

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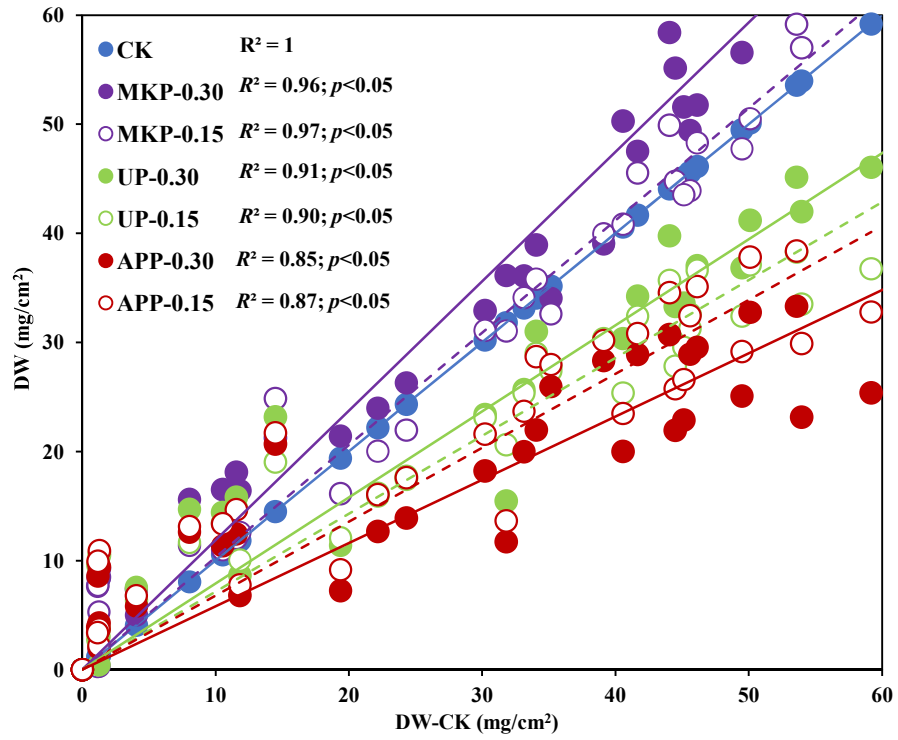
Note: The x - axis is the *Dra* or *CU* of CK, and the y - axis is the *Dra* or *CU* across different treatments. p

476

< 0.05 indicate the treatments are significantly different. The detailed variations for *Dra* and *CU* are shown

477

in Fig. A3 and Fig. A4.



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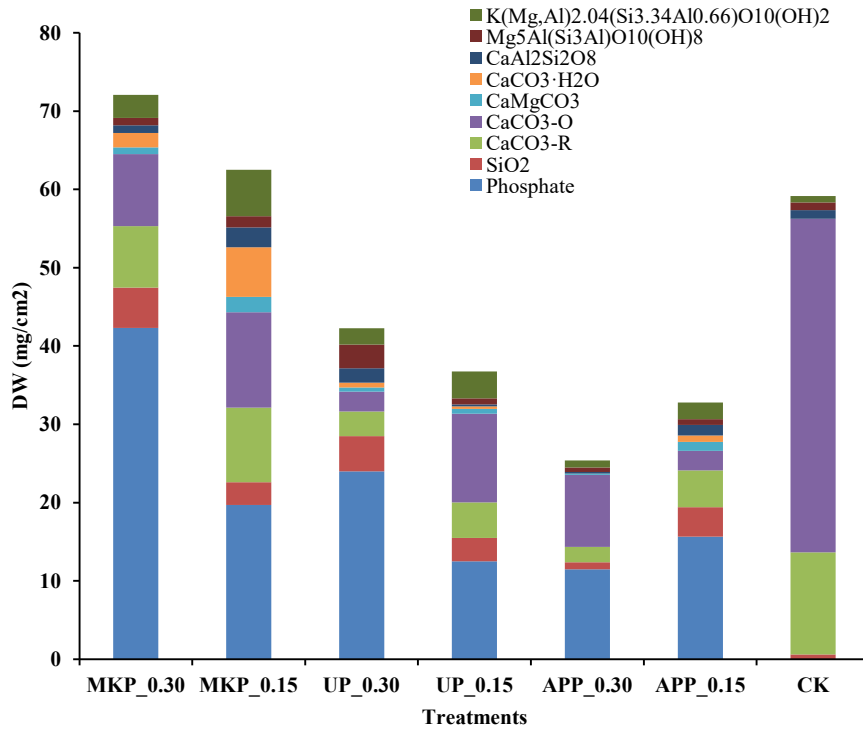
479

Fig. 3. Correlation of *DW* between CK and fertilization treatments.

480

Note: The detailed variation of *DW* is shown in Fig. A5.

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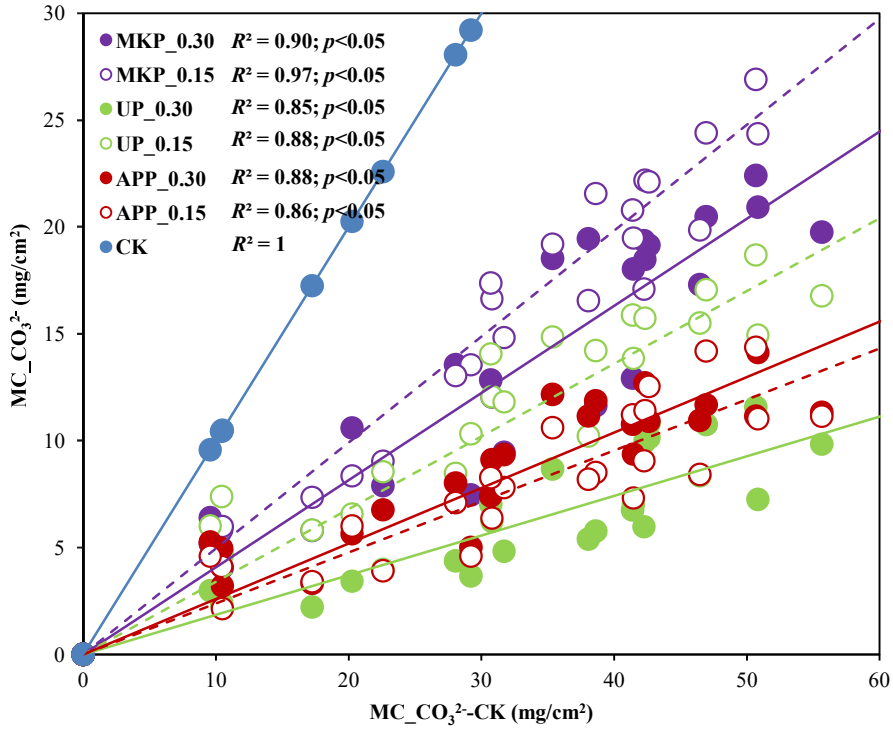


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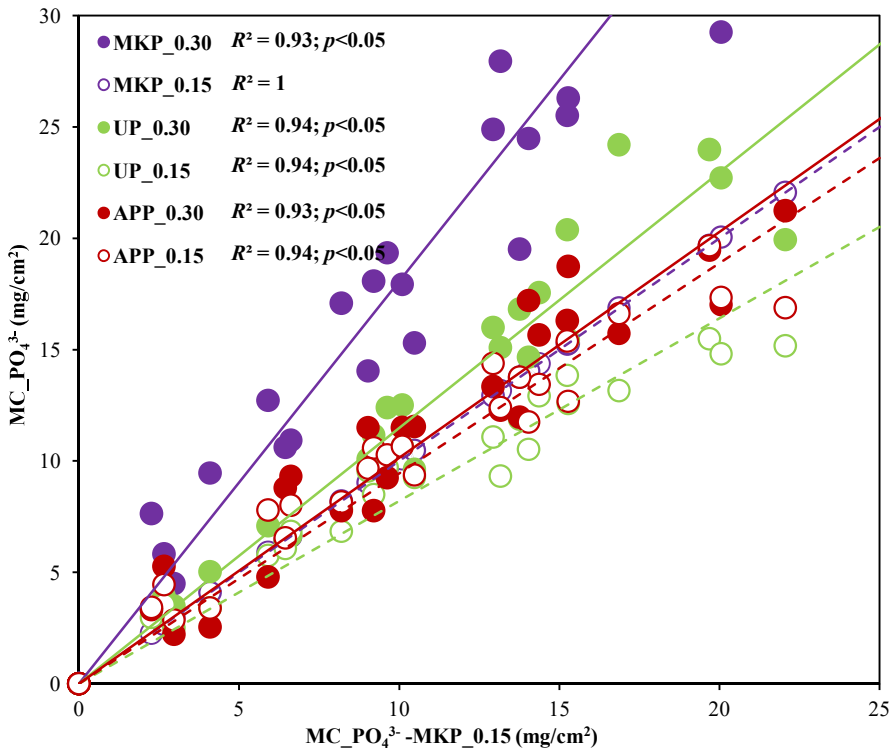
483 **Fig. 4.** Mineral components in each treatment obtained at the end of the experiment (E1)

484 Note: As the mineral components were similar across different types of emitters and different periods, only
 485 results of FE1 at the end of the periods are shown as an example. Other emitters and periods are shown in
 486 Fig. A6. The proportions of each mineral component are shown in Fig. A9.

487



(a) Carbonate



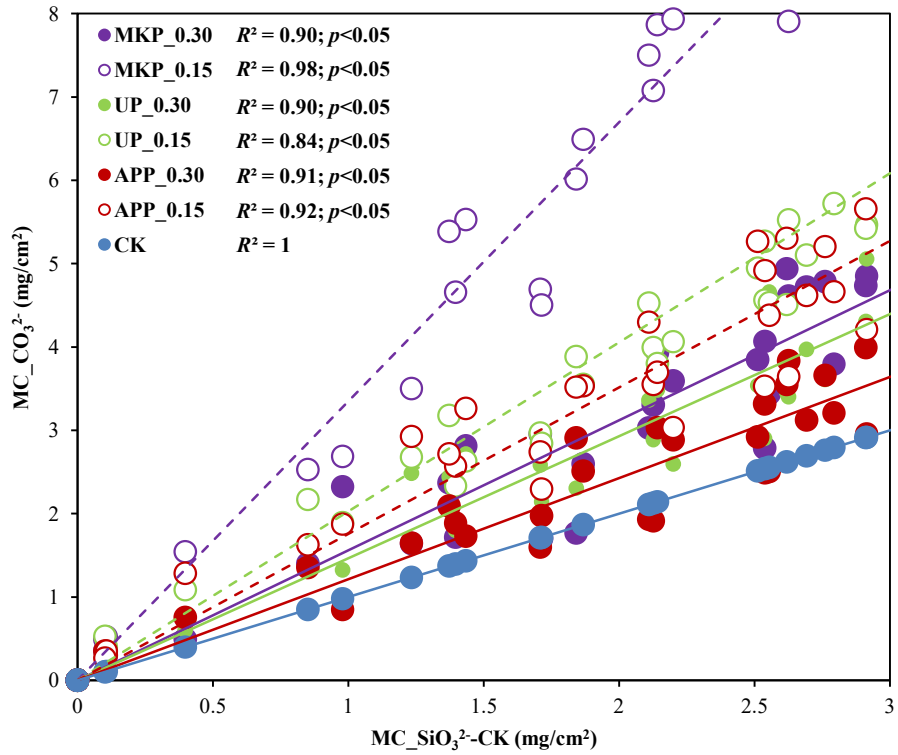
(b) Phosphate

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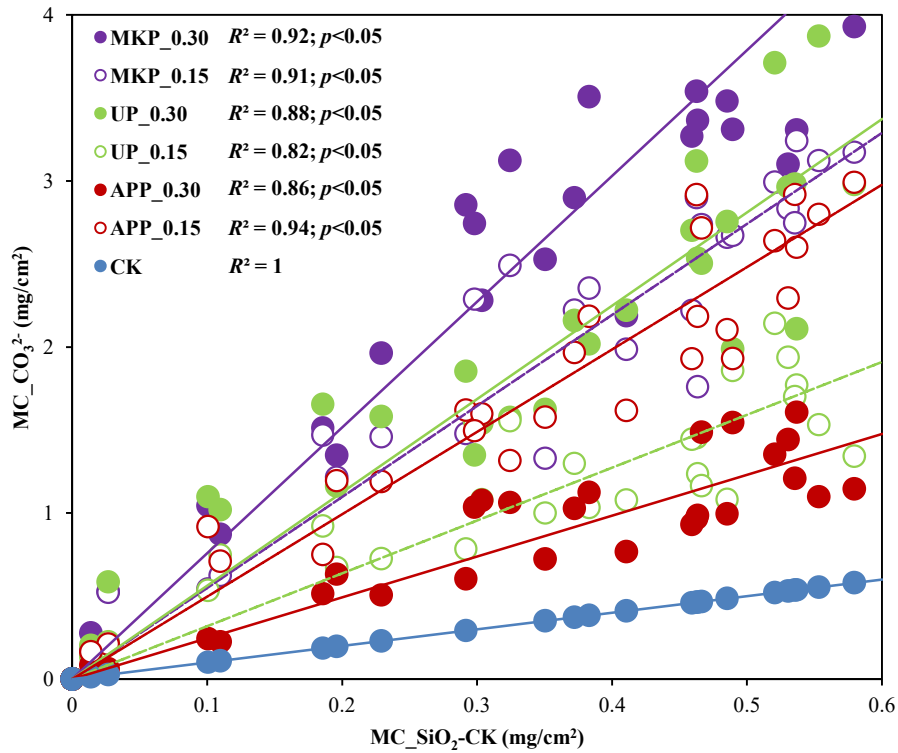
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(c) Silicate



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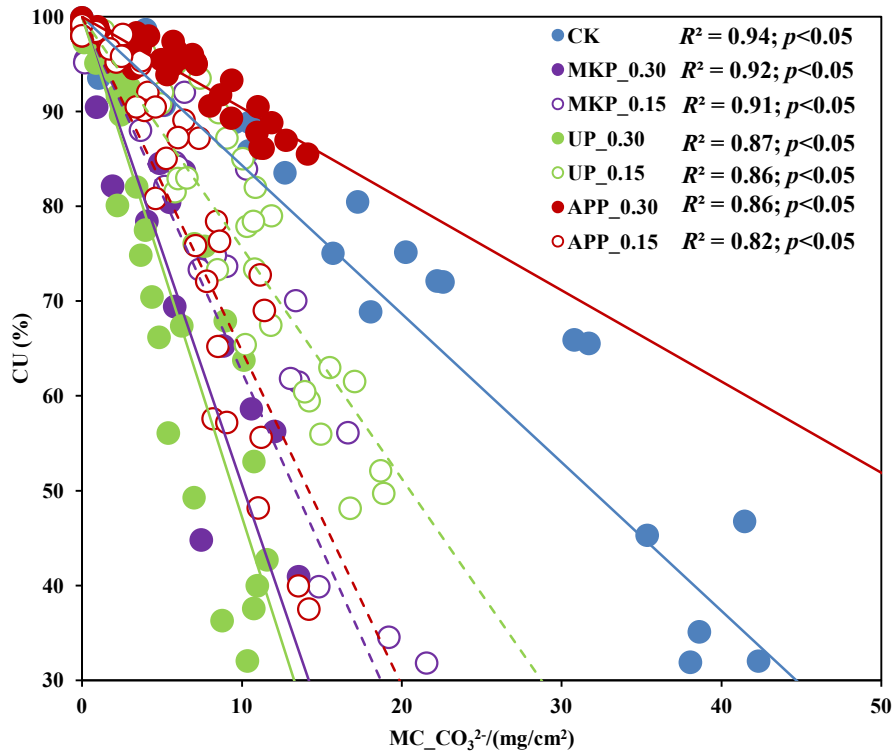
(d) Quartz

Fig. 5. Correlation of mineral constituent treatments.

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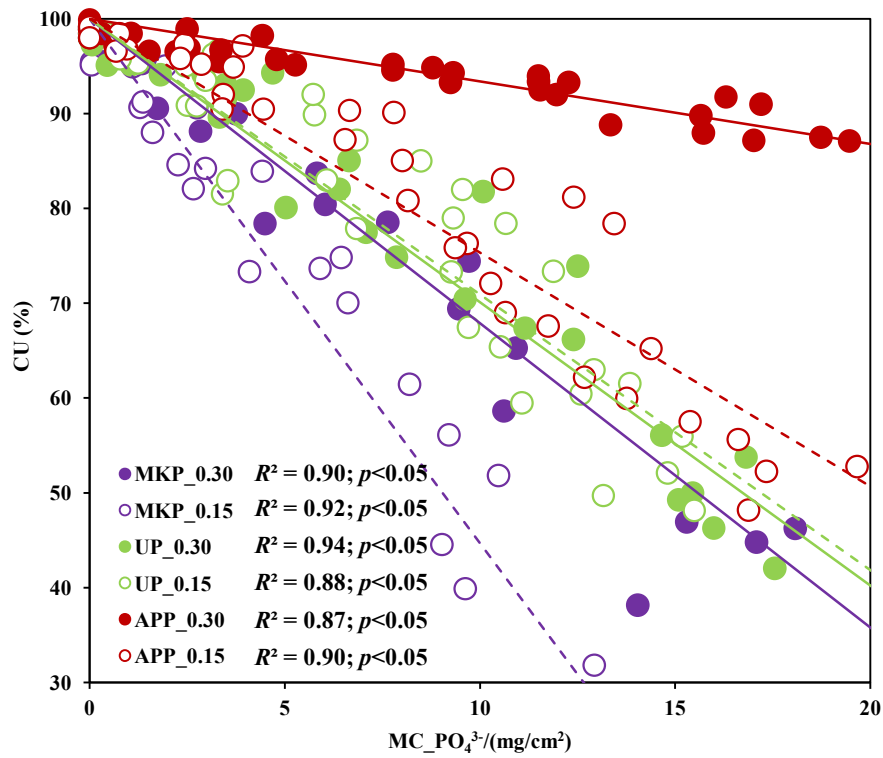
Note: The detailed variations of minerals are shown in Fig. A10.



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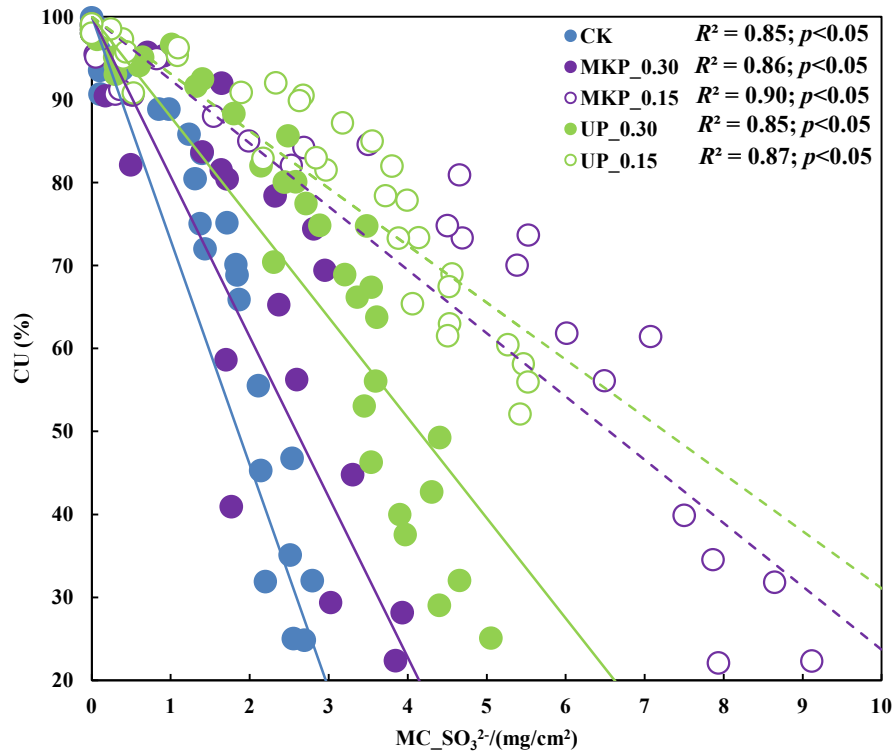
(a) Carbonate



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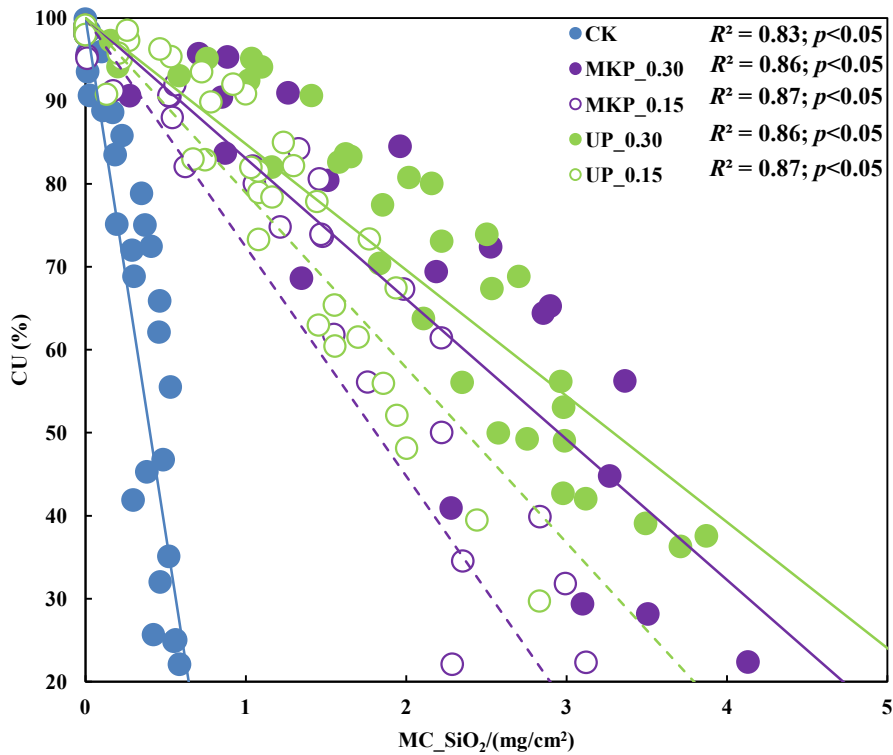
(b) Phosphate



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(c) Silicate



504

505

(d) Quartz

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Fig. 6. Correlation between the mineral composition and *CU* for the different emitters.

507

SUPPLEMENTARY MATERIALS for

Using Phosphate Fertilizer to Reduce Emitter Clogging of Drip

Fertigation Systems with High Salinity Water

Correspondence to: liyunkai@126.com

1. Supplementary information in *Experimental section*

1.1. Preparation of phosphate fertilizer

The UP was produced by continuous thermal manufacturing process. The main reaction conditions were as follows: the concentration of phosphoric acid was 80% -85 %, the molar ratio of phosphoric acid to urea was 1:1.00 - 1.05, the reaction temperature was 75 - 85 °C, and the reaction time was 30 min. Its product index was P₂O₅ 45.12%, N 17.24%. Based on the preparation of UP, APP was produced by urea phosphate-phosphorus pentoxide polymerization. The ratio of UP to phosphorus pentoxide was 4.44:1, the reaction temperature was 218.93 °C, and the reaction time was 70.82 min. Under these conditions, the polymerization degree of APP was 23.64, and the solubility was 2.24 g/100g H₂O. MKP was produced by neutralization method. Add 30% potassium carbonate solution to the neutralizer, then add 50% phosphoric acid solution and stir. The reaction temperature was 75 - 85 °C, and pH was ranged 4 - 5. The neutralized product was filtered, concentrated, cooled, crystallized, centrifuged and dried to obtain the finished product. The crystallization mother liquor was returned to the concentration section for reuse. UP, APP, and MKP were produced at Shandong Kingenta Eco-engineering Co., Ltd.

1.2. Ranges of water quality parameters

Table A1. Ranges of water quality parameters.

| pH | Ca ²⁺ mg/L | Mg ²⁺ mg/L | Fe ³⁺ mg/L | Mn ²⁺ mg/L | TH mg/L | TDS mg/L |
|-------------|--------------------------|--------------------------|--------------------------|--------------------------|------------|-------------|
| 7.50 - 7.55 | 77 - 85 | 78 - 86 | 0.051 - 0.054 | 0.114 - 0.132 | 518 - 535 | 1016 - 1058 |

Note: Water quality parameters were tested by Pony Testing International Group Co., Ltd., China. pH was measured by pH meter. Ca²⁺, Mg²⁺, Fe³⁺ and Mn²⁺ were tested by inductively coupled plasma optical emission spectrometry. Total hardness was tested by burettes. Total dissolved solids were tested by electric blast drying oven and analytical balance.

1.3. Geometrical characteristic of emitters used in the experiment

Table A2. Geometrical characteristic of emitters used in the experiment.

| Emitter | Rated discharge(L/h) | Flow path dimensions (mm) | | | Discharge coefficient | Flow index |
|---------|----------------------|---------------------------|-------|-------|-----------------------|------------|
| | | Length | Width | Depth | | |
| E1 | 0.95 | 85.0 | 0.55 | 0.51 | 3.10 | 0.51 |
| E2 | 1.40 | 47.0 | 0.56 | 0.55 | 4.90 | 0.51 |
| E3 | 1.60 | 19.0 | 0.55 | 0.49 | 5.20 | 0.51 |
| E4 | 2.00 | 24.5 | 0.61 | 0.60 | 6.50 | 0.61 |

Note: The flow path dimensions were obtained by an electron microscope after peeling the emitters, and the rated discharge, discharge coefficient, flow index were tested according to China standard (GB/T17188 - 1997).

1.4. Drip fertigation/irrigation schedules

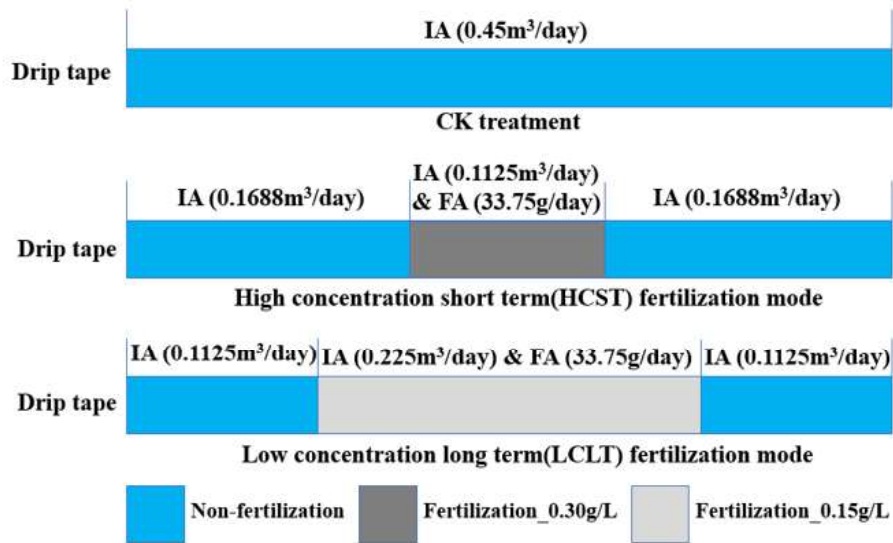


Fig. A1. Drip irrigation system composition Fertigation and/or irrigation schedules with different fertilizer concentrations.

Note: IA, irrigation amount; FA, fertilization amount. Fertilization_0.30 g/L and Fertilization_0.15 g/L represent that the concentrations of fertilizer were 0.30 g/L and 0.15 g/L, respectively. The IA and FA were the same in two fertigation modes (HCST and LCLT), and the amount of irrigation and fertilization per drip irrigation lateral (18 m) was $0.45\text{ m}^3/\text{d}$ and $33.75\text{ g}/\text{d}$ respectively. The two fertigation modes were adopting the “(1) Non-fertilization (Only irrigation); (2) Fertigation; and (3) Non-fertilization” operating schedules, and the fertilization was applied at the center of the whole operation time. Besides, the fertigation treatments were not applied every day, the system fertigation ran every other day.

1.5. Evaluation parameters for emitter performance (*Dra* and *CU*)

The theoretical maximum and minimum values of *Dra* were 100% (initial value, non-clogging) and 0% (complete-clogging), respectively. *Dra* was calculated as follows.

$$Dra = \frac{\sum_{i=1}^n \frac{q_i^t}{q_i^0}}{n} \times 100\% \quad (1)$$

Where q_i^0 is initial flow rate for emitter i , in L/h; q_i^t is flow rate for emitter i at t days, in L/h; and n is the total number of emitter installed along the lateral.

CU values were less than 100% (100% indicates all the emitters along a lateral has same flow rate).

CU was calculated follows.

$$CU = 100 \left(1 - \frac{\sum_{i=1}^n |q_i^t - \bar{q}^t|}{n\bar{q}^t} \right) \quad (2)$$

Where \bar{q}^t is average flow of each emitter along the lateral at t time, in L/h; and other parameters are defined in Eq. (1).

1.6. Diffraction pattern of crystal

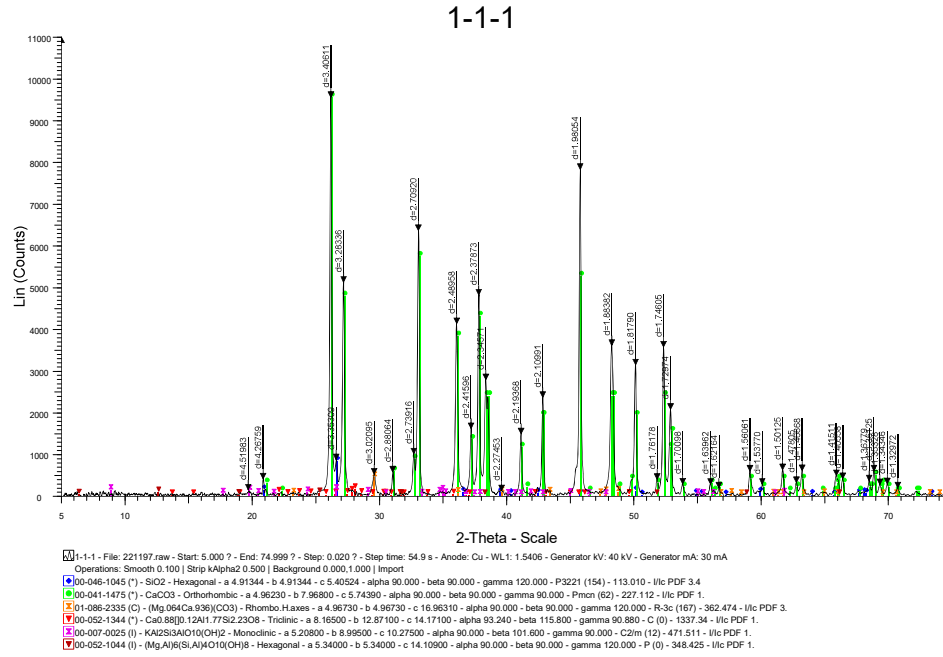


Fig. A2. Polycrystalline diffraction patterns of the emitter clogging substances (E1 as an example).

2. Supplementary information in *Results section*

2.1. Dynamic variation of *Dra*

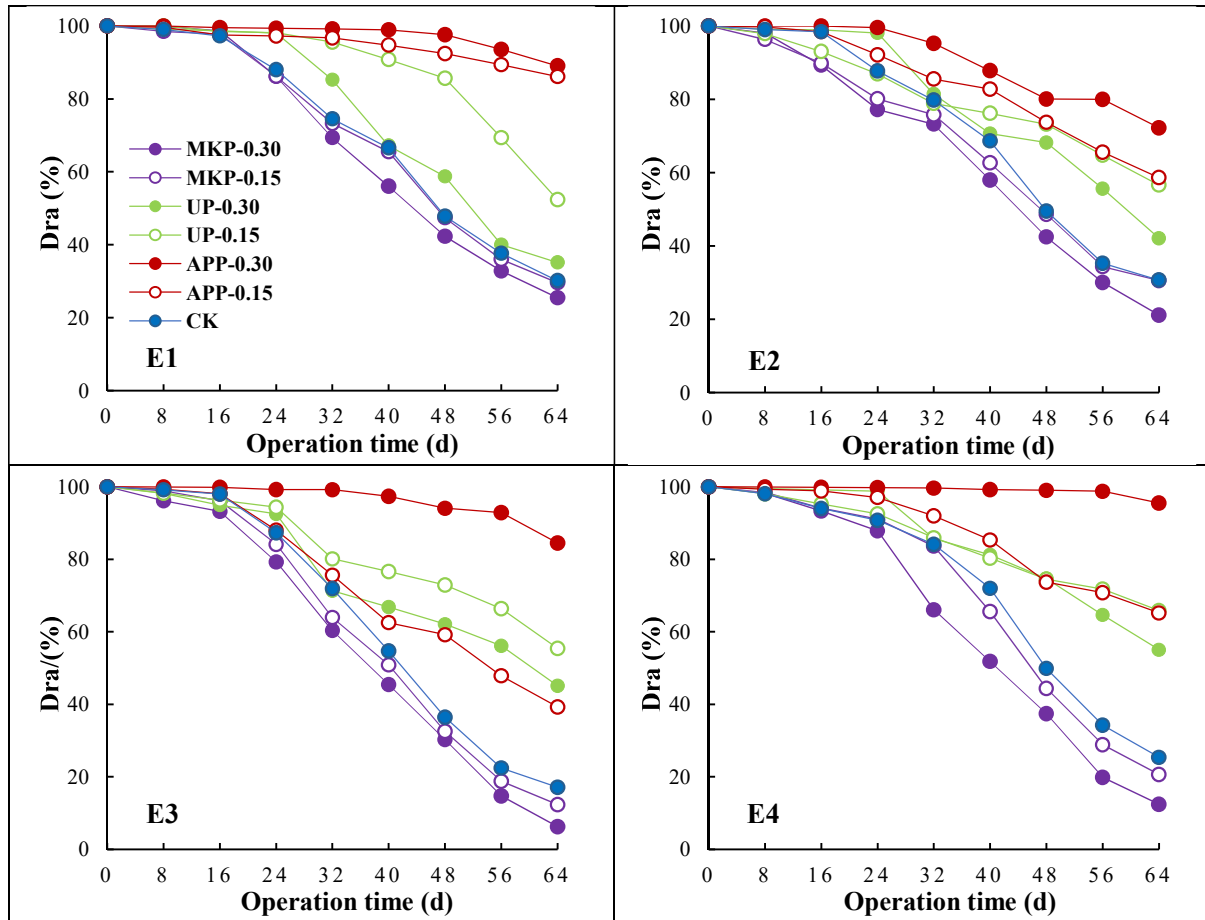


Fig. A3. Dynamic variation of *Dra* for the different emitters (E1-E4) and fertilization treatments.

2.2. Dynamic variation of *CU*

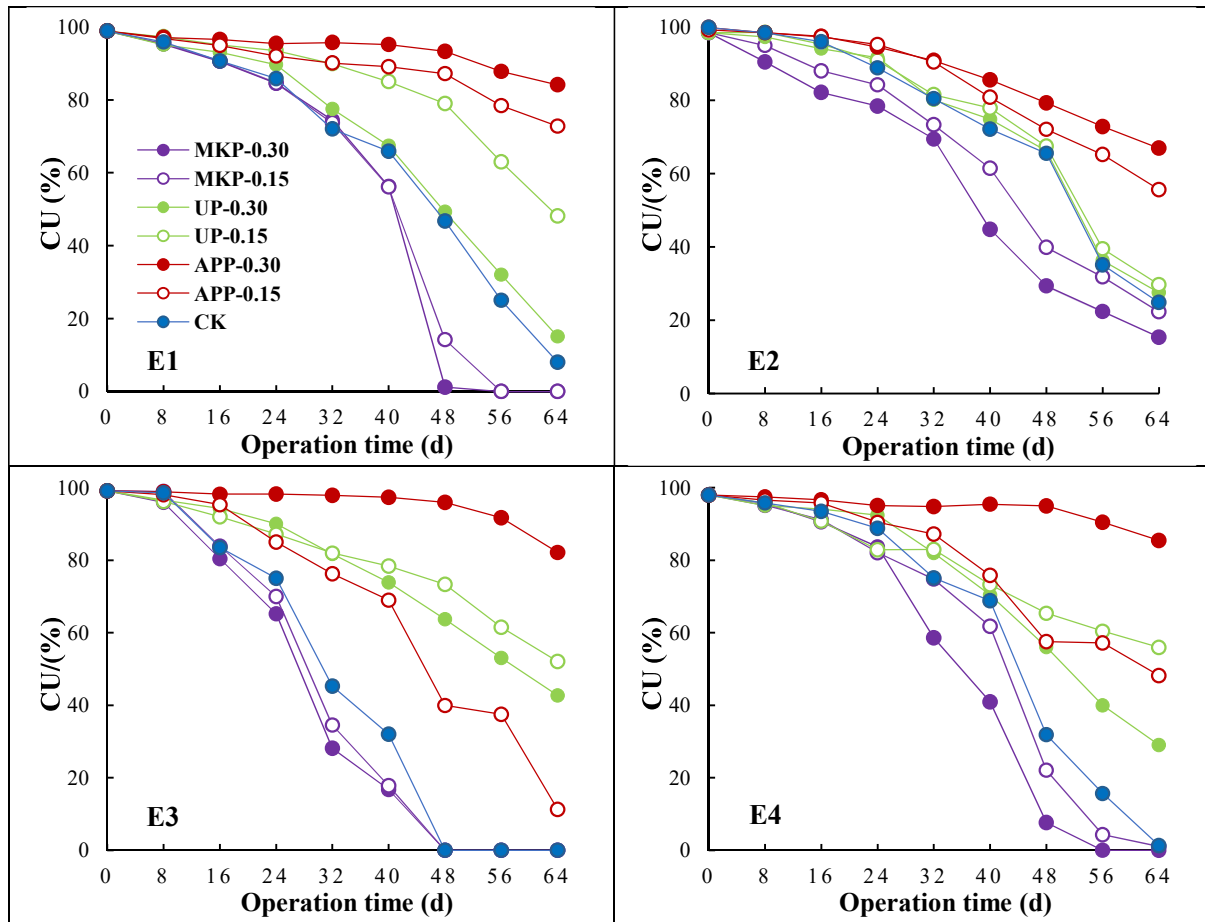


Fig. A4. Dynamic variation of *CU* for the different emitters (E1-E4) and fertilization treatments.

Table A3. Paired samples t-test of emitter clogging parameters in different treatments.

| Treatments | CK | MKP_0.15 | UP_0.15 | APP_0.15 | MKP_0.30 | UP_0.30 | APP_0.30 |
|------------|----|----------|---------|----------|----------|---------|----------|
| CK | — | ** | ** | ** | ** | ** | ** |
| MKP_0.15 | ** | — | ** | ** | ** | ** | ** |
| UP_0.15 | ** | ** | — | NS | ** | ** | ** |
| APP_0.15 | ** | ** | NS | — | ** | * | ** |
| MKP_0.30 | ** | ** | ** | ** | — | ** | ** |
| UP_0.30 | ** | ** | ** | * | ** | — | ** |
| APP_0.30 | ** | ** | ** | ** | ** | ** | — |

Note: asterisks indicate that differences between treatments are significant at $p < 0.05$ (*) or $p < 0.01$ (**), and NS means not significant at $p < 0.05$. The upper right is *Dra*, the lower left is *CU*.

2.3. Dynamic variation of dry matter weight

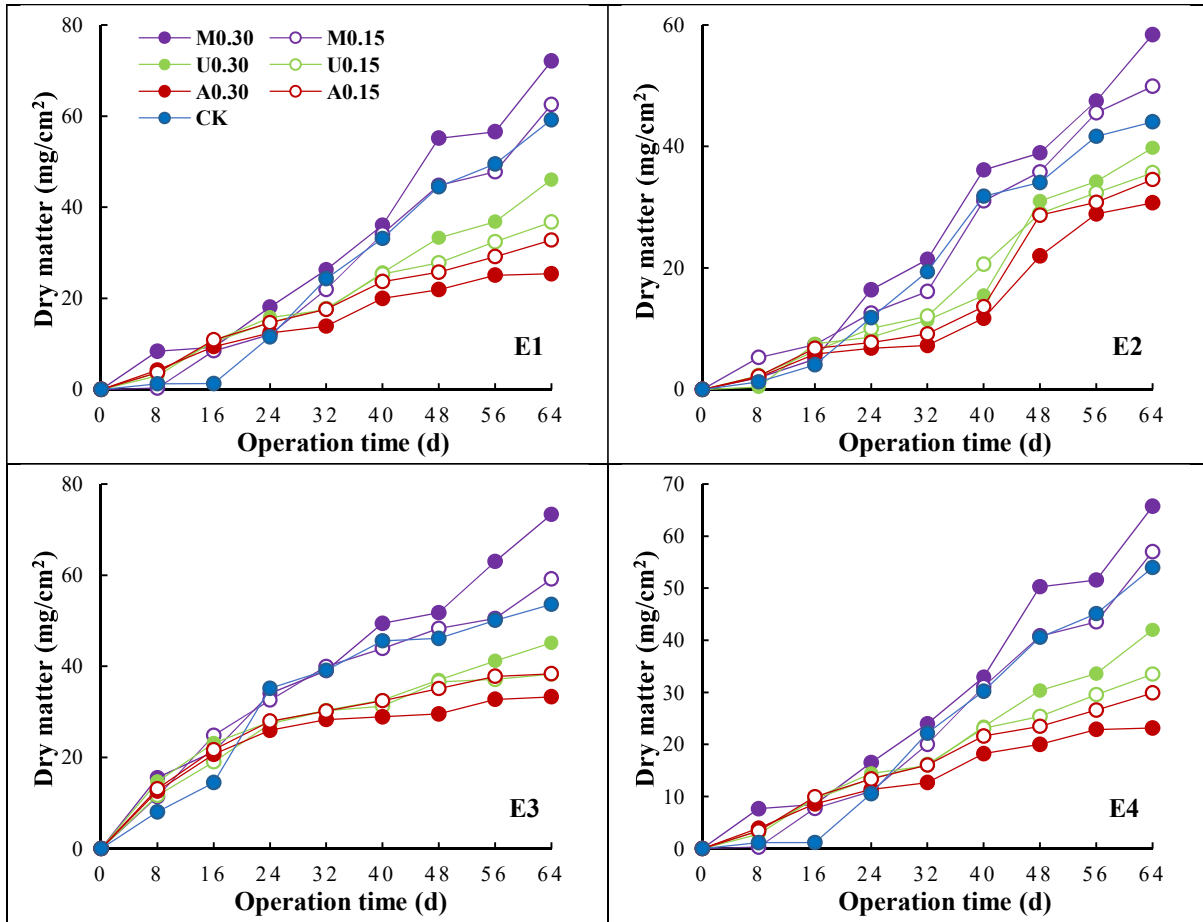


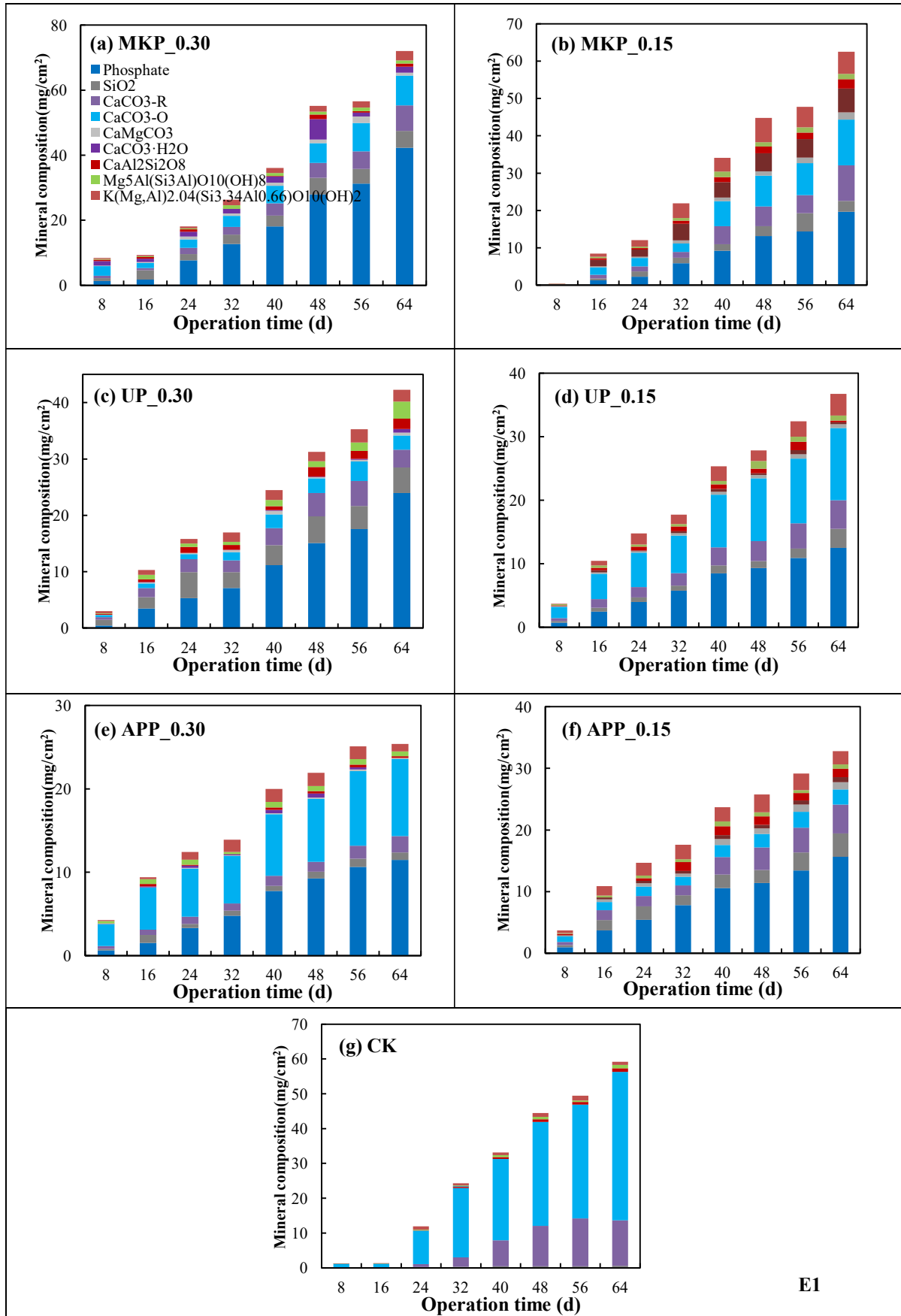
Fig. A5. Dynamic variation of dry matter weight for the different emitters and fertilization treatments.

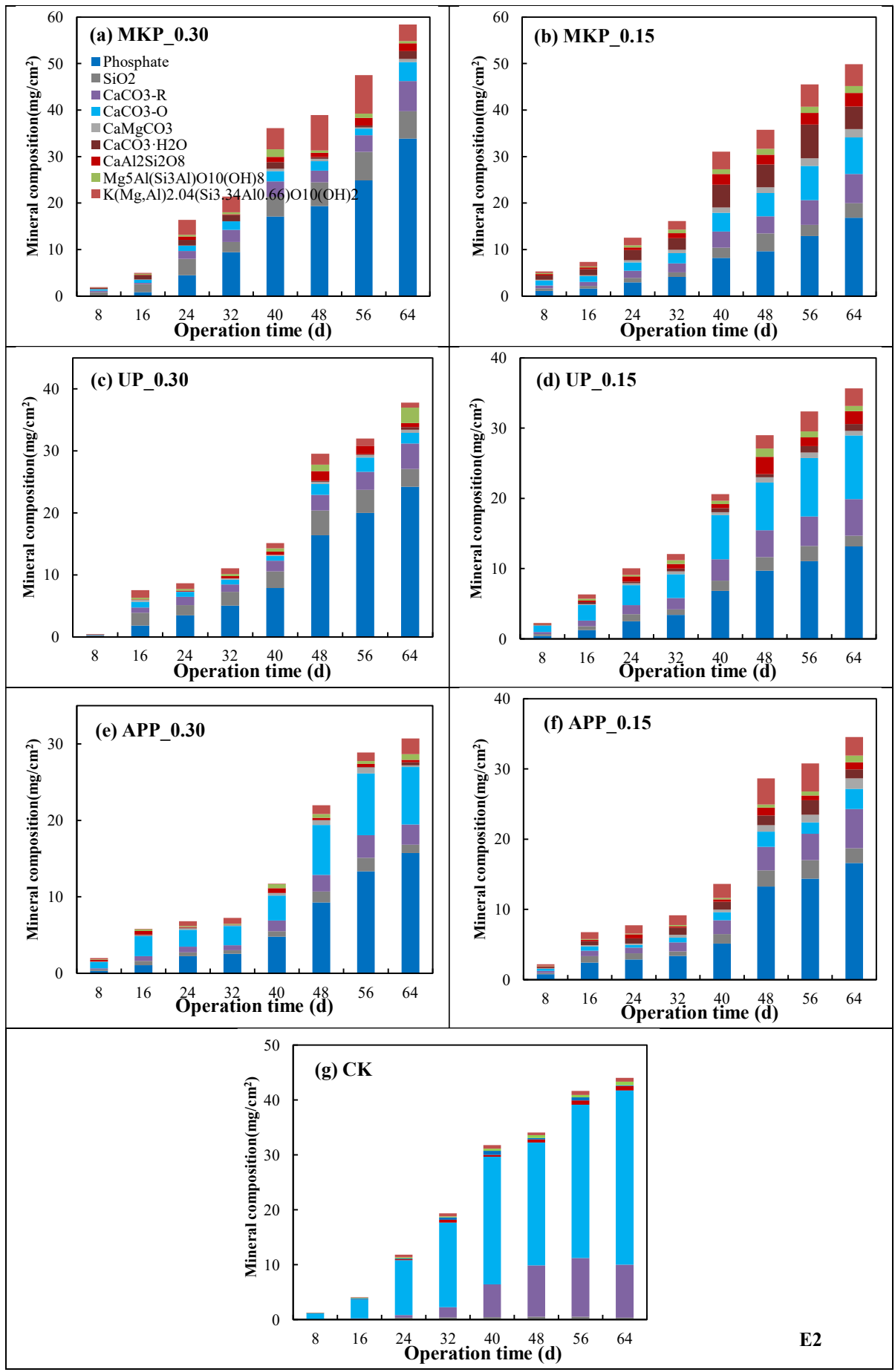
Table A4. Paired samples t-test of emitter clogging DW in different treatments.

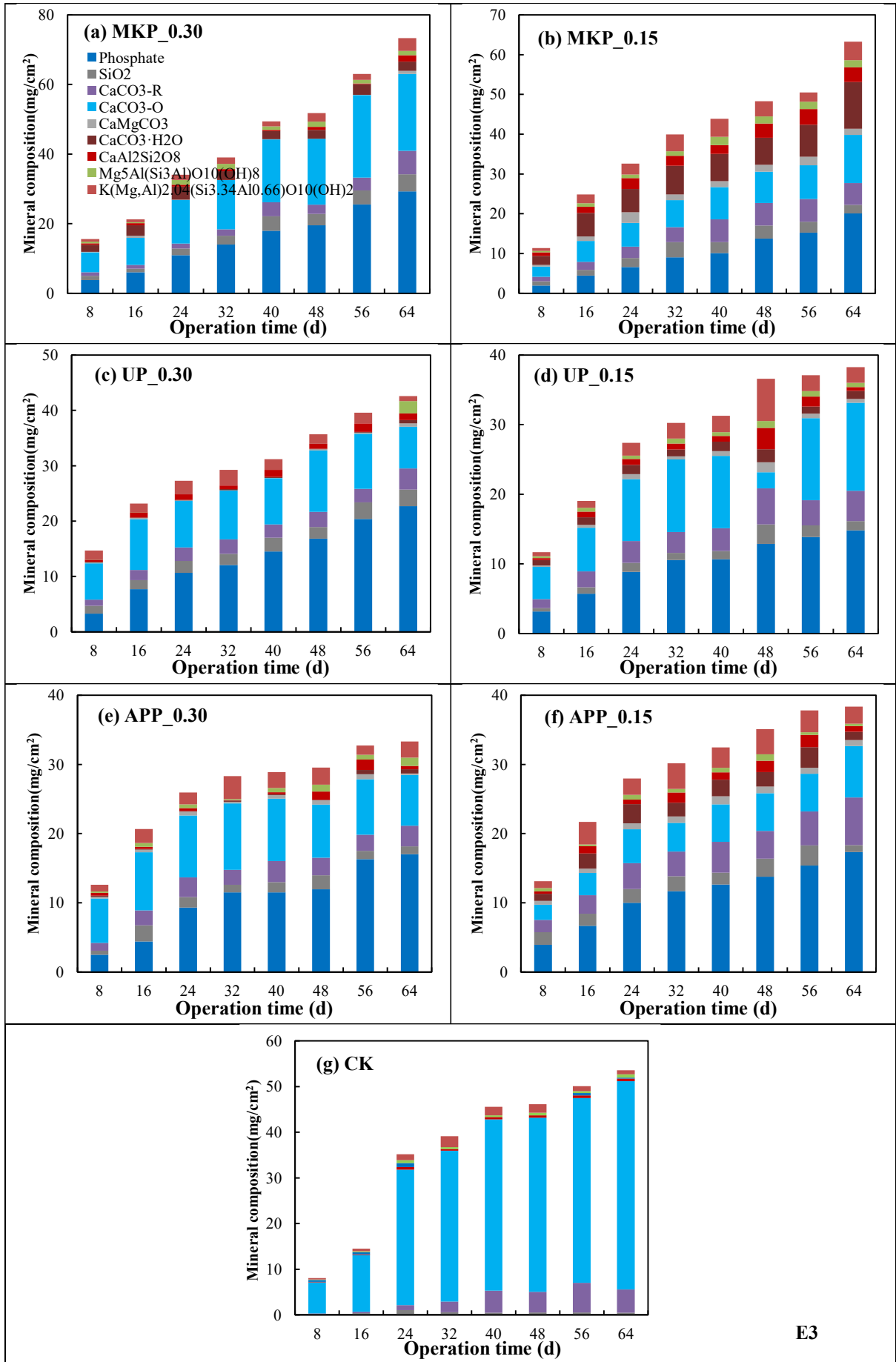
| Treatments | CK | MKP_0.15 | UP_0.15 | APP_0.15 | MKP_0.30 | UP_0.30 | APP_0.30 |
|------------|----|----------|---------|----------|----------|---------|----------|
| CK | — | * | ** | ** | ** | ** | ** |
| MKP_0.15 | | — | ** | ** | ** | ** | ** |
| UP_0.15 | | | — | ** | ** | ** | ** |
| APP_0.15 | | | | — | ** | ** | ** |
| MKP_0.30 | | | | | — | ** | ** |
| UP_0.30 | | | | | | — | ** |
| APP_0.30 | | | | | | | — |

Note: asterisks indicate that differences between treatments are significant at $p < 0.05$ (*) or $p < 0.01$ (**).

2.4. Basic mineral components of clogging substances found inside emitters (E1-E4).







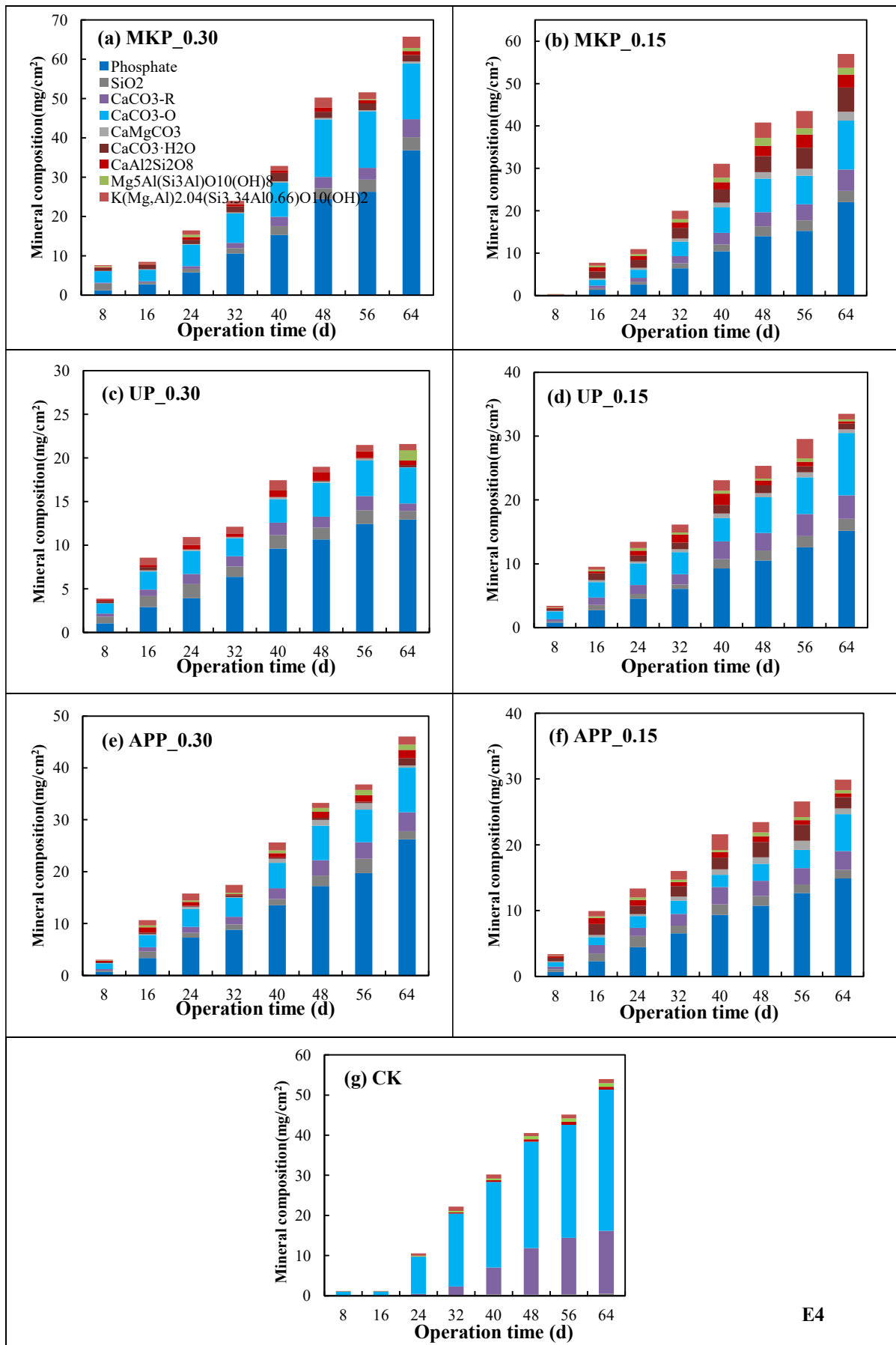


Fig. A6. Dynamic change of the mineral components for the different emitters and fertilizer treatments.

2.5. Determination of amorphous composition in MKP, UP and APP treatments

In order to further explore the specific composition of non-crystalline part of clogging substance in emitter under the condition of phosphate fertilizer application in drip irrigation of high salinity water, the component of amorphous components was tested with a Fourier transform infrared spectrometer (FTIR) (manufacturer: PerkinElmer, USA; type: PE Spectrum 400), and scanning electron microscope with an energy Dispersive Spectrometer (SEM-EDS) (manufacturer: Jeol, Japan, type: JSM-6510A). The results of FTIR and SEM-EDS are shown in Fig. A7 and Fig. A8. Fig. A7 indicated that organic substances were not present in amorphous substances. Also, we observed that the microscope views (SEM) across the three types of fertigation treatments varied greatly (Fig. A8), and EDS results (Fig. A8) demonstrated that the clogging substances in the three treatments contained many phosphorus and calcium elements. Thus, the results in the three figures suggested that amorphous components were phosphate.

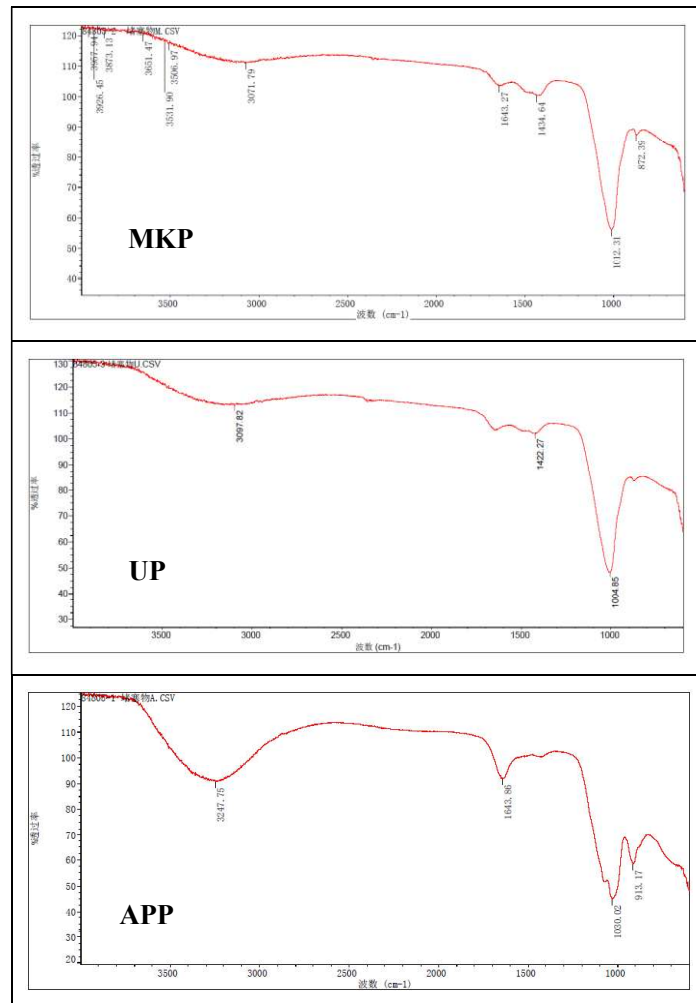


Fig. A7. Infrared spectrum.

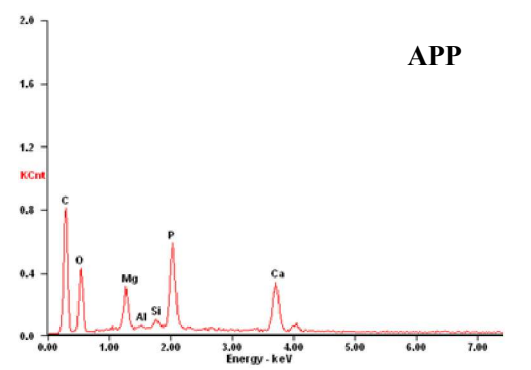
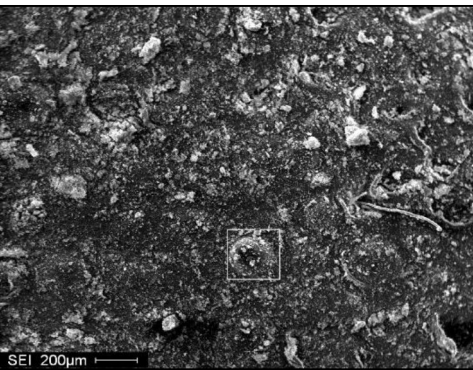
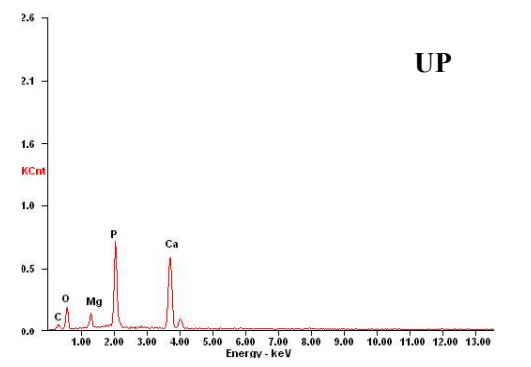
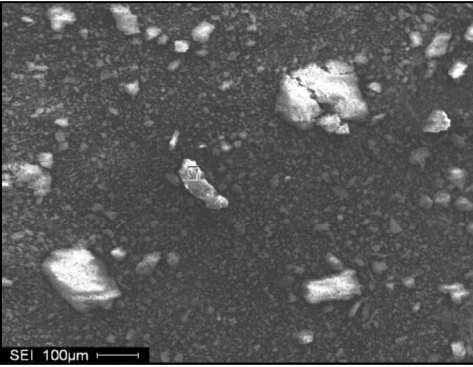
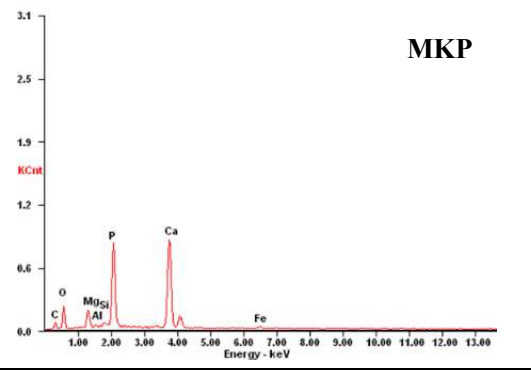
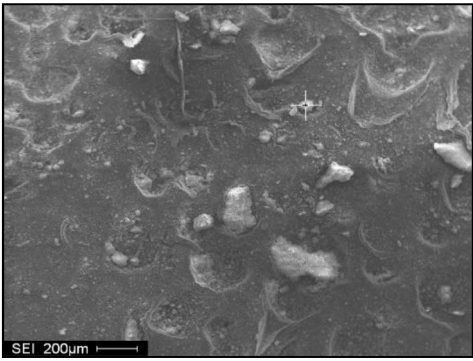


Fig. A8. Scanning electron microscope (SEM) and X-ray energy spectrum analysis.

2.6. Dynamic variation of mineral components

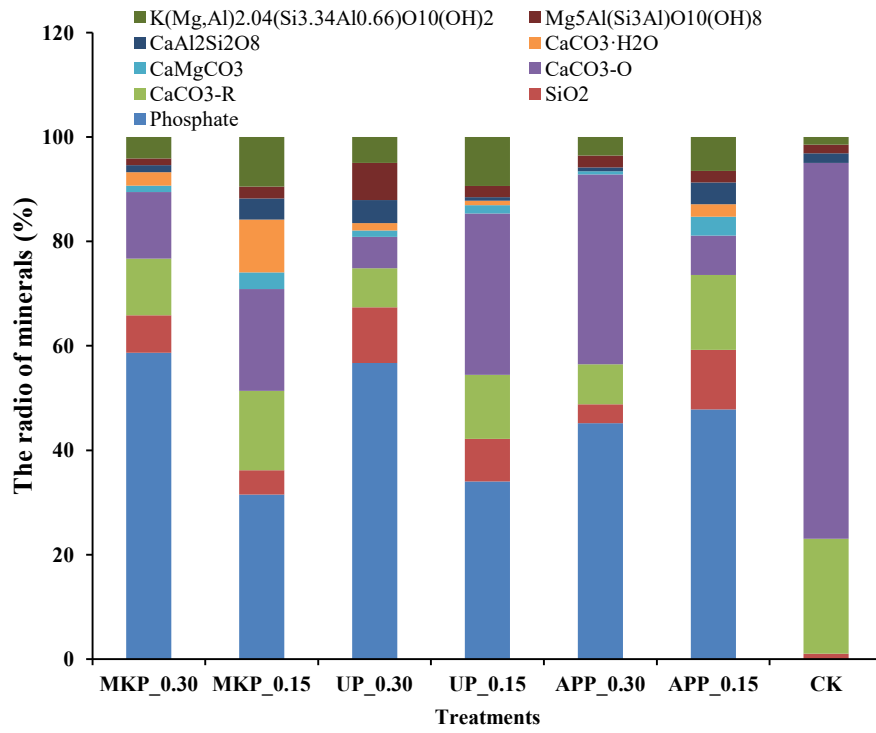
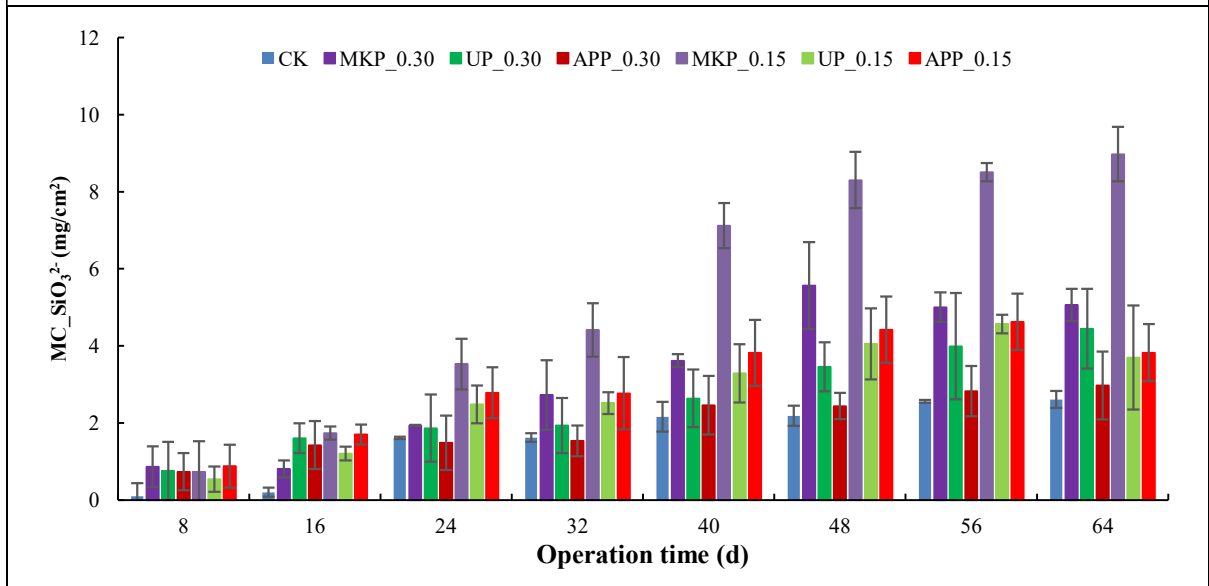
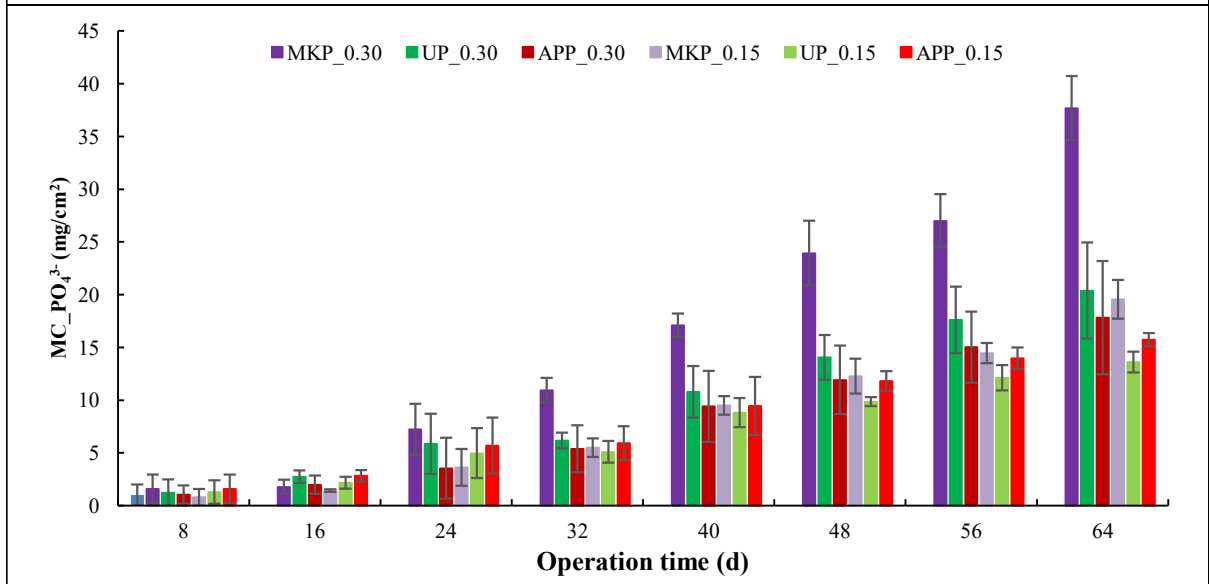
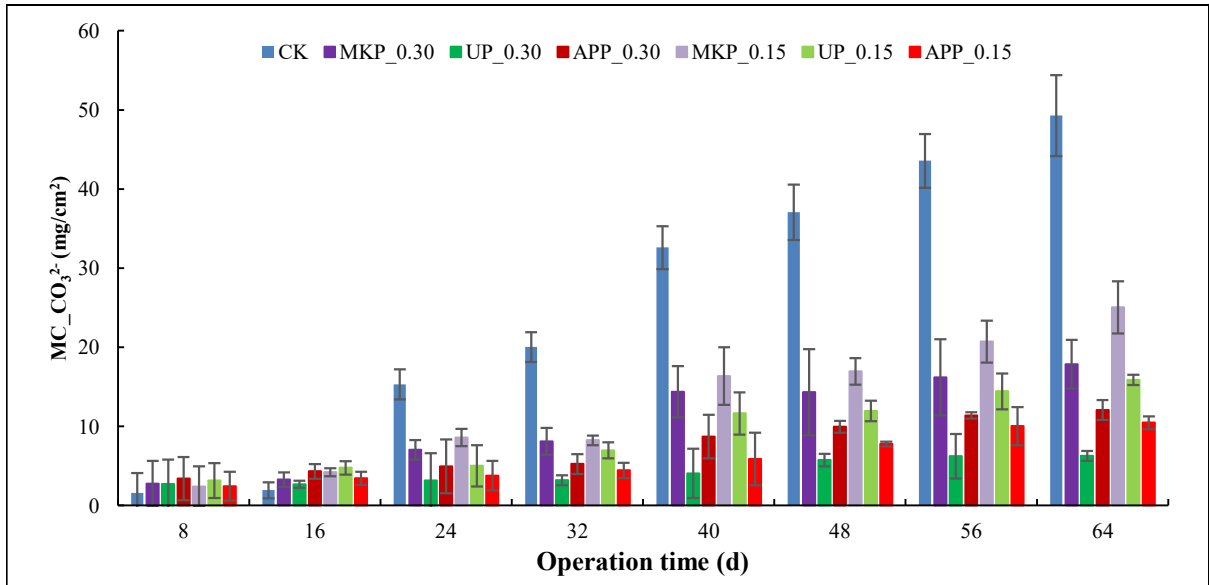


Fig. A9. The proportion of mineral components in 7 treatments.



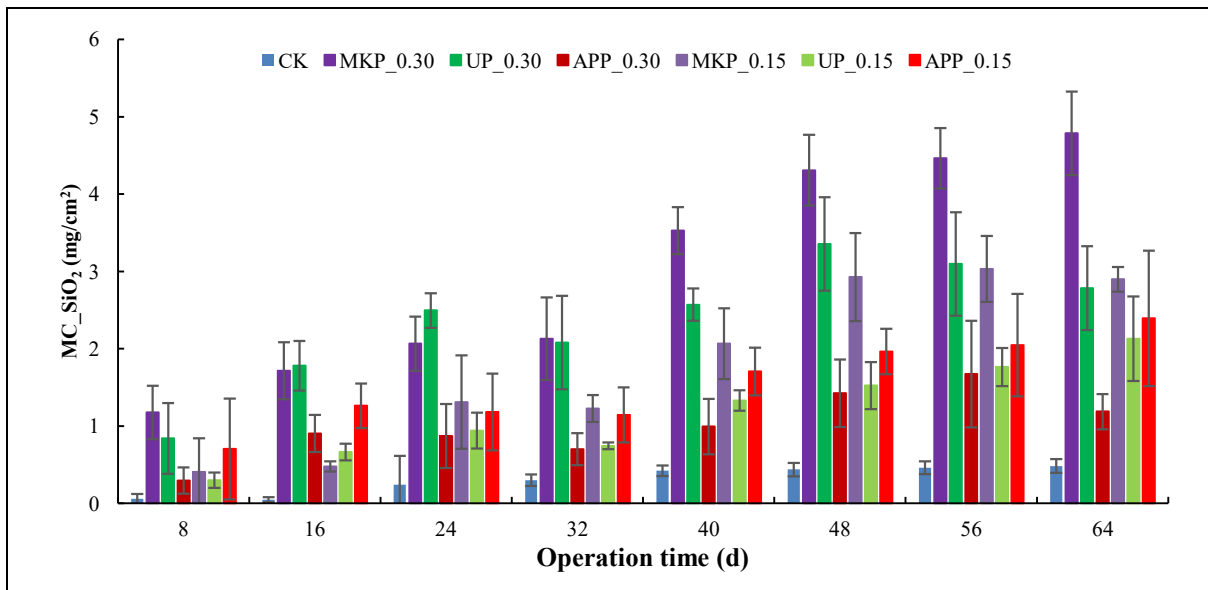


Fig. A10. Changes on average \pm standard error of mineral constituent content for the different treatments across the experiment.

Note: there were no phosphate in clogging substances of CK treatment

Table A5. Paired samples t-test of emitter clogging mineral composition in different treatments.

| Minerals | Treatments | CK | MKP_0.15 | UP_0.15 | APP_0.15 | MKP_0.30 | UP_0.30 | APP_0.30 |
|-----------|------------|----|----------|---------|----------|----------|---------|----------|
| Carbonate | CK | — | ** | ** | ** | ** | ** | ** |
| | MKP_0.15 | | — | NS | NS | ** | ** | ** |
| | UP_0.15 | | | — | * | ** | ** | ** |
| | APP_0.15 | | | | — | ** | NS | ** |
| | MKP_0.30 | | | | | — | ** | ** |
| | UP_0.30 | | | | | | — | ** |
| | APP_0.30 | | | | | | | — |
| phosphate | CK | — | ** | ** | ** | ** | ** | ** |
| | MKP_0.15 | | — | ** | ** | ** | ** | ** |
| | UP_0.15 | | | — | ** | ** | ** | ** |
| | APP_0.15 | | | | — | ** | ** | ** |
| | MKP_0.30 | | | | | — | ** | ** |
| | UP_0.30 | | | | | | — | * |
| | APP_0.30 | | | | | | | — |
| Silicate | CK | — | ** | ** | ** | ** | * | * |
| | MKP_0.15 | | — | ** | ** | NS | ** | ** |
| | UP_0.15 | | | — | ** | ** | NS | NS |
| | APP_0.15 | | | | — | ** | NS | NS |
| | MKP_0.30 | | | | | — | ** | ** |
| | UP_0.30 | | | | | | — | NS |
| | APP_0.30 | | | | | | | — |
| Quartz | CK | — | ** | ** | ** | ** | ** | ** |
| | MKP_0.15 | | — | ** | ** | * | NS | NS |
| | UP_0.15 | | | — | * | * | ** | ** |
| | APP_0.15 | | | | — | ** | ** | ** |
| | MKP_0.30 | | | | | — | NS | * |
| | UP_0.30 | | | | | | — | NS |
| | APP_0.30 | | | | | | | — |

Note: asterisks indicate that differences between treatments are significant at $p < 0.05$ (*) or $p < 0.01$ (**), and NS means not significant at $p < 0.05$.

2.7. Correlations between *CU* and *Dra*

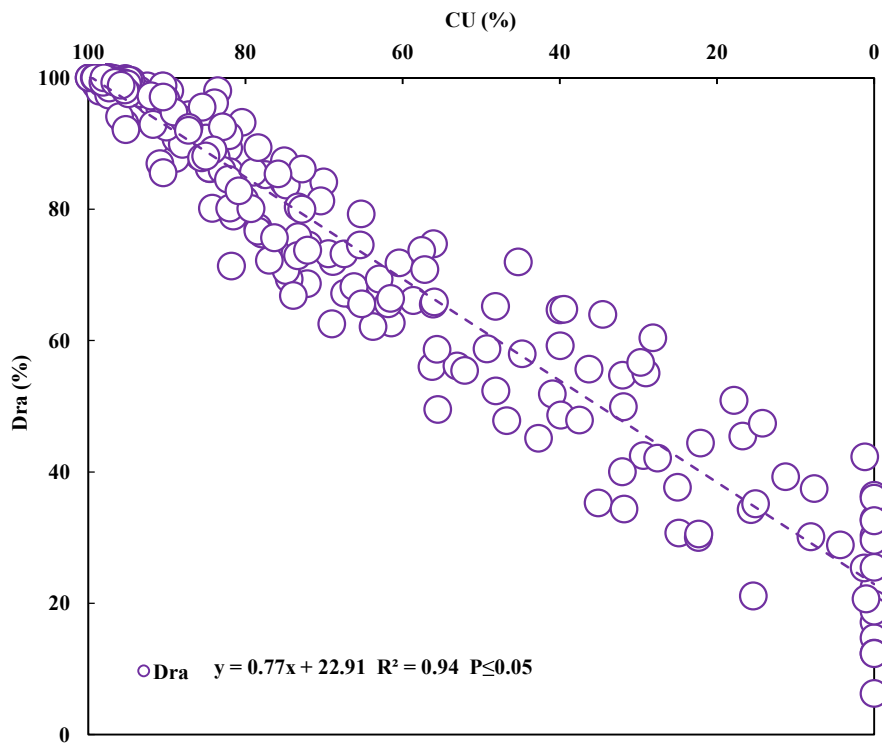


Fig. A11. Correlations between *CU* and *Dra*.

3. Supplementary information in *Discussion section*

3.1. Average \pm standard deviation of water pH

Table A5. Average \pm standard deviation of water pH.

| CK | MKP_0.15 | UP_0.15 | APP_0.15 | MKP_0.30 | UP_0.30 | APP_0.30 |
|---------------|---------------|---------------|---------------|---------------|---------------|---------------|
| 7.5 \pm 0.4 | 6.7 \pm 0.4 | 5.6 \pm 0.4 | 7.5 \pm 0.4 | 6.5 \pm 0.4 | 3.1 \pm 0.4 | 7.5 \pm 0.4 |

Note: pH was measured by a pH meter (manufacture: Rex, China; type: PHSJ-6L).

3.2. Correlation analysis of the content changes of primary mineral components

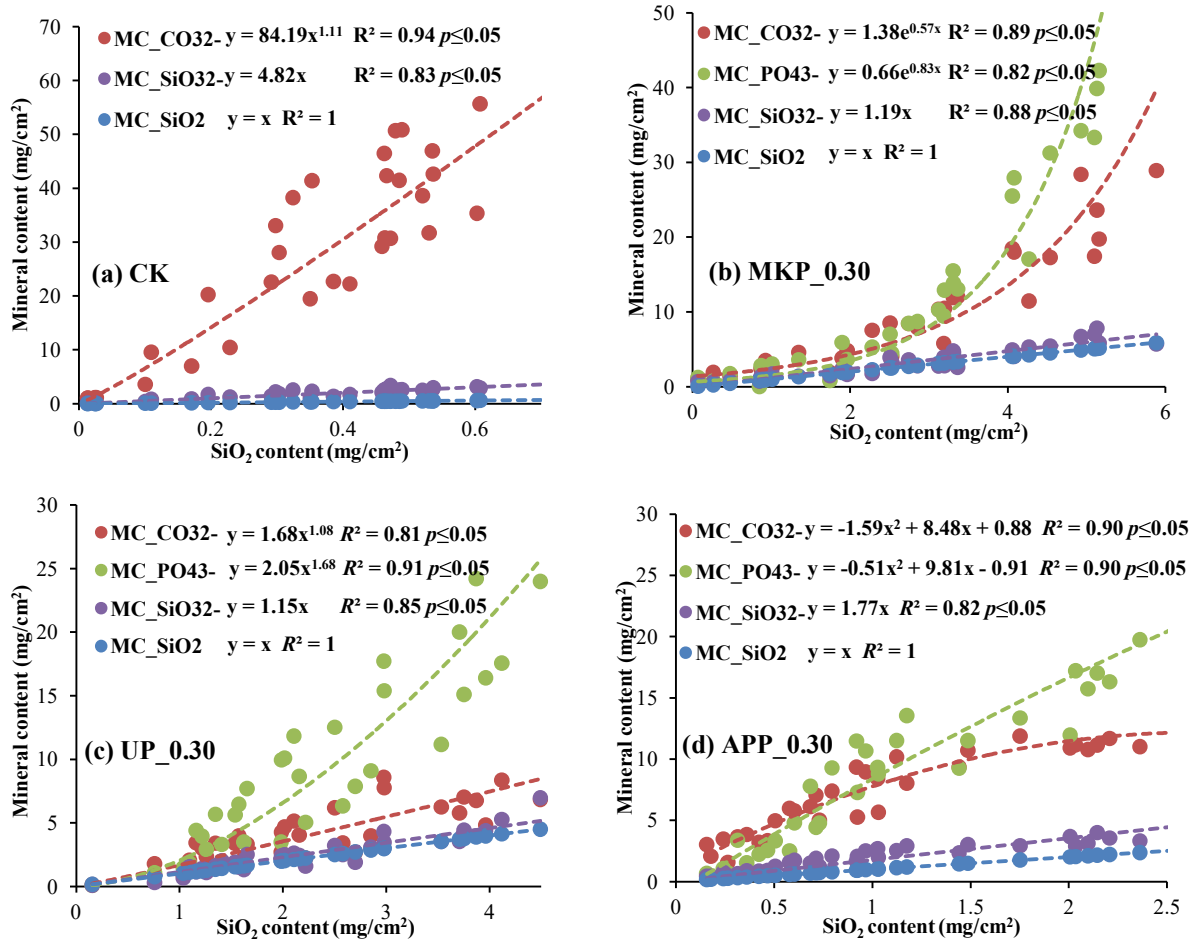


Fig. A12. Correlation analysis of the content changes of primary mineral components.

Note: (a), (b), (c), and (d) shown the results of CK, MKP_0.30, UP_0.30 and APP_0.30 respectively. The x - axes are the quartz of CK, and the y - axes are the composition of other minerals.